



IPPC BAT Conclusions

[COMMISSION IMPLEMENTING DECISION \(EU\) 2017/1442](#) establishing best available techniques (BAT) conclusions, under Directive 2010/75/EU of the European Parliament and of the Council, for large combustion plants.

In accordance with Article 14(3) of the Directive on Industrial Emissions [2010/75/EU](#) (IED) *“BAT conclusions shall be the reference for setting the permit conditions”*.

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GENERAL CONSIDERATIONS:

SCOPE

These BAT conclusions concern the following activities specified in Annex I to Directive 2010/75/EU:

- 1.1: Combustion of fuels in installations with a total rated thermal input of 50 MW or more, only when this activity takes place in combustion plants with a total rated thermal input of 50 MW or more.
- 1.4: Gasification of coal or other fuels in installations with a total rated thermal input of 20 MW or more, only when this activity is directly associated to a combustion plant.
- 5.2: Disposal or recovery of waste in waste co-incineration plants for non-hazardous waste with a capacity exceeding 3 tonnes per hour or for hazardous waste with a capacity exceeding 10 tonnes per day, only when this activity takes place in combustion plants covered under 1.1 above.

In particular, these BAT conclusions cover upstream and downstream activities directly associated with the aforementioned activities including the emission prevention and control techniques applied.

The fuels considered in these BAT conclusions are any solid, liquid and/or gaseous combustible material including:

- solid fuels (e.g. coal, lignite, peat),
- biomass (as defined in Article 3(31) of Directive 2010/75/EU),
- liquid fuels (e.g. heavy fuel oil and gas oil),
- gaseous fuels (e.g. natural gas, hydrogen-containing gas and syngas),
- industry-specific fuels (e.g. by-products from the chemical and iron and steel industries),
- waste except mixed municipal waste as defined in Article 3(39) and except other waste listed in Article 42(2)(a)(ii) and (iii) of Directive 2010/75/EU.

These BAT conclusions do not address the following:

- combustion of fuels in units with a rated thermal input of less than 15 MW,
- combustion plants benefitting from the limited life time or district heating derogation as set out in Articles 33 and 35 of Directive 2010/75/EU, until the derogations set in their permits expire, for what concerns the BAT-AELs for the pollutants covered by the derogation, as well as for other pollutants whose emissions would have been reduced by the technical measures obviated by the derogation,
- gasification of fuels, when not directly associated to the combustion of the resulting syngas,

- gasification of fuels and subsequent combustion of syngas when directly associated to the refining of mineral oil and gas,
- the upstream and downstream activities not directly associated to combustion or gasification activities,
- combustion in process furnaces or heaters,
- combustion in post-combustion plants,
- flaring,
- combustion in recovery boilers and total reduced sulphur burners within installations for the production of pulp and paper, as this is covered by the BAT conclusions for the production of pulp, paper and board,
- combustion of refinery fuels at the refinery site, as this is covered by the BAT conclusions for the refining of mineral oil and gas,
- disposal or recovery of waste in:
 - waste incineration plants (as defined in Article 3(40) of Directive 2010/75/EU),
 - waste co-incineration plants where more than 40 % of the resulting heat release comes from hazardous waste,
 - waste co-incineration plants combusting only wastes, except if these wastes are composed at least partially of biomass as defined in Article 3(31)(b) of Directive 2010/75/EU,as this is covered by the BAT conclusions for waste incineration.

Other BAT conclusions and reference documents that could be relevant for the activities covered by these BAT conclusions are the following:

- Common Waste Water and Waste Gas Treatment/Management Systems in the Chemical Sector (CWW)
- Chemical BREF series (LVOC, etc.)
- Economics and Cross-Media Effects (ECM)
- Emissions from Storage (EFS)
- Energy Efficiency (ENE)
- Industrial Cooling Systems (ICS)
- Iron and Steel Production (IS)
- Monitoring of Emissions to Air and Water from IED installations (ROM)
- Production of Pulp, Paper and Board (PP)
- Refining of Mineral Oil and Gas (REF)

- Waste Incineration (WI)
- Waste Treatment (WT)

GENERAL CONSIDERATIONS

Best Available Techniques

The techniques listed and described in these BAT conclusions are neither prescriptive nor exhaustive. Other techniques may be used that ensure at least an equivalent level of environmental protection.

Unless otherwise stated, these BAT conclusions are generally applicable.

Emission levels associated with the best available techniques (BAT-AELs)

Where emission levels associated with the best available techniques (BAT-AELs) are given for different averaging periods, all of those BAT-AELs have to be complied with.

The BAT-AELs set out in these BAT conclusions may not apply to liquid-fuel-fired and gas-fired turbines and engines for emergency use operated less than 500 h/yr, when such emergency use is not compatible with meeting the BAT-AELs.

BAT-AELs for emissions to air

Emission levels associated with the best available techniques (BAT-AELs) for emissions to air given in these BAT conclusions refer to concentrations, expressed as mass of emitted substance per volume of flue-gas under the following standard conditions: dry gas at a temperature of 273,15 K, and a pressure of 101,3 kPa, and expressed in the units mg/Nm3, µg/Nm3 or ng I-TEQ/Nm3.

The monitoring associated with the BAT-AELs for emissions to air is given in BAT 4

Reference conditions for oxygen used to express BAT-AELs in this document are shown in the table given below.

Activity	Reference oxygen level (OR)
Combustion of solid fuels	6 vol-%
Combustion of solid fuels in combination with liquid and/or gaseous fuels	
Waste co-incineration	
Combustion of liquid and/or gaseous fuels when not taking place in a gas turbine or an engine	3 vol-%
Combustion of liquid and/or gaseous fuels when taking place in a gas turbine or an engine	15 vol-%
Combustion in IGCC plants	

$$E_R = \frac{21 - O_R}{21 - O_M} (E_M)$$

Where:

E_R: emission concentration at the reference oxygen level O_R;

O_R: reference oxygen level in vol- %;

E_M: measured emission concentration;

O_M: measured oxygen level in vol- %.

For averaging periods, the following definitions apply

Averaging period	Definition
Daily average	Average over a period of 24 Hours of valid hourly measurements
Yearly average	Average over a period of one year of valid hourly measurements
Average over the sampling period	Average value of three consecutive measurements of at least 30 minutes each ¹
Average of samples obtained during one year	Average of the values obtained during one year of the periodic measurements taken with the monitoring frequency set for each parameter

BAT-AELs for emissions to water

Emission levels associated with the best available techniques (BAT-AELs) for emissions to water given in these BAT conclusions refer to concentrations, expressed as mass of emitted substance per volume of water, and expressed in µg/l, mg/l, or g/l. The BAT-AELs refer to daily averages, i.e. 24-hour flow-proportional composite samples. Time-proportional composite samples can be used provided that sufficient flow stability can be demonstrated.

The monitoring associated with BAT-AELs for emissions to water is given in BAT 5

Energy efficiency levels associated with the best available techniques (BAT-AEELs)

An energy efficiency level associated with the best available techniques (BAT-AEEL) refers to the ratio between the combustion unit's net energy output(s) and the combustion unit's fuel/feedstock energy input at actual unit design. The net energy output(s) is determined at the combustion, gasification, or IGCC unit boundaries, including auxiliary systems (e.g. flue-gas treatment systems), and for the unit operated at full load.

In the case of combined heat and power (CHP) plants:

¹ For any parameter where, due to sampling or analytical limitations, 30-minute measurement is inappropriate, a suitable sampling period is employed. For PCDD/F, a sampling period of 6 to 8 hours is used.

- the net total fuel utilisation BAT-AEEL refers to the combustion unit operated at full load and tuned to maximise primarily the heat supply and secondarily the remaining power that can be generated,
- the net electrical efficiency BAT-AEEL refers to the combustion unit generating only electricity at full load.

BAT-AEELs are expressed as a percentage. The fuel/feedstock energy input is expressed as lower heating value (LHV).

The monitoring associated with BAT-AEELs is given in BAT 2

Categorisation of combustion plants/units according to their total rated thermal input

For the purposes of these BAT conclusions, when a range of values for the total rated thermal input is indicated, this is to be read as 'equal to or greater than the lower end of the range and lower than the upper end of the range'. For example, the plant category 100–300 MW_{th} is to be read as: combustion plants with a total rated thermal input equal to or greater than 100 MW and lower than 300 MW.

When a part of a combustion plant discharging flue-gases through one or more separate ducts within a common stack is operated less than 1 500 h/yr, that part of the plant may be considered separately for the purpose of these BAT conclusions. For all parts of the plant, the BAT-AELs apply in relation to the total rated thermal input of the plant. In such cases, the emissions through each of those ducts are monitored separately.

Applicability checklist

Kindly tick relevant sections which are applicable and will be under consideration in this assessment.

	Tick	Comment (where N/A) kindly indicate
1. GENERAL BAT CONCLUSIONS	Compulsory	Addressed
2. BAT CONCLUSIONS FOR COMBUSTIONS OF SOLID FUELS	<input type="checkbox"/>	N/A
2.1 BAT CONCLUSIONS FOR THE COMBUSTION OF COAL AND/OR LIGNITE	<input type="checkbox"/>	N/A
2.2 BAT CONCLUSIONS FOR THE COMBUSTION OF SOLID BIOMASS AND/OR PEAT	<input type="checkbox"/>	N/A
3. BAT CONCLUSIONS FOR THE COMBUSTION OF LIQUID FUELS	<input type="checkbox"/>	N/A
3.1. HFO- AND/OR GAS-OIL-FIRED BOILERS	<input type="checkbox"/>	N/A
3.2. HFO- AND/OR GAS-OIL-FIRED ENGINES	<input type="checkbox"/>	N/A
3.3. GAS-OIL-FIRED GAS TURBINES	<input type="checkbox"/>	N/A
4. BAT CONCLUSIONS FOR THE COMBUSTION OF GASEOUS FUELS	<input checked="" type="checkbox"/>	CCGT uses LNG
4.1. BAT CONCLUSIONS FOR THE COMBUSTION OF NATURAL GAS	<input checked="" type="checkbox"/>	CCGT uses LNG
4.2. BAT CONCLUSIONS FOR THE COMBUSTION OF IRON AND STEEL PROCESS GASES	<input type="checkbox"/>	N/A
4.3. BAT CONCLUSIONS FOR THE COMBUSTION OF GASEOUS AND/OR LIQUID FUELS ON OFFSHORE PLATFORMS	<input type="checkbox"/>	N/A
5. BAT CONCLUSIONS FOR MULTI-FUEL-FIRED PLANT	<input type="checkbox"/>	N/A
5.1. BAT CONCLUSIONS FOR THE COMBUSTION OF PROCESS FUELS FROM THE CHEMICAL INDUSTRY	<input type="checkbox"/>	N/A
6. BAT CONCLUSIONS FOR THE CO-INCINERATION OF WASTE	<input type="checkbox"/>	N/A
7. BAT CONCLUSIONS FOR GASIFICATION	<input type="checkbox"/>	N/A

Comparison Exercise with BAT

1. GENERAL BAT CONCLUSIONS

BAT conclusion		STATUS AT INSTALLATION: [ENTER NAME OF OPERATOR] DATE: [ENTER DATE OF ASSESSMENT] Applicability Assessment (describe how the technique applies or not to your installation)	STATE WHETHER IT IS IN PLACE OR STATE SCHEDULE FOR IMPLEMENTATIO N	ERA Reply	EGM Reply	ERA reply	EGM Reply (9 th Dec 2021)
BAT 1 Environmental Management System	<p>In order to improve the overall environmental performance, BAT is to implement and adhere to an environmental management system (EMS) that incorporates all of the following features:</p> <ul style="list-style-type: none"> (i) commitment of the management, including senior management; (ii) definition, by the management, of an environmental policy that includes the continuous improvement of the environmental performance of the installation; (iii) planning and establishing the necessary procedures, objectives and targets, in conjunction with financial planning and investment; (iv) implementation of procedures paying particular attention to: 	<p>An environmental management system certified to ISO14001:2015 is in place for ElectroGas Malta Limited.</p> <p>The scope of the certification includes 'Electricity production by natural gas burning. Storage and re-gasification of Liquid Natural Gas'.</p> <p>i. Management</p>	Implemented.	<p>Noted. Kindly indicate whether an OTNOC management plan is in place. Kindly provide :</p> <ul style="list-style-type: none"> a) management plan referred to in point xi b) Waste management plan referred in point xii c) Plan mentioned in point xiii d) Plan mentioned in point xiv 	<ul style="list-style-type: none"> a) Kindly refer to Annex 15 – OTNOC plan b) Kindly refer to Annex 10 – Waste Management Plan c) Kindly refer to the updated ERP which will be provided in August 2021 and which is currently being updated to reflect the updates in CERP which is 	<ul style="list-style-type: none"> a) Noted b) Noted c) Noted, such an item will be addressed with COMAH d) Noted e) Noted 	

	<p>(a) structure and responsibility</p> <p>(b) recruitment, training, awareness and competence</p> <p>(c) communication</p> <p>(d) employee involvement</p> <p>(e) documentation</p> <p>(f) effective process control</p> <p>(g) planned regular maintenance programmes</p> <p>(h) emergency preparedness and response</p> <p>(i) safeguarding compliance with environmental legislation;</p> <p>(v) checking performance and taking corrective action, paying particular attention to:</p> <p>(a) monitoring and measurement (see also the JRC Reference Report on Monitoring of emissions to air and water from IED-installations — ROM)</p> <p>(b) corrective and preventive action</p> <p>(c) maintenance of records</p> <p>(d) independent (where practicable) internal and external auditing in order to determine whether or not the EMS conforms to planned arrangements and has been properly implemented and maintained;</p> <p>(vi) review, by senior management, of the EMS and its continuing suitability, adequacy and effectiveness;</p> <p>(vii) following the development of cleaner technologies;</p>	<p>commitment is demonstrated through the implementation of the ISO14001:2015 certified EMS.</p> <p>ii. EGM's environmental policy 'EGM-HSE-POL-002' is in place and have been endorsed by the board of directors.</p> <p>iii. Planning is in intrinsic part of the ISO14001 methodology. The necessary procedures, objectives and targets and financial resources are all addressed through the ISO14001:2015 certified EMS.</p> <p>iv. The required documented evidence to attest to the various aspects listed has been established</p>		<p>e) Noise management plan mentioned in xv</p>	<p>currently at its final stages of review.</p> <p>d) Fuels used do not lead to dust generation. Loading and unloading of fuels is carried out on hard surfaces.</p> <p>e) Kindly refer to Annex 16 – Noise and vibrations management plan</p>		
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	<p>consideration for the environmental impacts from the eventual decommissioning of the installation at the stage of designing a new plant, and throughout its operating life including;</p> <p>(a) avoiding underground structures</p> <p>(b) incorporating features that facilitate dismantling</p> <p>(c) choosing surface finishes that are easily decontaminated</p> <p>(d) using an equipment configuration that minimises trapped chemicals and facilitates drainage or cleaning</p> <p>(d) designing flexible, self-contained equipment that enables phased closure</p> <p>(f) using biodegradable and recyclable materials where possible;</p> <p>(ix) application of sectoral benchmarking on a regular basis. Specifically for this sector, it is also important to consider the following features of the EMS, described where appropriate in the relevant BAT:</p> <p>(x) quality assurance/quality control programmes to ensure that the characteristics of all fuels are fully determined and controlled (see BAT 9);</p> <p>(xi) a management plan in order to reduce emissions to air and/or to water during other than normal operating conditions, including start-up and shutdown periods (see BAT 10 and BAT 11);</p> <p>(xii) a waste management plan to ensure that waste is avoided, prepared for reuse, recycled or otherwise recovered, including the use of techniques given in BAT 16;</p>	<p>and is maintained securely.</p> <p>v. Performance evaluation including internal and external auditing is addressed through the ISO14001:2015 certified EMS. A register of corrective actions is maintained as a live document. Maintenance is monitored and recorded. A monitoring programme has already been established through the existing permit process.</p> <p>vi. The suitability, adequacy and effectiveness of the EMS is discussed and addressed during frequent management</p>					
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	<p>(xiii) a systematic method to identify and deal with potential uncontrolled and/or unplanned emissions to the environment, in particular:</p> <p>(a) emissions to soil and groundwater from the handling and storage of fuels, additives, by-products and wastes</p> <p>(b) emissions associated with self-heating and/or self-ignition of fuel in the storage and handling activities;</p> <p>(xiv) a dust management plan to prevent or, where that is not practicable, to reduce diffuse emissions from loading, unloading, storage and/or handling of fuels, residues and additives;</p> <p>(xv) a noise management plan where a noise nuisance at sensitive receptors is expected or sustained, including:</p> <p>(a) a protocol for conducting noise monitoring at the plant boundary</p> <p>(b) a noise reduction programme</p> <p>(c) a protocol for response to noise incidents containing appropriate actions and timelines</p> <p>(d) a review of historic noise incidents, corrective actions and dissemination of noise incident knowledge to the affected parties;</p> <p>(xvi) for the combustion, gasification or co-incineration of malodorous substances, an odour management plan including:</p> <p>(a) a protocol for conducting odour monitoring</p> <p>(b) where necessary, an odour elimination programme to identify and eliminate or reduce the odour emissions</p>	<p>t review held.</p> <p>vii. A life-cycle approach is adopted to establish and regularly maintain a register of environmental aspects and their associated impacts</p> <p>ix. External audits including ISO14001:2015 certification audits take into consideration what is appropriate for the sector of this installation. Moreover, particular attention was given to the scope of the ISO14001 audit certification.</p> <p>x. Refer to BAT 9.</p> <p>xi. Environmental aspects and their impacts have been determined</p>					
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	<p>(c) a protocol to record odour incidents and the appropriate actions and timelines</p> <p>(e) a review of historic odour incidents, corrective actions and the dissemination of odour incident knowledge to the affected parties.</p> <p>Where an assessment shows that any of the elements listed under items x to xvi are not necessary, a record is made of the decision, including the reasons.</p>	<p>for normal operating conditions as well as abnormal or emergency situations. An emergency response plan has been established and emergency drills are performed regularly in order to exercise and improve the emergency procedures.</p> <p>xii. A waste management plan 'EGM-HSE-EP-13' has been established. Internal audits focussing on waste management are carried out.</p> <p>xiii. This feature is addressed through:</p> <p>a) Risk assessments which were carried out to assess</p>					
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		<p>the risk of chemical spills. Containment measures have been identified and established. Furthermore, auditing routines take these issues into consideration.</p> <p>b) Extensive safety studies which were carried out and are being updated.</p> <p>xiv. Fuels used do not lead to dust generation. Loading and unloading of fuels is carried out on hard surfaces.</p> <p>xv. Noise monitoring is performed annually, and any</p>					
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			complaints submitted are investigated. Additional internal noise monitoring is carried out periodically. All incidents related to noise are captured in the environmental incidents statistics. Noise management was taken into consideration at design stage. xvi. Odour monitoring is not applicable as LNG is odourless and no mercaptan is used.					
	Applicability	The scope (e.g. level of detail) and nature of the EMS (e.g. standardised or non-standardised) will generally be related to the nature, scale and complexity of the installation, and the range of environmental impacts it may have.						
BAT 2 Determine the net electrical efficiency	BAT is to determine the net electrical efficiency and/or the net total fuel utilisation and/or the net mechanical energy efficiency of the gasification, IGCC and/or		This BAT is not applicable to this CCGT installation as	Not applicable	As stated above this section is compulsory and does not relate	Kindly refer to Annex 11 – Performance test	Noted	

and/or the net total fuel utilisation and/or the net mechanical energy efficiency of the gasification.	combustion units by carrying out a performance test at full load ² , according to EN standards, after the commissioning of the unit and after each modification that could significantly affect the net electrical efficiency and/or the net total fuel utilisation and/or the net mechanical energy efficiency of the unit. If EN standards are not available, BAT is to use ISO, national or other international standards that ensure the provision of data of an equivalent scientific quality.	no gasification process is carried out.		exclusively to gasification as described in the BREF. It is ERA’s interpretation that this needs to be provided. Any performance tests are completed to the required EN/ISO standards as detailed within BAT 2.															
BAT 3 monitor key process parameters relevant for emissions to air and water	<p>BAT is to monitor key process parameters relevant for emissions to air and water including those given below.</p> <table><tr><th>Stream</th><th>Parameter(s)</th><th>Monitoring</th></tr><tr><td rowspan="3">Flue-gas</td><td>Flow</td><td>Periodic or continuous determination</td></tr><tr><td>Oxygen content, temperature, and pressure</td><td rowspan="2">Periodic or continuous measurement</td></tr><tr><td>Water vapour content⁽¹⁾</td></tr><tr><td>Waste water from flue-gas treatment</td><td>Flow, pH, and temperature</td><td>Continuous measurement</td></tr></table> <p>⁽¹⁾ The continuous measurement of the water vapour content of the flue-gas is not necessary if the sampled flue-gas is dried before analysis.</p>	Stream	Parameter(s)	Monitoring	Flue-gas	Flow	Periodic or continuous determination	Oxygen content, temperature, and pressure	Periodic or continuous measurement	Water vapour content ⁽¹⁾	Waste water from flue-gas treatment	Flow, pH, and temperature	Continuous measurement	<p>All main stacks and bypass stacks have a continuous emissions monitoring system (CEMS) connected back to the CCGT Distributed control system (DCS).</p> <p>Flue gas flow, oxygen content and temperature are monitored continuously by CEMS.</p> <p>Flue-gas from CCGT stacks is</p>	Implemented.	Noted.			
Stream	Parameter(s)	Monitoring																	
Flue-gas	Flow	Periodic or continuous determination																	
	Oxygen content, temperature, and pressure	Periodic or continuous measurement																	
	Water vapour content ⁽¹⁾																		
Waste water from flue-gas treatment	Flow, pH, and temperature	Continuous measurement																	

² In the case of CHP units, if for technical reasons the performance test cannot be carried out with the unit operated at full load for the heat supply, the test can be supplemented or substituted by a calculation using full load parameters.

		<p>dried before analysis and therefore water vapour content analysis does not apply.</p> <p>Pressure is monitored at inlet to ensure correct plant operation.</p> <p>No flue-gas treatment is carried out, therefore no wastewater from flue-gas treatment is generated.</p>																					
BAT 4 Monitor emissions to air	<p>BAT is to monitor emissions to air with at least the frequency given below standards. If EN standards are not available, BAT is to use SO₂, national or other ensure the provision of data of an equivalent scientific quality.</p> <table><tr><th>Substance/Parameter</th><th>Fuel/Process/Type of combustion plant</th><th>Combustion plant total rated thermal input</th><th>Standard(s)¹ which are applicable to</th><th>Monitoring frequency</th></tr><tr><td>NH₃</td><td>— When SCR and/or SNCR is used</td><td>All sizes</td><td>natural-gas-fired turbines, along with dust, are continuously monitored by CEMS, in compliance to Generic EN 14181 standards</td><td>Continuous</td></tr><tr><td>NO_x</td><td>— Coal and/or lignite including waste co-incineration</td><td>All sizes</td><td>Generic EN 14181 standards. Routine QAL3, Annual Surveillance Tests (AST) and QAL2 tests are run on the CEMS</td><td>Continuous</td></tr></table>			Substance/Parameter	Fuel/Process/Type of combustion plant	Combustion plant total rated thermal input	Standard(s) ¹ which are applicable to	Monitoring frequency	NH ₃	— When SCR and/or SNCR is used	All sizes	natural-gas-fired turbines, along with dust, are continuously monitored by CEMS, in compliance to Generic EN 14181 standards	Continuous	NO _x	— Coal and/or lignite including waste co-incineration	All sizes	Generic EN 14181 standards. Routine QAL3, Annual Surveillance Tests (AST) and QAL2 tests are run on the CEMS	Continuous	Implemented.	Noted, with respect to the monitoring of methane, this requirement shall be reflected in the permit.	As per BAT 4, CH4 monitoring is applicable to natural gas fired engines and not to CCGTs. As such, EGM is of the opinion that this should not be introduced in the permit.	Agreed, no methane monitoring is required as per BAT	Noted.
Substance/Parameter	Fuel/Process/Type of combustion plant	Combustion plant total rated thermal input	Standard(s) ¹ which are applicable to	Monitoring frequency																			
NH ₃	— When SCR and/or SNCR is used	All sizes	natural-gas-fired turbines, along with dust, are continuously monitored by CEMS, in compliance to Generic EN 14181 standards	Continuous																			
NO _x	— Coal and/or lignite including waste co-incineration	All sizes	Generic EN 14181 standards. Routine QAL3, Annual Surveillance Tests (AST) and QAL2 tests are run on the CEMS	Continuous																			

[illegible]

	CO	<ul style="list-style-type: none"> — Coal and/or lignite including waste co-incineration — Solid biomass and/or peat including waste co-incineration — HFO- and/or gas-oil-fired boilers and engines — Gas-oil-fired gas turbines — Natural-gas-fired boilers, engines, and turbines — Iron and steel process gases — Process fuels from the chemical industry — IGCC plants 	All sizes	Generic EN standards	Cor						
		<ul style="list-style-type: none"> — Combustion plants on offshore platforms 	All sizes	EN 15058	On (6)						
	SO ₂	<ul style="list-style-type: none"> — Coal and/or lignite including waste co-incineration — Solid biomass and/or peat including waste co-incineration 	All sizes	Generic EN standards and EN 14791	Cor (8),(9)						

[illegible]

[illegible]

		waste co-incineration	$\geq 300 \text{ MW}_{\text{th}}$	Generic EN standards and EN 14884	Con					
		— Solid biomass and/or peat	All sizes	EN 13211	One year					
		— Waste co-incineration with solid biomass and/or peat	All sizes	EN 13211	One through					
		— IGCC plants	$\geq 100 \text{ MW}_{\text{th}}$	EN 13211	One year					
	TVOC	— HFO- and/or gas-oil-fired engines	All sizes	EN 12619	One month					
		— Process fuels from the chemical industry in boilers								
		— Waste co-incineration with coal, lignite, solid biomass and/or peat	All sizes	Generic EN standards	Con					
	Formaldehyde	— Natural-gas in spark-ignited lean-burn gas and dual fuel engines	All sizes	No EN standard available	One					
	CH ₄	— Natural-gas-fired engines	All sizes	EN ISO 25139	One (21)					
	PCDD/F	— Process fuels from the chemical industry in boilers	All sizes	EN 1948-1, EN 1948-2, EN 1948-3	One month					
		— Waste co-incineration								
<p>(1) Generic EN standards for continuous measurements are EN 15267-1, EN 15267-2, EN 15267-3, and EN 14181. EN standards for periodic measurements are given in the table.</p> <p>(2) The monitoring frequency does not apply where plant operation would be for the sole purpose of performing an emission measurement.</p> <p>(3) In the case of plants with a rated thermal input of < 100 MW operated < 1 500 h/yr, the minimum monitoring frequency may be at least once every six months. For gas turbines, periodic monitoring is carried out with a combustion plant load of > 70 %. For co-incineration of waste with coal, lignite, solid biomass and/or peat, the monitoring frequency needs to also take into account Part 6 of Annex VI to the IED.</p>										

	<p>(4) In the case of use of SCR, the minimum monitoring frequency may be at least once every year, if the emission levels are proven to be sufficiently stable.</p> <p>(5) In the case of natural-gas-fired turbines with a rated thermal input of < 100 MW operated < 1 500 h/yr, or in the case of existing OCGTs, PEMS may be used instead.</p> <p>(6) PEMS may be used instead.</p> <p>(7) Two sets of measurements are carried out, one with the plant operated at loads of > 70 % and the other one at loads of < 70 %.</p> <p>(8) As an alternative to the continuous measurement in the case of plants combusting oil with a known sulphur content and where there is no flue- gas desulphurisation system, periodic measurements at least once every three months and/or other procedures ensuring the provision of data of an equivalent scientific quality may be used to determine the SO₂ emissions.</p> <p>(9) In the case of process fuels from the chemical industry, the monitoring frequency may be adjusted for plants of < 100 MWth after an initial characterisation of the fuel (see BAT 5) based on an assessment of the relevance of pollutant releases (e.g. concentration in fuel, flue-gas treatment employed) in the emissions to air, but in any case at least each time that a change of the fuel characteristics may have an impact on the emissions.</p> <p>(10) If the emission levels are proven to be sufficiently stable, periodic measurements may be carried out each time that a change of the fuel and/or waste characteristics may have an impact on the emissions, but in any case at least once every year. For co-incineration of waste with coal, lignite, solid biomass and/or peat, the monitoring frequency needs to also take into account Part 6 of Annex VI to the IED.</p> <p>(11) In the case of process fuels from the chemical industry, the monitoring frequency may be adjusted after an initial characterisation of the fuel (see BAT 5) based on an assessment of the relevance of pollutant releases (e.g. concentration in fuel, flue-gas treatment employed) in the emissions to air, but in any case at least each time that a change of the fuel characteristics may have an impact on the emissions.</p> <p>(12) In the case of plants with a rated thermal input of < 100 MW operated < 500 h/yr, the minimum monitoring frequency may be at least once every year. In the case of plants with a rated thermal input of < 100 MW operated between 500 h/yr and 1 500 h/yr, the monitoring frequency may be reduced to at least once every six months.</p> <p>(13) If the emission levels are proven to be sufficiently stable, periodic measurements may be carried out each time that a change of the fuel and/or waste characteristics may have an impact on the emissions, but in any case at least once every six months.</p> <p>(14) In the case of plants combusting iron and steel process gases, the minimum monitoring frequency may be at least once every six months if the emission levels are proven to be sufficiently stable.</p> <p>(15) The list of pollutants monitored and the monitoring frequency may be adjusted after an initial characterisation of the fuel (see BAT 5) based on an assessment of the relevance of pollutant releases (e.g. concentration in fuel, flue-gas treatment employed) in the emissions to air, but in any case at least each time that a change of the fuel characteristics may have an impact on the emissions.</p> <p>(16) In the case of plants operated < 1 500 h/yr, the minimum monitoring frequency may be at least once every six months.</p> <p>(17) In the case of plants operated < 1 500 h/yr, the minimum monitoring frequency may be at least once every year.</p>						
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	<p>(18) Continuous sampling combined with frequent analysis of time-integrated samples, e.g. by a standardised sorbent trap monitoring method, may be used as an alternative to continuous measurements.</p> <p>(19) If the emission levels are proven to be sufficiently stable due to the low mercury content in the fuel, periodic measurements may be carried out only each time that a change of the fuel characteristics may have an impact on the emissions.</p> <p>(20) The minimum monitoring frequency does not apply in the case of plants operated < 1 500 h/yr.</p> <p>(21) Measurements are carried out with the plant operated at loads of > 70 %.</p> <p>(22) In the case of process fuels from the chemical industry, monitoring is only applicable when the fuels contain chlorinated substances. 17.8.2017 L 212/17 Official Journal of the European Union EN</p>																																	
BAT 5 monitor emissions to water from flue-gas treatment	<p>BAT is to monitor emissions to water from flue-gas treatment with at least the frequency given below and in accordance with EN standards. If EN standards are not available, BAT is to use ISO, national or other international standards that ensure the provision of data of an equivalent scientific quality.</p> <table><tr><td colspan="2">Substance/Parameter</td><td>Standard(s)</td></tr><tr><td colspan="2">Total organic carbon (TOC)⁽¹⁾</td><td>EN 1484</td></tr><tr><td colspan="2">Chemical oxygen demand (COD)⁽¹⁾</td><td>No EN standard available</td></tr><tr><td colspan="2">Total suspended solids (TSS)</td><td>EN 872</td></tr><tr><td colspan="2">Fluoride (F⁻)</td><td>EN ISO 10304-1</td></tr><tr><td colspan="2">Sulphate (SO₄²⁻)</td><td>EN ISO 10304-1</td></tr><tr><td colspan="2">Sulphide, easily released (S²⁻)</td><td>No EN standard available</td></tr><tr><td colspan="2">Sulphite (SO₃²⁻)</td><td>EN ISO 10304-3</td></tr><tr><td>Metals and mettalooids</td><td>As</td><td></td></tr></table>	Substance/Parameter		Standard(s)	Total organic carbon (TOC) ⁽¹⁾		EN 1484	Chemical oxygen demand (COD) ⁽¹⁾		No EN standard available	Total suspended solids (TSS)		EN 872	Fluoride (F ⁻)		EN ISO 10304-1	Sulphate (SO ₄ ²⁻)		EN ISO 10304-1	Sulphide, easily released (S ²⁻)		No EN standard available	Sulphite (SO ₃ ²⁻)		EN ISO 10304-3	Metals and mettalooids	As		<p>This BAT is not applicable to this natural-gas-fired CCGT installation as flue-gas treatment is not carried out.</p>	<p>Not applicable</p>	<p>Whilst noting EGM’s reply, the permit is to maintain the stipulated monitoring as prescribed by the permit at the tie-in point.</p>	<p>While it is noted that monitoring requirements will remain the same in the permit, it is to be noted that no waste water from flue-gas treatment is produced at D4 power plant.</p>	<p>Noted.</p>	
Substance/Parameter		Standard(s)																																
Total organic carbon (TOC) ⁽¹⁾		EN 1484																																
Chemical oxygen demand (COD) ⁽¹⁾		No EN standard available																																
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Sulphide, easily released (S ²⁻)		No EN standard available																																
Sulphite (SO ₃ ²⁻)		EN ISO 10304-3																																
Metals and mettalooids	As																																	

		Cd	Various EN standards available (e.g. EN ISO 11885 or EN ISO 17294-2)						
		Cr							
		Cu							
		Ni							
		Pb							
		Zn							
		Hg	Various EN standards available (e.g. EN ISO 12846 or EN ISO 17852)						
	Chloride (Cl ⁻)		Various EN standards available (e.g. EN ISO 10304-1 or EN ISO 15682)						
	Total nitrogen		EN 12260						
	(1) TOC monitoring and COD monitoring are alternatives. TOC monitoring is the preferred option b it does not rely on the use of very toxic compounds.								
BAT 6 General environmental and combustion performance	In order to improve the general environmental performance of combustion plants and to reduce emissions to air of CO and unburnt substances, BAT is to ensure optimised combustion and to use an appropriate combination of the techniques given below.			a) No mixing is required as the parameters of fuel are monitored to	Implemented	Noted.			
	Technique		Description						
	a	Fuel bending and mixing	Ensure stable combustion conditions and/or reduce the emission pollutants by mixing different qualities of the same fuel type						

	b	Maintenance of the combustion system	Regular planned maintenance according to suppliers' recommendations	ensure quality					
	c	Advanced control system	See description in Section 8.1	b) The CCGT installation is a combustion command system					
	d	Good design of the combustion equipment	Good design of furnace, combustion chambers, burners and associated devices	Generally applicable by a long-term service					
	e	Fuel choice	Select or switch totally or partially to another fuel(s) with a better environmental profile (e.g. with low sulphur and/or mercury content) amongst the available fuels, including in start-up situations or when back-up fuels are used	e) Applicable with agreement (LTSA) with the origin of the process fuels. For existing combustion plants, the fuel chosen at the configuration of the plant (OEM).					
				Planned maintenance inspections and works arising are supervised by OEM. c) CCGTs are run using the					

		<p>install ed Sieme ns T 3000 plant contro l system .</p> <p>d) Not applic able, howev er, GT fulfils ISO 21789 minim um safety design requir ement for a GT.</p> <p>e) CCGTs run on Natura l Gas which is consid ered as a clean burnin g fossil fuel due to the negligi ble amoun</p>						
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		ts of sulfur, mercury and particulates emitted.					
BAT 7 reduce emissions of ammonia to air from the use of selective catalytic reduction (SCR) and/or selective non-catalytic reduction (SNCR)	<p>In order to reduce emissions of ammonia to air from the use of selective catalytic reduction (SCR) and/or selective non-catalytic reduction (SNCR) for the abatement of NO_x emissions, BAT is to optimise the design and/or operation of SCR and/or SNCR (e.g. optimised reagent to NO_x ratio, homogeneous reagent distribution and optimum size of the reagent drops).</p> <p>The BAT-associated emission level</p> <p>(BAT-AEL) for emissions of NH₃ to air from the use of SCR and/or SNCR is < 3–10 mg/Nm³ as a yearly average or average over the sampling period. The lower end of the range can be achieved when using SCR and the upper end of the range can be achieved when using SNCR without wet abatement techniques. In the case of plants combusting biomass and operating at variable loads as well as in the case of engines combusting HFO and/or gas oil, the higher end of the BAT-AEL range is 15 mg/Nm³.</p>	This BAT is not applicable this CCGT installation does not make use of selective catalytic reduction (SCR) and/or selective non-catalytic reduction (SNCR).	Not applicable	Noted.			
BAT 8 emission abatement systems	In order to prevent or reduce emissions to air during normal operating conditions, BAT is to ensure, by appropriate design, operation and maintenance, that the emission abatement systems are used at optimal capacity and availability.	CCGT design ensures optimal capacity and availability of emissions control using measures such as dry low-NO _x burners.	Not applicable	Non-applicability noted.			
BAT 9 Quality assurance/quality control	In order to improve the general environmental performance of combustion and/or gasification plants and to reduce emissions to air, BAT is to include the following elements in the quality assurance/quality	(i) Upon each LNG shipment a sample of the LNG is	Implemented	<p>i. Noted</p> <p>ii. Noted</p>			

programmes for all the fuels used	control programmes for all the fuels used, as part of the environmental management system (see BAT 1):	analysed in accordance to ISO 6974 and ISO 6975, for a number of parameters including LHV, CH ₄ , C ₂ H ₆ , C ₃ , C ₄ +, CO ₂ , N ₂ and Wobbe index.		iii.	Note d			
	(i)Initial full characterisation of the fuel used including at least the parameters listed below and in accordance with EN standards. ISO, national or other international standards may be used provided they ensure the provision of data of an equivalent scientific quality;							
	(ii)Regular testing of the fuel quality to check that it is consistent with the initial characterisation and according to the plant design specifications. The frequency of testing and the parameters chosen from the table below are based on the variability of the fuel and an assessment of the relevance of pollutant releases (e.g. concentration in fuel, flue-gas treatment employed);							
	(ii)Subsequent adjustment of the plant settings as and when needed and practicable (e.g. integration of the fuel characterisation and control in the advanced control system (see description in Section 8.1)).							
	Description							
	Initial characterisation and regular testing of the fuel can be performed by the operator and/or the fuel supplier. If performed by the supplier, the full results are provided to the operator in the form of a product (fuel) supplier specification and/or guarantee.							

		<ul style="list-style-type: none"> Metals and metalloids (As, Cd, Co, Cr, Cu, Fe, Hg, Mn, Ni, Pb, Se, Sn, Ti, V, Zn) 					
	HFO	<ul style="list-style-type: none"> Ash C, S, N, Ni, V 					
	Gas oil	<ul style="list-style-type: none"> Ash N, C, S 					
	Natural gas	<ul style="list-style-type: none"> LHV CH₄, C₂H₆, C₃, C₄+, CO₂, N₂, Wobbe index 					
	Process fuels from the chemical industry ³	<ul style="list-style-type: none"> Br, C, Cl, F, H, N, O, S Metals and metalloids (As, Cd, Co, Cr, Cu, Fe, Hg, Mn, Ni, Pb, Se, Sn, Ti, V, Zn) 					
	Iron and steel process gases	<ul style="list-style-type: none"> LHV, CH₄ (for COG), C_xH_y (for COG), dust, Wobbe index 					
	Waste ⁴	<ul style="list-style-type: none"> LHV Moisture Volatiles, ash, Br, C, Cl, F, H, N, O, S Metals and metalloids (As, Cd, Co, Cr, Cu, Fe, Hg, Mn, Ni, Pb, Se, Sn, Ti, V, Zn) 					
BAT 10 Reduce emissions to air and/or to water during other than normal operating conditions (OTNOC)	<p>In order to reduce emissions to air and/or to water during other than normal operating conditions (OTNOC), BAT is to set up and implement a management plan as part of the environmental management system (see BAT 1), commensurate with the relevance of potential pollutant releases, that includes the following elements:</p> <ul style="list-style-type: none"> appropriate design of the systems considered relevant in causing OTNOC that may have an impact on emissions to air, water and/or soil (e.g. low-load design concepts for reducing the minimum start-up and shutdown loads for stable generation in gas turbines), set-up and implementation of a specific preventive maintenance plan for these relevant systems, 	<p>OEM LTSA maintenance programme is in place.</p> <p>Moreover, this CCGT plant is designed in 3 GTs +1 ST configuration with the possibility of operating in 1+1, 2+1 and 3+1,</p>	Implemented	With respect to the requirement for the periodic assessment of OTNOC emissions. Kindly provide relevant OTNOC management plan/ SOP. With respect to the replies provided, kindly specify which OTNOC events are considered.	Kindly refer to Annex 15 – OTNOC plan	Noted	

³ The list of substances/parameters characterised can be reduced to only those that can reasonably be expected to be present in the fuel(s) based on information on the raw materials and the production processes.

⁴ This characterisation is carried out without prejudice of application of the waste pre-acceptance and acceptance procedure set in BAT 60(a), which may lead to the characterisation and/or checking of other substances/parameters besides those listed here.

	<p>— review and recording of emissions caused by OTNOC and associated circumstances and implementation of corrective actions if necessary,</p> <p>— periodic assessment of the overall emissions during OTNOC (e.g. frequency of events, duration, emissions quantification/estimation) and implementation of corrective actions if necessary.</p>	<p>while also with GT in open cycle.</p> <p>This gives flexibility to operate the plant in different load points while maintaining efficiency and emission limits. This flexibility minimises potential for OTNOC.</p> <p>GT's, via the control system, are programmed in order to minimise start up and shut down periods and normal operation occurs once minimum stable</p>					
BAT 11 monitor emissions to air and/or to water during OTNOC	<p>BAT is to appropriately monitor emissions to air and/or to water during OTNOC.</p> <p>Description</p> <p>The monitoring can be carried out by direct measurement of emissions or by monitoring of surrogate parameters if this proves to be of equal or better scientific quality than the direct measurement of emissions.</p> <p>Emissions during start-up and shutdown (SU/SD) may be assessed based on a detailed emission measurement</p>	<p>Emissions to air are monitored during OTNOC via CEMS. Water usage is monitored for all operating conditions. Cold starting of a HRSG is the most water intensive OTNOC e</p>	In progress	Kindly provide update, notwithstanding as per the requirements of the permit and per BAT 4, the monitoring of emissions takes place continuously including during OTNOC events.	Noted. Data on water consumption is being collected during start up and shut down periods, to evaluate viability to reduce consumption.	Noted	

	carried out for a typical SU/SD procedure at least once every year, and using the results of this measurement to estimate the emissions for each and every SU/SD throughout the year.	vent from a water consumption point of view but this is extremely rare in D4. .																													
BAT 12 Energy Efficiency	In order to increase the energy efficiency of combustion, gasification and/or IGCC units operated ≥ 1 500 h/yr, BAT is to use an appropriate combination of the techniques given below.		a) Combustion optimisation is achieved through Siemens T 3000 advanced control system and through staggered pre-mix combustion using dry low-NOx burners. b) Turbine temperature and pressure are operated at design parameters of the turbine. c) Optimisation of the steam cycle is achieved through the use of a Once-through sea water condenser,	Implemented.	Noted.																										
	<table><tr><td colspan="2">Technique</td><td>Description</td></tr><tr><td>A</td><td>Combustion optimisation</td><td>See description in Optimising the combustion minimises the contaminants in the flue gas solid combustion residues</td></tr><tr><td>B</td><td>Optimisation of the working medium conditions</td><td>Operate at the pressure and temperature working medium within the constraints with, for example NOx emissions or temperature of energy demand</td></tr><tr><td>C</td><td>Optimisation of the steam cycle</td><td>Operate with lower pressure by utilisation of possible temperature condenser cooling design conditions</td></tr><tr><td>D</td><td>Minimisation of energy consumption</td><td>Minimising the consumption (e.g. of the feed-water)</td></tr><tr><td>E</td><td>Preheating of combustion air</td><td>Reuse of part of the heat from the combustion to preheat the air used</td></tr><tr><td>F</td><td>Fuel preheating</td><td>Preheating of fuel heat</td></tr><tr><td>G</td><td>Advanced control system</td><td>See description in</td></tr></table>							Technique		Description	A	Combustion optimisation	See description in Optimising the combustion minimises the contaminants in the flue gas solid combustion residues	B	Optimisation of the working medium conditions	Operate at the pressure and temperature working medium within the constraints with, for example NOx emissions or temperature of energy demand	C	Optimisation of the steam cycle	Operate with lower pressure by utilisation of possible temperature condenser cooling design conditions	D	Minimisation of energy consumption	Minimising the consumption (e.g. of the feed-water)	E	Preheating of combustion air	Reuse of part of the heat from the combustion to preheat the air used	F	Fuel preheating	Preheating of fuel heat	G	Advanced control system	See description in
	Technique							Description																							
	A	Combustion optimisation						See description in Optimising the combustion minimises the contaminants in the flue gas solid combustion residues																							
	B	Optimisation of the working medium conditions						Operate at the pressure and temperature working medium within the constraints with, for example NOx emissions or temperature of energy demand																							
	C	Optimisation of the steam cycle						Operate with lower pressure by utilisation of possible temperature condenser cooling design conditions																							
	D	Minimisation of energy consumption						Minimising the consumption (e.g. of the feed-water)																							
	E	Preheating of combustion air						Reuse of part of the heat from the combustion to preheat the air used																							
	F	Fuel preheating						Preheating of fuel heat																							
	G	Advanced control system						See description in																							

			Computerised control of the which is more the combustion parameters enables the combustion efficiency to be improved than cooling towers or						
H	Feed-water preheating using recovered heat	Preheat water coming out of the steam condenser with recovered heat, before reusing it in the boiler	air-cooled condensers. Periodic maintenance is conducted on the seawater side						
I	Heat recovery by cogeneration (CHP)	Recovery of heat (mainly from the steam system) for producing hot water/steam to be used in industrial processes/activities or in a public network for district heating. Additional heat recovery is possible from:	of the condenser to ensure cleanliness and efficiency. d) Cooling water pumps, pumps and condensate extraction pumps are variable frequency drive (VFD) operated in order to minimise energy consumption.						
J	CHP readiness	See description in Section 8.2.							
K	Flue-gas condenser	See description in Section 8.2.							
L	Heat accumulation	Heat accumulation storage in CHP mode							
M	Wet stack	See description in Section 8.2.							
N	Cooling tower discharge	The release of emissions to air through a cooling tower and not via a dedicated stack	air is not a good practice for gas turbines as it has a						

				major negative impact on power output.						
	O	Fuel pre-drying	The reduction of fuel moisture content before combustion to improve combustion conditions.	f) Natural gas is pre-heated using recovered heat from the CCGT process						
	P	Minimisation of heat losses	Minimising residual heat losses, e.g. those that occur via the slag or those that can be reduced by insulating radiating sources	CCGTs include						
	Q	Advanced materials	Use of advanced materials proven to be capable of withstanding high operating temperatures and pressures and thus to achieve increased steam/combustion process efficiencies	Steam plants 3000 plant control system						
	R	Steam turbine upgrades	This includes techniques such as increasing the temperature and pressure of medium-pressure steam, addition of a low-pressure turbine, and modifications to the geometry of the turbine rotor blades	Water coming out of the steam condenser is pre-heated						
	S	Supercritical and ultra-supercritical steam conditions	Use of a steam circuit, including steam reheating systems, in which steam can reach pressures above 220,6 bar and temperatures above 374 °C in the case of supercritical conditions, and above 250 – 300 bar and temperatures above 580 –	using heat recovered from the CCGT process. i) This technique is						

			600 °C in the case of ultra-supercritical conditions	not applicable to this CCGT installation as there is no public network of district heating.						
				j) This technique is not applicable to this existing CCGT installation. k) This technique is not applicable to this CCGT installation. l) This technique is not applicable to this CCGT installation. m) This technique is not applicable to this CCGT installation. n) This technique is not						

		<p>applicable to this CCGT installation.</p> <p>o) This technique is not applicable to this CCGT installation as natural gas is derived from a cryogenic process, which implies that fuel is dry.</p> <p>p) This technique is not applicable to this CCGT installation.</p> <p>q) Although this technique is not applicable to this existing CCGT installation, CCGT installation has Single/ unidirectional crystal on first two stages and</p>					
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		<p>ceramic coating.</p> <p>r) This technique is not applicable to this CCGT installation due to constraints of heat coming from gas turbine, and no additional firing in HRSG.</p> <p>s) This technique is not applicable to this CCGT installation as thermal rating of each CCGT is <600 MWth.</p>					
BAT 13 Water usage and emissions to water	In order to reduce water usage and the volume of contaminated waste water discharged, BAT is to use one or both of the techniques given below.		a) Not applicable as main water streams use sea water with no scope	Not applicable	Noted		
	Technique	Description					
	a. Water recycling	Residual aqueous streams, including water, from the plant are reused for various purposes. The degree of recycling is limited by the quality requirements of the recipient stream and the water balance of the plant.					

	b.	Dry bottom ash handling	Dry, hot bottom ash falls from the furnace onto a mechanical conveyor system and is cooled down by ambient air. No water is used in the process.	for a recycling process. Only applicable for solid fuels. There may be other processes for combustion products.					
				waters have been considered but their recovery and treatment for reuse has been found to not be viable. b) This technique is not applicable to this CCGT installation as LNG does not generate bottom ash.					
BAT 14		In order to prevent the contamination of uncontaminated waste water and to reduce emissions to water, BAT is to		Different wastewater streams are	Implemented	Noted, as per previous communication	The IGG was submitted as one of the variations. The	Noted, monitoring requirement for the aforementioned	Noted.

Segregation of waste water streams	segregate waste water streams and to treat them separately, depending on the pollutant content.	segregated as follows: <ul style="list-style-type: none"> Wastewater streams potentially contaminated by oil are collected in an oily-water intercept or. Hydrocarbons sensors monitor the quality of the effluent before being discharged to the sea. Storm water is collected by the storm water system, which discharges to the sea. Grey and black wastewater 		it is to be noted that the discharge from the IGG shall be included as part of the permit through a variation. In addition, kindly include such a discharge in wastewater streams identified for BAT 14.	IGG applies to the FSU and not to LCP at the D4. As such, the IGG does not fall within the scope of these BATs.	discharges will be included in the permit.	
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		<p>streams are collected separately and discharged into the municipal sewer. This is authorised through a Sewer Discharge Permit issued by Water Services Corporation.</p> <ul style="list-style-type: none">• Process wastewater generated from equipment blow down is collected in the neutralisation pit, where its pH is adjusted, before being disposed in the sea.• Waste water streams					
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		<p>that arise from periodical activities and which include drains from gas turbine compressor wash, drains within the glycol heat exchanger area as well as other wastewater streams that may be potentially contaminated are collected separately in the 'black water' pit. Samples are sent to an accredited laboratory for analyses before</p>					
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		<p>being disposed to the sewer as per parameters stipulated in the Sewer Discharge Permit.</p> <ul style="list-style-type: none"> Sea water used in the once-through sea water cooling system. Analysis of the sea water intake and outfall is carried out every 6 months. 					
	<p>Description</p> <p>Waste water streams that are typically segregated and treated include surface run-off water, cooling water, and waste water from flue-gas treatment.</p> <p>Applicability</p> <p>The applicability may be restricted in the case of existing plants due to the configuration of the drainage systems</p>						

BAT 15 Reduction of emissions to water from flue-gas treatment	In order to reduce emissions to water from flue-gas treatment, BAT is to use an appropriate combination of the techniques given below, and to use secondary techniques as close as possible to the source in order to avoid dilution.		This BAT is not applicable to this CCGT installation as flue-gas treatment is not carried out.	Not applicable	Noted.					
	<table><tr><th>Technique</th><th>Typical pollutants prevented/abated</th></tr></table>								Technique	Typical pollutants prevented/abated
	Technique	Typical pollutants prevented/abated								
	Primary techniques									
	a.	Optimised combustion (see BAT 6) and flue-gas treatment systems (e.g. SCR/SNCR, see BAT 7)							Organic compounds, ammonia (NH ₃)	
	Secondary techniques									
	b.	Adsorption on activated carbon							Organic compounds, mercury (Hg)	
	c.	Aerobic biological treatment							Biodegradable organic compounds, ammonium (NH ₄ ⁺)	
	d.	Anoxic/anaerobic biological treatment							Mercury (Hg), nitrate (NO ₃ ⁻), nitrite (NO ₂ ⁻)	
	e.	Coagulation and flocculation							Suspended solids	
	f.	Crystallisation							Metals and metalloids, sulphate (SO ₄ ²⁻), fluoride (F ⁻)	
	g.	Filtration (e.g. sand filtration, microfiltration, ultrafiltration)							Suspended solids, metals	
	h.	Flotation							Suspended solids, free oil	
	i.	Ion exchange							Metals	
	j.	Neutralisation							Acids, alkalis	
	k.	Oxidation							Sulphide (S ²⁻), sulphite (SO ₃ ²⁻)	
	l.	Precipitation							Metals and metalloids, sulphate (SO ₄ ²⁻), fluoride (F ⁻)	
m.	Sedimentation	Suspended solids								

⁵ The descriptions of the techniques are given in Section 8.6

n.	Stripping	Ammonia (NH ₃)	Generally applicable																													
<p>The BAT-AELs refer to direct discharges to a receiving water body at the point where the emission leaves the installation.</p> <p><i>Table 1</i></p> <p>BAT-AELs for direct discharges to a receiving water body from flue-gas treatment</p> <table><tr><th colspan="2">Substance/Parameter</th></tr><tr><td colspan="2">Total organic carbon (TOC)</td></tr><tr><td colspan="2">Chemical oxygen demand (COD)</td></tr><tr><td colspan="2">Total suspended solids (TSS)</td></tr><tr><td colspan="2">Fluoride (F⁻)</td></tr><tr><td colspan="2">Sulphate (SO₄²⁻)</td></tr><tr><td colspan="2">Sulphide (S²⁻), easily released</td></tr><tr><td colspan="2">Sulphite (SO₃²⁻)</td></tr><tr><td rowspan="7">Metals and metalloids</td><td>As</td></tr><tr><td>Cd</td></tr><tr><td>Cr</td></tr><tr><td>Cu</td></tr><tr><td>Hg</td></tr><tr><td>Ni</td></tr><tr><td>Pb</td></tr><tr><td>Zn</td></tr></table>			Substance/Parameter		Total organic carbon (TOC)		Chemical oxygen demand (COD)		Total suspended solids (TSS)		Fluoride (F ⁻)		Sulphate (SO ₄ ²⁻)		Sulphide (S ²⁻), easily released		Sulphite (SO ₃ ²⁻)		Metals and metalloids	As	Cd	Cr	Cu	Hg	Ni	Pb	Zn					
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	Cr																															
	Cu																															
	Hg																															
	Ni																															
	Pb																															
Zn																																
<p>(1) Either the BAT-AEL for TOC or the BAT-AEL for COD applies. TOC is the preferred option because its monitoring does not rely on the use of very toxic compounds.</p> <p>(2) This BAT-AEL applies after subtraction of the intake load.</p> <p>(3) This BAT-AEL only applies to waste water from the use of wet FGD.</p> <p>(4) This BAT-AEL only applies to combustion plants using calcium compounds in flue-gas treatment.</p> <p>(5)The higher end of the BAT-AEL range may not apply in the case of highly saline waste water (e.g. chloride concentrations ≥ 5 g/l) due to the increased solubility of calcium sulphate.</p> <p>(6) This BAT-AEL does not apply to discharges to the sea or to brackish water bodies.</p>																																

BAT 16 Waste Management	In order to reduce the quantity of waste sent for disposal from the combustion and/or gasification process and abatement techniques, BAT is to organise operations so as to maximise, in order of priority and taking into account life-cycle thinking:		Techniques a. to d. do not apply to the technology of this CCGT installation, which produces very small volumes of waste, mainly from packaging. Waste streams are separated according to the EWC codes. Waste produced is monitored and recorded in EGM-HSE-EMR-09 'Waste Register'.	Implemente d	Noted.													
	a) waste prevention, e.g. maximise the proportion of residues which arise as by-products;																	
	b) waste preparation for reuse, e.g. according to the specific requested quality criteria;																	
	c) waste recycling;																	
	d) other waste recovery (e.g. energy recovery),																	
	by implementing an appropriate combination of techniques such as:																	
	<table><tr><th>Technique</th><th>Description</th></tr><tr><td>a. Generation of gypsum as a by-product</td><td>Quality optimisation of the calcium-b reaction residues generated by the w that they can be used as a substitute gypsum (e.g. as raw material in the p industry). The quality of limestone us wet FGD influences the purity of the g produced</td></tr><tr><td>b. Recycling or recovery of residues in the construction sector</td><td>Recycling or recovery of residues (e.g. dry desulphurisation processes, fly ash) as a construction material (e.g. in building, to replace sand in concrete or in the cement industry)</td></tr><tr><td>c. Energy recovery by using waste in the fuel mix</td><td>The residual energy content of carbon and sludges generated by the combust coal, lignite, heavy fuel oil, peat or bio be recovered for example by mixing v</td></tr><tr><td>d. Preparation of spent catalyst for reuse</td><td>Preparation of catalyst for reuse (e.g. times for SCR catalysts) restores some the original performance, extending t life of the catalyst to several decades Preparation of spent catalyst for reus integrated in a catalyst management</td></tr></table>								Technique	Description	a. Generation of gypsum as a by-product	Quality optimisation of the calcium-b reaction residues generated by the w that they can be used as a substitute gypsum (e.g. as raw material in the p industry). The quality of limestone us wet FGD influences the purity of the g produced	b. Recycling or recovery of residues in the construction sector	Recycling or recovery of residues (e.g. dry desulphurisation processes, fly ash) as a construction material (e.g. in building, to replace sand in concrete or in the cement industry)	c. Energy recovery by using waste in the fuel mix	The residual energy content of carbon and sludges generated by the combust coal, lignite, heavy fuel oil, peat or bio be recovered for example by mixing v	d. Preparation of spent catalyst for reuse	Preparation of catalyst for reuse (e.g. times for SCR catalysts) restores some the original performance, extending t life of the catalyst to several decades Preparation of spent catalyst for reus integrated in a catalyst management
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d. Preparation of spent catalyst for reuse	Preparation of catalyst for reuse (e.g. times for SCR catalysts) restores some the original performance, extending t life of the catalyst to several decades Preparation of spent catalyst for reus integrated in a catalyst management																	

BAT 17 Noise emissions	In order to reduce noise emissions, BAT is to use one or a combination of the techniques given below.						
	Technique	Description	Applicability	<p>The noise generated by the operation under all operating conditions and site climatic conditions was designed to comply with EU Directive 2002/49/EC and the Maltese Directive LN 193/2004 in order to comply with the limits imposed by the environmental and personnel safety regulations. Furthermore, equipment was located accordingly such that propagation of noise on site is attenuated.</p> <p>Reduction in noise emission is</p>	<p>It is to be noted that LN 193/2004 was amended by L 426/2007 and LN 366 of 2018. (S.L. 549.37). No additional comments with respect the applied techniques. With respect to b) and c) it is to be noted that this may be considered as applicable solutions in the event of noise issue emanate from the plant.</p>	Noted.	
	a) Operational measures	<p>These include:</p> <ul style="list-style-type: none"> –improved inspection and maintenance of equipment –closing of doors and windows of enclosed areas, if possible –equipment operated by experienced staff –avoidance of noisy activities at night, if possible –provisions for noise control during maintenance activities 	Generally applicable				
	b) Low-noise equipment	This potentially includes compressors, pumps and disks	Generally applicable when the equipment is new or replaced				
	c) Noise attenuation	Noise propagation can be reduced by inserting obstacles between the emitter and the receiver. Appropriate obstacles include protection walls, embankments and buildings	Generally applicable to new plants. In the case of existing plants, the insertion of obstacles may be restricted by lack of space				

	Noise-control equipment	<p>This includes:</p> <ul style="list-style-type: none">— noise-reducers— equipment insulation— enclosure of noisy equipment— soundproofing of buildings	<p>The applicability may be restricted by lack of space</p>	<p>achieved through a scheduled maintenance and inspection plan covered by the LTSA with the OEM and also through the implementation of the following techniques:</p>					
	Appropriate location of equipment and buildings	<p>Noise levels can be reduced by increasing the distance between the emitter and the receiver and by using buildings as noise screens</p>	<p>Generally applicable to new plants. In the case of existing plants, the relocation of equipment and production units may be restricted by lack of space or by excessive costs</p>	<p>a) i. Operational measures including inspection and maintenance of equipment covered by LTSA with OEM. ii. Closing of doors and windows of enclosed areas; iii.</p>					

		<p>Equipment is operated by fully competent staff;</p> <p>iv. Avoidance of noisy activities at night</p> <p>v. Provision of the necessary PPE for noise control</p> <p>b) Not applicable to an existing plant.</p> <p>c) Not applicable to an existing plant.</p> <p>d) Noisy equipment is</p>					
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		<p>install ed in appro priate acoust ic enclos ures to contro l noise levels.</p> <p>e) As above.</p>					
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2. BAT CONCLUSIONS FOR COMBUSTIONS OF SOLID FUELS

2.1 BAT conclusions for the combustion of coal and/or lignite

Unless otherwise stated, the BAT conclusions presented in this section are generally applicable to the combustion of coal and/or lignite. They apply in addition to the general BAT conclusions given in Section 1.

BAT conclusion			STATUS AT INSTALLATION: [ENTER NAME OF OPERATOR]	STATE WHETHER IT IS IN PLACE OR STATE SCHEDULE FOR IMPLEMENTATION					
			DATE: [ENTER DATE OF ASSESSMENT]						
			Applicability Assessment (describe how the technique applies or not to your installation)						
BAT 18 General environmental performance	In order to improve the general environmental performance of the combustion of coal and/or lignite, and in addition to BAT 6, BAT is to use the technique given below.		N/A	N/A					
	<table><tr><th colspan="2">Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a.</td><td>Integrated combustion process ensuring high boiler efficiency and including primary techniques for NO_x reduction (e.g. air staging, fuel staging, low-NO_x burners (LNB) and/or flue-gas recirculation)</td><td>Combustion processes such as pulverised combustion, fluidised bed combustion or moving grate firing allow this integration</td><td>Generally applicable</td></tr></table>				Technique		Description	Applicability	a.
Technique		Description	Applicability						
a.	Integrated combustion process ensuring high boiler efficiency and including primary techniques for NO _x reduction (e.g. air staging, fuel staging, low-NO _x burners (LNB) and/or flue-gas recirculation)	Combustion processes such as pulverised combustion, fluidised bed combustion or moving grate firing allow this integration	Generally applicable						
BAT 19 Energy efficiency	In order to increase the energy efficiency of the combustion of coal and/or lignite, BAT is to use an appropriate combination of the techniques given in BAT 12 and below.		N/A	N/A					
	<table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a.</td><td>Dry bottom ash handling</td><td>Dry hot bottom ash falls from the furnace onto a mechanical conveyor system and, after redirection to the furnace for reburning, is cooled down by ambient air. Useful energy is recovered from both the ash reburning and ash cooling</td><td>There may be technical restrictions that prevent retrofitting to existing combust</td></tr></table> <i>Table 2</i>				Technique	Description	Applicability	a.	Dry bottom ash handling
Technique	Description	Applicability							
a.	Dry bottom ash handling	Dry hot bottom ash falls from the furnace onto a mechanical conveyor system and, after redirection to the furnace for reburning, is cooled down by ambient air. Useful energy is recovered from both the ash reburning and ash cooling	There may be technical restrictions that prevent retrofitting to existing combust						

	<div>BAT-associated energy efficiency levels (BAT-AEELs) for coal and/or lignite combustion</div> <table><tr><th rowspan="3">Type of combustion unit</th><th colspan="3">BAT-AEELs ⁽¹⁾⁽²⁾</th></tr><tr><th colspan="2">Net electrical efficiency (%) ⁽³⁾</th><th>Net total fuel utilisation (%) ⁽³⁾⁽⁴⁾⁽⁵⁾</th></tr><tr><th>New unit ⁽⁶⁾⁽⁷⁾</th><th>Existing unit ⁽⁶⁾⁽⁸⁾</th><th>New or existing unit</th></tr><tr><td>Coal-fired, ≥ 1 000 MW_{th}</td><td>45 – 46</td><td>33,5 – 44</td><td>75 – 97</td></tr><tr><td>Lignite-fired, ≥ 1 000 MW_{th}</td><td>42 – 44 ⁽⁹⁾</td><td>33,5 – 42,5</td><td>75 – 97</td></tr><tr><td>Coal-fired, < 1 000 MW_{th}</td><td>36,5 – 41,5 ⁽¹⁰⁾</td><td>32,5 – 41,5</td><td>75 – 97</td></tr><tr><td>Lignite-fired, < 1 000 MW_{th}</td><td>36,5 – 40 ⁽¹¹⁾</td><td>31,5 – 39,5</td><td>75 – 97</td></tr></table> <div>(1) These BAT-AEELs do not apply in the case of units operated < 1 500 h/yr.</div> <div>(2) In the case of CHP units, only one of the two BAT-AEELs ‘Net electrical efficiency’ or ‘Net total fuel utilisation’ applies, depending on the CHP unit design (i.e. either more oriented towards electricity generation or towards heat generation).</div> <div>(3) The lower end of the range may correspondent to cases where the achieved energy efficiency is negatively affected (up to four percentage points) by the type of cooling system used or the geographical location of the unit.</div> <div>(4) These levels may not be achievable if the potential heat demand is too low.</div> <div>(5) These BAT-AEELs do not apply to plants generating only electricity.</div> <div>(6) The lower ends of the BAT-AEEL ranges are achieved in the case of unfavourable climatic conditions, low-grade lignite- fired units, and/or old units (first commissioned before 1985).</div> <div>(7) The higher end of the BAT-AEEL range can be achieved with high steam parameters (pressure, temperature).</div> <div>(8)The achievable electrical efficiency improvement depends on the specific unit, but an increase of more than three percentage points is considered as reflecting the use of BAT for existing units, depending on the original design of the unit and on the retrofits already performed.</div> <div>(9) In the case of units burning lignite with a lower heating value below 6 MJ/kg, the lower end of the BAT-AEEL range is 41,5 %.</div> <div>(10) The higher end of the BAT-AEEL range may be up to 46 % in the case of units of ≥ 600 MWth using supercritical or ultra-supercritical steam conditions.</div> <div>(11) The higher end of the BAT-AEEL range may be up to 44 % in the case of units of ≥ 600 MWth using supercritical or ultra-supercritical steam conditions.</div>	Type of combustion unit	BAT-AEELs ⁽¹⁾⁽²⁾			Net electrical efficiency (%) ⁽³⁾		Net total fuel utilisation (%) ⁽³⁾⁽⁴⁾⁽⁵⁾	New unit ⁽⁶⁾⁽⁷⁾	Existing unit ⁽⁶⁾⁽⁸⁾	New or existing unit	Coal-fired, ≥ 1 000 MW _{th}	45 – 46	33,5 – 44	75 – 97	Lignite-fired, ≥ 1 000 MW _{th}	42 – 44 ⁽⁹⁾	33,5 – 42,5	75 – 97	Coal-fired, < 1 000 MW _{th}	36,5 – 41,5 ⁽¹⁰⁾	32,5 – 41,5	75 – 97	Lignite-fired, < 1 000 MW _{th}	36,5 – 40 ⁽¹¹⁾	31,5 – 39,5	75 – 97		
Type of combustion unit	BAT-AEELs ⁽¹⁾⁽²⁾																												
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	New unit ⁽⁶⁾⁽⁷⁾	Existing unit ⁽⁶⁾⁽⁸⁾	New or existing unit																										
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Lignite-fired, < 1 000 MW _{th}	36,5 – 40 ⁽¹¹⁾	31,5 – 39,5	75 – 97																										
<div>BAT 20</div> <div>NO_x, N₂O and CO emissions to air</div>	<div>In order to prevent or reduce NO_x emissions to air while limiting CO and N₂O emissions to air from the combustion of coal and/or lignite, BAT is to use one or a combination of the techniques given below.</div> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Combustion optimisation</td><td>See description in Section 8.3.</td><td>Generally applicable</td></tr></table>	Technique	Description	Applicability	a. Combustion optimisation	See description in Section 8.3.	Generally applicable	N/A	N/A																				
Technique	Description	Applicability																											
a. Combustion optimisation	See description in Section 8.3.	Generally applicable																											

		Generally used in combination with other techniques	
b. Combination of other primary techniques for NO _x reduction (e.g. air staging, fuel staging, flue-gas recirculation, low-NO _x burners (LNB))	See description in Section 8.3 for each single technique. The choice and performance of (an) appropriate (combination of) primary techniques may be influenced by the boiler design		
c. Selective non-catalytic reduction (SNCR)	See description in Section 8.3. Can be applied with 'slip' SCR	The applicability may be limited in the case of boilers with a high cross-sectional area preventing homogeneous mixing of NH ₃ and NO _x . The applicability may be limited in the case of combustion plants operated < 1 500 h/yr with highly variable boiler loads	
d. Selective catalytic reduction (SCR)	See description in Section 8.3	Not applicable to combustion plants of < 300 MW _{th} operated < 500 h/yr. Not generally applicable to combustion plants of < 100 MW _{th} . There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr and for existing combustion plants of ≥ 300 MW _{th} operated < 500 h/yr	
e. Combined techniques for NO _x and SO _x reduction	See description in Section 8.3	Applicable on a case-by-case basis, depending on the fuel characteristics and combustion process	

Table 3

BAT-associated emission levels (BAT-AELs) for NO_x emissions to air from the combustion of coal and/or lignite

Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)			
	Yearly average		Daily average or average over the sampling period	
	New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾⁽³⁾

	<table><tr><td>< 100</td><td>100–150</td><td>100–270</td><td>155–200</td><td>165–330</td></tr><tr><td>100–300</td><td>50–100</td><td>100–180</td><td>80–130</td><td>155–210</td></tr><tr><td>≥ 300, FBC boiler combusting coal and/or lignite and lignite-fired PC boiler</td><td>50 – 85</td><td>< 85 – 150 ⁽⁴⁾⁽⁵⁾</td><td>80 – 125</td><td>140 – 165 ⁽⁶⁾</td></tr><tr><td>≥ 300, coal-fired PC boiler</td><td>65 – 85</td><td>65 – 150</td><td>80 – 125</td><td>< 85 – 165 ⁽⁷⁾</td></tr></table> <p>(1) These BAT-AELs do not apply to plants operated < 1 500 h/yr.</p> <p>(2) In the case of coal-fired PC boiler plants put into operation no later than 1 July 1987, which are operated < 1 500 h/yr and for which SCR and/or SNCR is not applicable, the higher end of the range is 340 mg/Nm3.</p> <p>(3) For plants operated < 500 h/yr, these levels are indicative.</p> <p>(4) The lower end of the range is considered achievable when using SCR.</p> <p>(5) The higher end of the range is 175 mg/Nm3 for FBC boilers put into operation no later than 7 January 2014 and for lignite-fired PC boilers.</p> <p>(6) The higher end of the range is 220 mg/Nm3 for FBC boilers put into operation no later than 7 January 2014 and for lignite-fired PC boilers.</p> <p>(7) In the case of plants put into operation no later than 7 January 2014, the higher end of the range is 200 mg/Nm3 for plants operated ≥ 1 500 h/yr, and 220 mg/Nm3 for plants operated < 1 500 h/yr.</p> <p>As an indication, the yearly average CO emission levels for existing combustion plants operated ≥ 1 500 h/yr or for new combustion plants will generally be as follows:</p> <table><tr><th>Combustion plant total rated thermal input (MW_{th})</th><th>CO indicative emission level (mg/Nm³)</th></tr><tr><td>< 300</td><td>< 30–140</td></tr><tr><td>≥ 300, FBC boiler combusting coal and/or lignite and lignite-fired PC boiler</td><td>< 30–100 ⁽¹⁾</td></tr><tr><td>≥ 300, coal-fired PC boiler</td><td>< 5–100 ⁽¹⁾</td></tr></table> <p>(1) The higher end of the range may be up to 140 mg/Nm3 in the case of limitations due to boiler design, and/or in the case of fluidised bed boilers not fitted with secondary abatement techniques for NOX emissions reduction.</p>	< 100	100–150	100–270	155–200	165–330	100–300	50–100	100–180	80–130	155–210	≥ 300, FBC boiler combusting coal and/or lignite and lignite-fired PC boiler	50 – 85	< 85 – 150 ⁽⁴⁾⁽⁵⁾	80 – 125	140 – 165 ⁽⁶⁾	≥ 300, coal-fired PC boiler	65 – 85	65 – 150	80 – 125	< 85 – 165 ⁽⁷⁾	Combustion plant total rated thermal input (MW _{th})	CO indicative emission level (mg/Nm ³)	< 300	< 30–140	≥ 300, FBC boiler combusting coal and/or lignite and lignite-fired PC boiler	< 30–100 ⁽¹⁾	≥ 300, coal-fired PC boiler	< 5–100 ⁽¹⁾		
< 100	100–150	100–270	155–200	165–330																											
100–300	50–100	100–180	80–130	155–210																											
≥ 300, FBC boiler combusting coal and/or lignite and lignite-fired PC boiler	50 – 85	< 85 – 150 ⁽⁴⁾⁽⁵⁾	80 – 125	140 – 165 ⁽⁶⁾																											
≥ 300, coal-fired PC boiler	65 – 85	65 – 150	80 – 125	< 85 – 165 ⁽⁷⁾																											
Combustion plant total rated thermal input (MW _{th})	CO indicative emission level (mg/Nm ³)																														
< 300	< 30–140																														
≥ 300, FBC boiler combusting coal and/or lignite and lignite-fired PC boiler	< 30–100 ⁽¹⁾																														
≥ 300, coal-fired PC boiler	< 5–100 ⁽¹⁾																														
BAT 21 SO_x, HCl and HF emissions to air	<p>In order to prevent or reduce SO_x, HCl and HF emissions to air from the combustion of coal and/or lignite, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Boiler sorbent injection (in-furnace or in-bed)</td><td>See description in Section 8.4</td><td rowspan="5">Generally applicable</td></tr><tr><td>b. Duct sorbent injection (DSI)</td><td>See description in Section 8.4. The technique can be used for HCl/HF removal when no specific FGD end-of-pipe technique is implemented</td></tr><tr><td>c. Spray dry absorber (SDA)</td><td rowspan="2">See description in Section 8.4</td></tr><tr><td>d. Circulating fluidised bed (CFB) dry scrubber</td></tr><tr><td>e. Wet scrubbing</td><td>See description in Section 8.4.</td></tr></table>	Technique	Description	Applicability	a. Boiler sorbent injection (in-furnace or in-bed)	See description in Section 8.4	Generally applicable	b. Duct sorbent injection (DSI)	See description in Section 8.4. The technique can be used for HCl/HF removal when no specific FGD end-of-pipe technique is implemented	c. Spray dry absorber (SDA)	See description in Section 8.4	d. Circulating fluidised bed (CFB) dry scrubber	e. Wet scrubbing	See description in Section 8.4.	N/A	N/A															
Technique	Description	Applicability																													
a. Boiler sorbent injection (in-furnace or in-bed)	See description in Section 8.4	Generally applicable																													
b. Duct sorbent injection (DSI)	See description in Section 8.4. The technique can be used for HCl/HF removal when no specific FGD end-of-pipe technique is implemented																														
c. Spray dry absorber (SDA)	See description in Section 8.4																														
d. Circulating fluidised bed (CFB) dry scrubber																															
e. Wet scrubbing	See description in Section 8.4.																														

		The techniques can be used for HCl/HF removal when no specific FGD end-of-pipe technique is implemented	
f. Wet flue-gas desulphurisation (wet FGD)	See description in Section 8.4	Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for applying the technique to combustion plants of < 300 MW _{th} , and for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr	Applicable on a case-by-case basis, depending on the fuel characteristics and combustion process
g. Seawater FGD			
h. Combined techniques for NO _x and SO _x reduction			
i. Replacement or removal of the gas-gas heater located downstream of the wet FGD	Replacement of the gas-gas heater downstream of the wet FGD by a multi-pipe heat extractor, or removal and discharge of the flue-gas via a cooling tower or a wet stack	Only applicable when the heat exchanger needs to be changed or replaced in combustion plants fitted with wet FGD and a downstream gas-gas heater	
j. Fuel choice	See description in Section 8.4. Use of fuel with low sulphur (e.g. down to 0,1 wt-%, dry basis), chlorine or fluorine content	Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State. The applicability may be limited due to design constraints in the case of combustion plants combusting highly specific indigenous fuels	

Table 4

BAT-associated emission levels (BAT-AELs) for SO₂ emissions to air from the combustion of coal and/or lignite

Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)			
	Yearly average		Daily average	Daily average or average over the sampling period ⁽²⁾
	New plant	Existing plant ⁽¹⁾	New plant	Existing plant
< 100	150–200	150–360	170–220	170–400
100–300	80–150	95–200	135–200	135–220 ⁽³⁾
≥ 300, PC boiler	10–75	10–130 ⁽⁴⁾	25–110	25–165 ⁽⁵⁾
≥ 300, Fluidised bed boiler	20–75	20–180	25–110	50–220

(1) These BAT-AELs do not apply to plants operated < 1 500 h/yr.

(2) For plants operated < 500 h/yr, these levels are indicative.

(3) In the case of plants put into operation no later than 7 January 2014, the upper end of the BAT-AEL range is 250 mg/Nm³.

(4) The lower end of the range can be achieved with the use of low-sulphur fuels in combination with the most advanced wet abatement system designs.

	<p>(5) The higher end of the BAT-AEL range is 220 mg/Nm³ in the case of plants put into operation no later than 7 January 2014 and operated < 1 500 h/yr. For other existing plants put into operation no later than 7 January 2014, the higher end of the BAT-AEL range is 205 mg/Nm³.</p> <p>(6) For circulating fluidised bed boilers, the lower end of the range can be achieved by using high-efficiency wet FGD. The higher end of the range can be achieved by using boiler in-bed sorbent injection.</p> <p>For a combustion plant with a total rated thermal input of more than 300 MW, which is specifically designed to fire indigenous lignite fuels and which can demonstrate that it cannot achieve the BAT-AELs mentioned in Table 4 for techno-economic reasons, the daily average BAT-AELs set out in Table 4 do not apply, and the upper end of the yearly average BAT-AEL range is as follows:</p> <p>(i) for a new FGD system: RCG × 0,01 with a maximum of 200 mg/Nm³;</p> <p>(ii) for an existing FGD system: RCG × 0,03 with a maximum of 320 mg/Nm³; in which RCG represents the concentration of SO₂ in the raw flue-gas as a yearly average (under the standard conditions given under General considerations) at the inlet of the SO_x abatement system, expressed at a reference oxygen content of 6 vol- % O₂.</p> <p>(iii) If boiler sorbent injection is applied as part of the FGD system, the RCG may be adjusted by taking into account the SO₂ reduction efficiency of this technique (η_{BSI}), as follows: RCG (adjusted) = RCG (measured)/(1-η_{BSI}).</p> <p style="text-align: center;"><i>Table 5</i></p> <p>BAT-associated emission levels (BAT-AELs) for HCl and HF emissions to air from the combustion of coal and/or lignite</p> <table><tr><th rowspan="3">Pollutant</th><th rowspan="3">Combustion plant total rated thermal input (MW_{th})</th><th colspan="2">BAT-AELs (mg/Nm³)</th></tr><tr><th colspan="2">Yearly average or average of samples obtained during one year</th></tr><tr><th>New plant</th><th>Existing plant ⁽¹⁾</th></tr><tr><td rowspan="2">HCl</td><td>< 100</td><td>1–6</td><td>2–10 ⁽²⁾</td></tr><tr><td>≥ 100</td><td>1–3</td><td>1–5 ⁽²⁾⁽³⁾</td></tr><tr><td rowspan="2">HF</td><td>< 100</td><td>< 1–3</td><td>< 1–6 ⁽⁴⁾</td></tr><tr><td>≥ 100</td><td>< 1–2</td><td>< 1–3 ⁽⁴⁾</td></tr></table> <p>(1)The lower end of these BAT-AEL ranges may be difficult to achieve in the case of plants fitted with wet FGD and a downstream gas-gas heater.</p> <p>(2) The higher end of the BAT-AEL range is 20 mg/Nm3 in the following cases: plants combusting fuels where the average chlorine content is 1 000 mg/kg (dry) or higher; plants operated < 1 500 h/yr; FBC boilers. For plants operated < 500 h/yr, these levels are indicative.</p> <p>(3) In the case of plants fitted with wet FGD with a downstream gas-gas heater, the higher end of the BAT-AEL range is 7 mg/Nm3.</p> <p>(4) The higher end of the BAT-AEL range is 7 mg/Nm3 in the following cases: plants fitted with wet FGD with a downstream gas-gas heater; plants operated < 1 500 h/yr; FBC boilers. For plants operated < 500 h/yr, these levels are indicative.</p>	Pollutant	Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)		Yearly average or average of samples obtained during one year		New plant	Existing plant ⁽¹⁾	HCl	< 100	1–6	2–10 ⁽²⁾	≥ 100	1–3	1–5 ⁽²⁾⁽³⁾	HF	< 100	< 1–3	< 1–6 ⁽⁴⁾	≥ 100	< 1–2	< 1–3 ⁽⁴⁾		
Pollutant	Combustion plant total rated thermal input (MW _{th})			BAT-AELs (mg/Nm ³)																					
				Yearly average or average of samples obtained during one year																					
		New plant	Existing plant ⁽¹⁾																						
HCl	< 100	1–6	2–10 ⁽²⁾																						
	≥ 100	1–3	1–5 ⁽²⁾⁽³⁾																						
HF	< 100	< 1–3	< 1–6 ⁽⁴⁾																						
	≥ 100	< 1–2	< 1–3 ⁽⁴⁾																						
BAT 22 Dust and particulate-bound metal emissions to air	<p>In order to reduce dust and particulate-bound metal emissions to air from the combustion of coal and/or lignite, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Electrostatic precipitator (ESP)</td><td rowspan="2">See description in Section 8.5</td><td rowspan="3">Generally applicable</td></tr><tr><td>b. Bag filter</td></tr><tr><td>c. Boiler sorbent injection</td><td>See descriptions in Section 8.5.</td></tr></table>	Technique	Description	Applicability	a. Electrostatic precipitator (ESP)	See description in Section 8.5	Generally applicable	b. Bag filter	c. Boiler sorbent injection	See descriptions in Section 8.5.	N/A	N/A													
Technique	Description	Applicability																							
a. Electrostatic precipitator (ESP)	See description in Section 8.5	Generally applicable																							
b. Bag filter																									
c. Boiler sorbent injection	See descriptions in Section 8.5.																								

	<table><tr><td></td><td>(in-furnace or in-bed)</td><td rowspan="3">The techniques are mainly used for SO_x, HCl and/or HF control</td><td rowspan="3">See applicability in BAT 21</td></tr><tr><td>d.</td><td>Dry or semi-dry FGD system</td></tr><tr><td>e.</td><td>Wet flue-gas desulphurisation (wet FGD)</td></tr></table>		(in-furnace or in-bed)	The techniques are mainly used for SO _x , HCl and/or HF control	See applicability in BAT 21	d.	Dry or semi-dry FGD system	e.	Wet flue-gas desulphurisation (wet FGD)																														
		(in-furnace or in-bed)	The techniques are mainly used for SO _x , HCl and/or HF control			See applicability in BAT 21																																	
	d.	Dry or semi-dry FGD system																																					
	e.	Wet flue-gas desulphurisation (wet FGD)																																					
	<p style="text-align: center;">Table 6</p> <p>BAT-associated emission levels (BAT-AELs) for dust emissions to air from the combustion of coal and/or lignite</p> <table><tr><td rowspan="3">Combustion plant total rated thermal input (MW_{th})</td><td colspan="4">BAT-AELs (mg/Nm³)</td></tr><tr><td colspan="2">Yearly average</td><td colspan="2">Daily average or average over the sampling period</td></tr><tr><td>New plant</td><td>Existing plant ⁽¹⁾</td><td>New plant</td><td>Existing plant ⁽²⁾</td></tr><tr><td>< 100</td><td>2–5</td><td>2–18</td><td>4–16</td><td>4–22 ⁽³⁾</td></tr><tr><td>100–300</td><td>2–5</td><td>2–14</td><td>3–15</td><td>4–22 ⁽⁴⁾</td></tr><tr><td>300–1 000</td><td>2–5</td><td>2–10 ⁽⁵⁾</td><td>3–10</td><td>3–11 ⁽⁶⁾</td></tr><tr><td>≥ 1 000</td><td>2–5</td><td>2–8</td><td>3–10</td><td>3–11 ⁽⁷⁾</td></tr></table> <p>(1) These BAT-AELs do not apply to plants operated < 1 500 h/yr. (2) For plants operated < 500 h/yr, these levels are indicative. (3) The higher end of the BAT-AEL range is 28 mg/Nm3 for plants put into operation no later than 7 January 2014. (4) The higher end of the BAT-AEL range is 25 mg/Nm3 for plants put into operation no later than 7 January 2014. (5) The higher end of the BAT-AEL range is 12 mg/Nm3 for plants put into operation no later than 7 January 2014. (6) The higher end of the BAT-AEL range is 20 mg/Nm3 for plants put into operation no later than 7 January 2014. (7) The higher end of the BAT-AEL range is 14 mg/Nm3 for plants put into operation no later than 7 January 2014.</p>				Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)				Yearly average		Daily average or average over the sampling period		New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾	< 100	2–5	2–18	4–16	4–22 ⁽³⁾	100–300	2–5	2–14	3–15	4–22 ⁽⁴⁾	300–1 000	2–5	2–10 ⁽⁵⁾	3–10	3–11 ⁽⁶⁾	≥ 1 000	2–5	2–8	3–10	3–11 ⁽⁷⁾		
	Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)																																					
		Yearly average		Daily average or average over the sampling period																																			
		New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾																																		
	< 100	2–5	2–18	4–16	4–22 ⁽³⁾																																		
	100–300	2–5	2–14	3–15	4–22 ⁽⁴⁾																																		
300–1 000	2–5	2–10 ⁽⁵⁾	3–10	3–11 ⁽⁶⁾																																			
≥ 1 000	2–5	2–8	3–10	3–11 ⁽⁷⁾																																			
BAT 23																																							
Mercury emissions to air	<p>In order to prevent or reduce mercury emissions to air from the combustion of coal and/or lignite, BAT is to use one or a combination of the techniques given below.</p> <table><tr><td>Technique</td><td>Description</td><td>Applicability</td></tr><tr><td colspan="3">Co-benefit from techniques primarily used to reduce emissions of other pollutants</td></tr><tr><td>a. Electrostatic precipitator (ESP)</td><td>See description in Section 8.5. Higher mercury removal efficiency is achieved at flue-gas temperatures below 130 °C. The technique is mainly used for dust control</td><td rowspan="3">Generally applicable</td></tr><tr><td>b. Bag filter</td><td>See description in Section 8.5. The technique is mainly used for dust control</td></tr><tr><td>c. Dry or semi-dry FGD system</td><td>See descriptions in Section 8.5.</td></tr><tr><td>d. Wet flue-gas desulphurisation (wet FGD)</td><td>The techniques are mainly used for SO_x, HCl and/or HF control</td><td>See applicability in BAT 21</td></tr><tr><td>e. Selective catalytic reduction (SCR)</td><td>See description in Section 8.3. Only used in combination with other techniques to enhance or reduce the</td><td>See applicability in BAT 20</td></tr></table>	Technique	Description	Applicability	Co-benefit from techniques primarily used to reduce emissions of other pollutants			a. Electrostatic precipitator (ESP)	See description in Section 8.5. Higher mercury removal efficiency is achieved at flue-gas temperatures below 130 °C. The technique is mainly used for dust control	Generally applicable	b. Bag filter	See description in Section 8.5. The technique is mainly used for dust control	c. Dry or semi-dry FGD system	See descriptions in Section 8.5.	d. Wet flue-gas desulphurisation (wet FGD)	The techniques are mainly used for SO _x , HCl and/or HF control	See applicability in BAT 21	e. Selective catalytic reduction (SCR)	See description in Section 8.3. Only used in combination with other techniques to enhance or reduce the	See applicability in BAT 20	N/A	N/A																	
Technique	Description	Applicability																																					
Co-benefit from techniques primarily used to reduce emissions of other pollutants																																							
a. Electrostatic precipitator (ESP)	See description in Section 8.5. Higher mercury removal efficiency is achieved at flue-gas temperatures below 130 °C. The technique is mainly used for dust control	Generally applicable																																					
b. Bag filter	See description in Section 8.5. The technique is mainly used for dust control																																						
c. Dry or semi-dry FGD system	See descriptions in Section 8.5.																																						
d. Wet flue-gas desulphurisation (wet FGD)	The techniques are mainly used for SO _x , HCl and/or HF control	See applicability in BAT 21																																					
e. Selective catalytic reduction (SCR)	See description in Section 8.3. Only used in combination with other techniques to enhance or reduce the	See applicability in BAT 20																																					

		mercury oxidation before capture in a subsequent FGD or dedusting system. The technique is mainly used for NO _x control			
Specific techniques to reduce mercury emissions					
f.	Carbon sorbent (e.g. activated carbon or halogenated activated carbon) injection in the flue-gas	See description in Section 8.5. Generally used in combination with an ESP/bag filter. The use of this technique may require additional treatment steps to further segregate the mercury-containing carbon fraction prior to further reuse of the fly ash	Generally applicable		
g.	Use of halogenated additives in the fuel or injected in the furnace	See description in Section 8.5	Generally applicable in the case of a low halogen content in the fuel		
h.	Fuel pretreatment	Fuel washing, blending and mixing in order to limit/reduce the mercury content or improve mercury capture by pollution control equipment	Applicability is subject to a previous survey for characterising the fuel and for estimating the potential effectiveness of the technique		
i.	Fuel choice	See description in Section 8.5	Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State		
Table 7					
BAT-associated emission levels (BAT-AELs) for mercury emissions to air from the combustion of coal and lignite					
Combustion plant total rated thermal input (MW _{th})		BAT-AELs (µg/Nm ³)			
		Yearly average or average of samples obtained during one year			
		New plant		Existing plant ⁽¹⁾	
		Coal	lignite	coal	lignite
< 300		< 1–3	< 1–5	< 1–9	< 1–10
≥ 300		< 1–2	< 1–4	< 1–4	< 1–7
(1) The lower end of the BAT-AEL range can be achieved with specific mercury abatement techniques.					

2.2 BAT conclusions for the combustion of solid biomass and/or peat

Unless otherwise stated, the BAT conclusions presented in this section are generally applicable to the combustion of solid biomass and/or peat. They apply in addition to the general BAT conclusions given in Section 1

Bat conclusions					STATUS AT INSTALLATION: [ENTER NAME OF OPERATOR]		STATE WHETHER IT IS IN PLACE OR STATE SCHEDULE FOR IMPLEMENTATION			
					DATE: [ENTER DATE OF ASSESSMENT]					
					Applicability Assessment (describe how the technique applies or not to your installation)					
Energy efficiency	<i>Table 8</i> BAT-associated energy efficiency levels (BAT-AEELs) for the combustion of solid biomass and/or peat				N/A		N/A			
	Type of combustion unit		BAT-AEELs							
			Net electrical efficiency (%)						Net total fuel utilisation (%)	
			New unit						Existing unit	
	Solid biomass and/or peat boiler		33,5–to > 38						28–38	
BAT 24 NO _x , N ₂ O and CO emissions to air	In order to prevent or reduce NO _x emissions to air while limiting CO and N ₂ O emissions to air from the combustion of solid biomass and/or peat, BAT is to use one or a combination of the techniques given below.				N/A		N/A			
	Technique		Description						Applicability	
	a.	Combustion optimisation	See descriptions in Section 8.3						Generally applicable	
	b.	Low-NO _x burners (LNB)								
	c.	Air staging								
	d.	Fuel staging								
	e.	Flue-gas recirculation								

f. Selective non-catalytic reduction (SNCR)	See description in Section 8.3. Can be applied with 'slip' SCR	Not applicable to combustion plants operated < 500 h/yr with highly variable boiler loads. The applicability may be limited in the case of combustion plants operated between 500 h/yr and 1 500 h/yr with highly variable boiler loads. For existing combustion plants, applicable within the constraints associated with the required temperature window and residence time for the injected reactants
g. Selective catalytic reduction (SCR)	See description in Section 8.3. The use of high-alkali fuels (e.g. straw) may require the SCR to be installed downstream of the dust abatement system	Not applicable to combustion plants operated < 500 h/yr. There may be economic restrictions for retrofitting existing combustion plants of < 300 MW _{th} . Not generally applicable to existing combustion plants of < 100 MW _{th}

Table 9

BAT-associated emission levels (BAT-AELs) for NO_x emissions to air from the combustion of solid biomass and/or peat

Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)			
	Yearly average		Daily average or average over the sampling period	
	New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾
50–100	70–150 ⁽³⁾	70–225 ⁽⁴⁾	120–200 ⁽⁵⁾	120–275 ⁽⁶⁾
100–300	50–140	50–180	100–200	100–220
≥ 300	40–140	40–150 ⁽⁷⁾	65–150	95–165 ⁽⁸⁾

(1) These BAT-AELs do not apply to plants operated < 1 500 h/yr. (

2) For combustion plants operated < 500 h/yr, these levels are indicative.

(3) For plants burning fuels where the average potassium content is 2 000 mg/kg (dry) or higher, and/or the average sodium content is 300 mg/kg or higher, the higher end of the BAT-AEL range is 200 mg/Nm³.

(4) For plants burning fuels where the average potassium content is 2 000 mg/kg (dry) or higher, and/or the average sodium content is 300 mg/kg or higher, the higher end of the BAT-AEL range is 250 mg/Nm³.

(5) For plants burning fuels where the average potassium content is 2 000 mg/kg (dry) or higher, and/or the average sodium content is 300 mg/kg or higher, the higher end of the BAT-AEL range is 260 mg/Nm³.

	<p>(6) For plants put into operation no later than 7 January 2014 and burning fuels where the average potassium content is 2 000 mg/kg (dry) or higher, and/or the average sodium content is 300 mg/kg or higher, the higher end of the BAT-AEL range is 310 mg/Nm3.</p> <p>(7) The higher end of the BAT-AEL range is 160 mg/Nm3 for plants put into operation no later than 7 January 2014.</p> <p>(8) The higher end of the BAT-AEL range is 200 mg/Nm3 for plants put into operation no later than 7 January 2014.</p> <p>As an indication, the yearly average CO emission levels will generally be:</p> <p>— < 30–250 mg/Nm³ for existing combustion plants of 50–100 MW_{th} operated ≥ 1 500 h/yr, or new combustion plants of 50–100 MW_{th},</p> <p>— < 30–160 mg/Nm³ for existing combustion plants of 100–300 MW_{th} operated ≥ 1 500 h/yr, or new combustion plants of 100–300 MW_{th},</p> <p>— < 30–80 mg/Nm³ for existing combustion plants of ≥ 300 MW_{th} operated ≥ 1 500 h/yr, or new combustion plants of ≥ 300 MW_{th}.</p>																						
BAT 25 SO_x, HCl and HF emissions to air	<p>In order to prevent or reduce SO_x, HCl and HF emissions to air from the combustion of solid biomass and/or peat, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Boiler sorbent injection (in-furnace or in-bed)</td><td rowspan="6">See descriptions in Section 8.4</td><td rowspan="6">Generally applicable</td></tr><tr><td>b. Duct sorbent injection (DSI)</td></tr><tr><td>c. Spray dry absorber (SDA)</td></tr><tr><td>d. Circulating fluidised bed (CFB) dry scrubber</td></tr><tr><td>e. Wet scrubbing</td></tr><tr><td>f. Flue-gas condenser</td></tr><tr><td>g. Wet flue-gas desulphurisation (wet FGD)</td><td></td><td>Not applicable to combustion plants operated < 500 h/yr.</td></tr><tr><td></td><td></td><td>There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr</td></tr><tr><td>h. Fuel choice</td><td></td><td>Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State</td></tr></table> <p><i>Table 10</i></p>	Technique	Description	Applicability	a. Boiler sorbent injection (in-furnace or in-bed)	See descriptions in Section 8.4	Generally applicable	b. Duct sorbent injection (DSI)	c. Spray dry absorber (SDA)	d. Circulating fluidised bed (CFB) dry scrubber	e. Wet scrubbing	f. Flue-gas condenser	g. Wet flue-gas desulphurisation (wet FGD)		Not applicable to combustion plants operated < 500 h/yr.			There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr	h. Fuel choice		Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State	N/A	N/A
Technique	Description	Applicability																					
a. Boiler sorbent injection (in-furnace or in-bed)	See descriptions in Section 8.4	Generally applicable																					
b. Duct sorbent injection (DSI)																							
c. Spray dry absorber (SDA)																							
d. Circulating fluidised bed (CFB) dry scrubber																							
e. Wet scrubbing																							
f. Flue-gas condenser																							
g. Wet flue-gas desulphurisation (wet FGD)		Not applicable to combustion plants operated < 500 h/yr.																					
		There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr																					
h. Fuel choice		Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State																					

BAT-associated emission levels (BAT-AELs) for SO₂ emissions to air from the combustion of solid biomass and/or peat

Combustion plant total rated thermal input (MW _{th})	BAT-AELs for SO ₂ (mg/Nm ³)			
	Yearly average		Daily average or average over the sampling period	
	New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾
< 100	15–70	15–100	30–175	30–215
100–300	< 10–50	< 10–70 ⁽³⁾	< 20–85	< 20–175 ⁽⁴⁾
≥ 300	< 10–35	< 10–50 ⁽³⁾	< 20–70	< 20–85 ⁽²⁾

(1) These BAT-AELs do not apply to plants operated < 1 500 h/yr.

(2) For plants operated < 500 h/yr, these levels are indicative.

(3) For existing plants burning fuels where the average sulphur content is 0,1 wt-% (dry) or higher, the higher end of the BAT-AEL range is 100 mg/Nm³.

(4) For existing plants burning fuels where the average sulphur content is 0,1 wt-% (dry) or higher, the higher end of the BAT-AEL range is 215 mg/Nm³.

(5) For existing plants burning fuels where the average sulphur content is 0,1 wt-% (dry) or higher, the higher end of the BAT-AEL range is 165 mg/Nm³, or 215 mg/Nm³ if those plants have been put into operation no later than 7 January 2014 and/or are FBC boilers combusting peat.

Table 11

BAT-associated emission levels (BAT-AELs) for HCl and HF emissions to air from the combustion of solid biomass and/or peat

Combustion plant total rated thermal input (MW _{th})	BAT-AELs for HCl (mg/Nm ³) ⁽¹⁾⁽²⁾				BAT-AELs for HF (mg/Nm ³)	
	Yearly average or average of samples obtained during one year		Daily average or average over the sampling period		Average over the sampling period	
	New plant	Existing plant ⁽³⁾⁽⁴⁾	New plant	Existing plant ⁽⁵⁾	New plant	Existing plant ⁽⁵⁾
< 100	1–7	1–15	1–12	1–35	< 1	< 1,5
100–300	1–5	1–9	1–12	1–12	< 1	< 1
≥ 300	1–5	1–5	1–12	1–12	< 1	< 1

(1) For plants burning fuels where the average chlorine content is ≥ 0,1 wt-% (dry), or for existing plants co-combusting biomass with sulphur-rich fuel (e.g. peat) or using alkali chloride-converting additives (e.g. elemental sulphur), the higher end of the BAT-AEL range for the yearly average for new plants is 15 mg/Nm³, the higher end of the BAT-AEL range for the yearly average for existing plants is 25 mg/Nm³. The daily average BAT-AEL range does not apply to these plants.

(2) The daily average BAT-AEL range does not apply to plants operated < 1 500 h/yr. The higher end of the BAT-AEL range for the yearly average for new plants operated < 1 500 h/yr is 15 mg/Nm³.

(3) These BAT-AELs do not apply to plants operated < 1 500 h/yr.

(4) The lower end of these BAT-AEL ranges may be difficult to achieve in the case of plants fitted with wet FGD and a downstream gas-gas heater.

(5) For plants operated < 500 h/yr, these levels are indicative.

<div>BAT 26</div> <div>Dust and particulate-bound metal emissions to air</div>	<div>In order to reduce dust and particulate-bound metal emissions to air from the combustion of solid biomass and/or peat, BAT is to use one or a combination of the techniques given below.</div> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Electrostatic precipitator (ESP)</td><td rowspan="3">See description in Section 8.5</td><td rowspan="3">Generally applicable</td></tr><tr><td>b. Bag filter</td></tr><tr><td>c. Dry or semi-dry FGD system</td></tr><tr><td>d. Wet flue-gas desulphurisation (wet FGD)</td><td rowspan="2">See descriptions in Section 8.5 The techniques are mainly used for SO_x, HCl and/or HF control</td><td rowspan="2">See applicability in BAT 25</td></tr><tr><td>e. Fuel choice</td></tr><tr><td></td><td>See description in Section 8.5</td><td>Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State</td></tr></table> <div>Table 12</div> <div>BAT-associated emission levels (BAT-AELs) for dust emissions to air from the combustion of solid biomass and/or peat</div> <table><tr><th rowspan="3">Combustion plant total rated thermal input (MW_{th})</th><th colspan="4">BAT-AELs for dust (mg/Nm³)</th></tr><tr><th colspan="2">Yearly average</th><th colspan="2">Daily average or average over the sampling period</th></tr><tr><th>New plant</th><th>Existing plant ⁽¹⁾</th><th>New plant</th><th>Existing plant ⁽¹⁾</th></tr><tr><td>< 100</td><td>2–5</td><td>2–15</td><td>2–10</td><td>2–22</td></tr><tr><td>100–300</td><td>2–5</td><td>2–12</td><td>2–10</td><td>2–18</td></tr><tr><td>≥ 300</td><td>2–5</td><td>2–10</td><td>2–10</td><td>2–16</td></tr></table> <div>(1) These BAT-AELs do not apply to plants operated < 1 500 h/yr. (2) For plants operated < 500 h/yr, these levels are indicative.</div>	Technique	Description	Applicability	a. Electrostatic precipitator (ESP)	See description in Section 8.5	Generally applicable	b. Bag filter	c. Dry or semi-dry FGD system	d. Wet flue-gas desulphurisation (wet FGD)	See descriptions in Section 8.5 The techniques are mainly used for SO _x , HCl and/or HF control	See applicability in BAT 25	e. Fuel choice		See description in Section 8.5	Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State	Combustion plant total rated thermal input (MW _{th})	BAT-AELs for dust (mg/Nm ³)				Yearly average		Daily average or average over the sampling period		New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽¹⁾	< 100	2–5	2–15	2–10	2–22	100–300	2–5	2–12	2–10	2–18	≥ 300	2–5	2–10	2–10	2–16	N/A	N/A
Technique	Description	Applicability																																												
a. Electrostatic precipitator (ESP)	See description in Section 8.5	Generally applicable																																												
b. Bag filter																																														
c. Dry or semi-dry FGD system																																														
d. Wet flue-gas desulphurisation (wet FGD)	See descriptions in Section 8.5 The techniques are mainly used for SO _x , HCl and/or HF control	See applicability in BAT 25																																												
e. Fuel choice																																														
	See description in Section 8.5	Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State																																												
Combustion plant total rated thermal input (MW _{th})	BAT-AELs for dust (mg/Nm ³)																																													
	Yearly average		Daily average or average over the sampling period																																											
	New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽¹⁾																																										
< 100	2–5	2–15	2–10	2–22																																										
100–300	2–5	2–12	2–10	2–18																																										
≥ 300	2–5	2–10	2–10	2–16																																										
<div>BAT 27</div> <div>Mercury emissions to air</div>	<div>In order to prevent or reduce mercury emissions to air from the combustion of solid biomass and/or peat, BAT is to use one or a combination of the techniques given below.</div> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td colspan="3">Specific techniques to reduce mercury emissions</td></tr><tr><td>a. Carbon sorbent (e.g. activated carbon or halogenated activated carbon) injection in the flue-gas</td><td>See descriptions in Section 8.5</td><td>Generally applicable</td></tr></table>	Technique	Description	Applicability	Specific techniques to reduce mercury emissions			a. Carbon sorbent (e.g. activated carbon or halogenated activated carbon) injection in the flue-gas	See descriptions in Section 8.5	Generally applicable	N/A	N/A																																		
Technique	Description	Applicability																																												
Specific techniques to reduce mercury emissions																																														
a. Carbon sorbent (e.g. activated carbon or halogenated activated carbon) injection in the flue-gas	See descriptions in Section 8.5	Generally applicable																																												

	b. Use of halogenated additives in the fuel or injected in the furnace		Generally applicable in the case of a low halogen content in the fuel		
	c. Fuel choice		Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State		
	Co-benefit from techniques primarily used to reduce emissions of other pollutants				
	d. Electrostatic precipitator (ESP)	See descriptions in	Generally applicable		
	e. Bag filter	Section 8.5. The techniques are mainly used for dust control			
	f. Dry or semi-dry FGD system	See descriptions in	See applicability in BAT 25		
	g. Wet flue-gas desulphurisation (wet FGD)	Section 8.5. The techniques are mainly used for SO _x , HCl and/or HF control			
	The BAT-associated emission level (BAT-AEL) for mercury emissions to air from the combustion of solid biomass and/or peat is < 1–5 µg/Nm ³ as average over the sampling period.				

3. BAT CONCLUSIONS FOR THE COMBUSTION OF LIQUID FUELS

The BAT conclusions presented in this section do not apply to combustion plants on offshore platforms; these are covered by Section 4.3

3.1. HFO- and/or gas-oil-fired boilers

Unless otherwise stated, the BAT conclusions presented in this section are generally applicable to the combustion of HFO and/or gas oil in boilers. They apply in addition to the general BAT conclusions given in Section 1

Bat conclusions					STATUS AT INSTALLATION: [ENTER NAME OF OPERATOR]	STATE WHETHER IT IS IN PLACE OR STATE SCHEDULE FOR IMPLEMENTATION																				
					DATE: [ENTER DATE OF ASSESSMENT]																					
					Applicability Assessment (describe how the technique applies or not to your installation)																					
Energy efficiency	Table 13 BAT-associated energy efficiency levels (BAT-AEELs) for HFO and/or gas oil combustion in boilers				N/A	N/A																				
<table><tr><td rowspan="3">Type of combustion unit</td><td colspan="4">BAT-AEELs ⁽¹⁾⁽²⁾</td></tr><tr><td colspan="2">Net electrical efficiency (%)</td><td colspan="2">Net total fuel utilisation (%)</td></tr><tr><td>New unit</td><td>Existing unit</td><td>New unit</td><td>Existing unit ⁽³⁾</td></tr><tr><td>HFO- and/or gas-oil-fired boiler</td><td>> 36,4</td><td>35,6–37,4</td><td>80–96</td><td>80–96</td><td colspan="2"></td></tr></table> <p>(1) These BAT-AEELs do not apply to units operated < 1 500 h/yr.</p> <p>(2) In the case of CHP units, only one of the two BAT-AEELs ‘Net electrical efficiency’ or ‘Net total fuel utilisation’ applies, depending on the CHP unit design (i.e. either more oriented towards electricity generation or towards heat generation).</p> <p>(3) These levels may not be achievable if the potential heat demand is too low.</p>							Type of combustion unit	BAT-AEELs ⁽¹⁾⁽²⁾				Net electrical efficiency (%)		Net total fuel utilisation (%)		New unit	Existing unit	New unit	Existing unit ⁽³⁾	HFO- and/or gas-oil-fired boiler	> 36,4	35,6–37,4	80–96	80–96		
Type of combustion unit	BAT-AEELs ⁽¹⁾⁽²⁾																									
	Net electrical efficiency (%)		Net total fuel utilisation (%)																							
	New unit	Existing unit	New unit	Existing unit ⁽³⁾																						
HFO- and/or gas-oil-fired boiler	> 36,4	35,6–37,4	80–96	80–96																						
BAT 28	In order to prevent or reduce NO _x emissions to air while limiting CO emissions to air from the combustion of HFO and/or gas oil in boilers, BAT is to use one or a combination of the techniques given below.				N/A	N/A																				
NO _x and CO emissions to air	<table><tr><td>Technique</td><td>Description</td><td>Applicability</td></tr><tr><td>a. Air staging</td><td rowspan="3">See descriptions in Section 8.3</td><td rowspan="3">Generally applicable</td></tr><tr><td>b. Fuel staging</td></tr><tr><td>c. Flue-gas recirculation</td></tr></table>				Technique	Description	Applicability	a. Air staging	See descriptions in Section 8.3	Generally applicable	b. Fuel staging	c. Flue-gas recirculation	N/A	N/A												
Technique	Description	Applicability																								
a. Air staging	See descriptions in Section 8.3	Generally applicable																								
b. Fuel staging																										
c. Flue-gas recirculation																										

	d. Low-NO _x burners (LNB)		
	e. Water/steam addition		Applicable within the constraints of water availability
	f. Selective non-catalytic reduction (SNCR)		Not applicable to combustion plants operated < 500 h/yr with highly variable boiler loads. The applicability may be limited in the case of combustion plants operated between 500 h/yr and 1 500 h/yr with highly variable boiler loads
	g. Selective catalytic reduction (SCR)	See descriptions in Section 8.3	Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr. Not generally applicable to combustion plants of < 100 MW _{th}
	h. Advanced control system		Generally applicable to new combustion plants. The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system
	i. Fuel choice		Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State

Table 14

BAT-associated emission levels (BAT-AELs) for NO_x emissions to air from the combustion of HFO and/or gas oil in boilers

Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)			
	Yearly average		Daily average or average over the sampling period	
	New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾
< 100	75–200	150–270	100–215	210–330 ⁽³⁾
≥ 100	45–75	45–100 ⁽⁴⁾	85–100	85–110 ⁽⁵⁾⁽⁶⁾

(1) These BAT-AELs do not apply to plants operated < 1 500 h/yr.

(2) For plants operated < 500 h/yr, these levels are indicative.

(3) For industrial boilers and district heating plants put into operation no later than 27 November 2003, which are operated < 1 500 h/yr and for which SCR and/or SNCR is not applicable, the higher end of the BAT-AEL range is 450 mg/Nm3.

(4) The higher end of the BAT-AEL range is 110 mg/Nm3 for plants of 100–300 MWth and plants of ≥ 300 MWth that were put into operation no later than 7 January 2014.

(5) The higher end of the BAT-AEL range is 145 mg/Nm3 for plants of 100–300 MWth and plants of ≥ 300 MWth that were put into operation no later than 7 January 2014.

(6) For industrial boilers and district heating plants of > 100 MWth put into operation no later than 27 November 2003, which are operated < 1 500 h/yr and for which SCR and/or SNCR is not applicable, the higher end of the BAT-AEL range is 365 mg/Nm3.

	<p>As an indication, the yearly average CO emission levels will generally be:</p> <p>— 10-30 mg/Nm³ for existing combustion plants of < 100 MW_{th} operated ≥ 1 500 h/yr, or new combustion plants of <100 MW_{th},</p> <p>— 10–20mg/Nm³ for existing combustion plants of ≥ 100 MW_{th} operated ≥ 1 500 h/yr, or new combustion plants of ≥ 100 MW_{th}.</p>																														
<p>BAT 29</p> <p>SO_x, HCl and HF emissions to air</p>	<p>In order to prevent or reduce SO_x, HCl and HF emissions to air from the combustion of HFO and/or gas oil in boilers, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Duct sorbent injection (DSI)</td><td rowspan="4">See description in Section 8.4</td><td rowspan="3">Generally applicable</td></tr><tr><td>b. Spray dry absorber (SDA)</td></tr><tr><td>c. Flue-gas condenser</td></tr><tr><td>d. Wet flue-gas desulphurisation (wet FGD)</td><td>There may be technical and economic restrictions for applying the technique to combustion plants of < 300 MW_{th}.</td></tr><tr><td>e. Seawater FGD</td><td></td><td>Not applicable to combustion plants operated < 500 h/yr.</td></tr><tr><td></td><td></td><td>There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr</td></tr><tr><td>f. Fuel choice</td><td></td><td>There may be technical and economic restrictions for applying the technique to combustion plants of < 300 MW_{th}.</td></tr><tr><td></td><td></td><td>Not applicable to combustion plants operated < 500 h/yr.</td></tr><tr><td></td><td></td><td>There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr</td></tr><tr><td></td><td></td><td>Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State</td></tr></table>	Technique	Description	Applicability	a. Duct sorbent injection (DSI)	See description in Section 8.4	Generally applicable	b. Spray dry absorber (SDA)	c. Flue-gas condenser	d. Wet flue-gas desulphurisation (wet FGD)	There may be technical and economic restrictions for applying the technique to combustion plants of < 300 MW _{th} .	e. Seawater FGD		Not applicable to combustion plants operated < 500 h/yr.			There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr	f. Fuel choice		There may be technical and economic restrictions for applying the technique to combustion plants of < 300 MW _{th} .			Not applicable to combustion plants operated < 500 h/yr.			There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr			Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State	N/A	N/A
Technique	Description	Applicability																													
a. Duct sorbent injection (DSI)	See description in Section 8.4	Generally applicable																													
b. Spray dry absorber (SDA)																															
c. Flue-gas condenser																															
d. Wet flue-gas desulphurisation (wet FGD)		There may be technical and economic restrictions for applying the technique to combustion plants of < 300 MW _{th} .																													
e. Seawater FGD		Not applicable to combustion plants operated < 500 h/yr.																													
		There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr																													
f. Fuel choice		There may be technical and economic restrictions for applying the technique to combustion plants of < 300 MW _{th} .																													
		Not applicable to combustion plants operated < 500 h/yr.																													
		There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr																													
		Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State																													

Table 15

	<div>BAT-associated emission levels (BAT-AELs) for SO₂ emissions to air from the combustion of HFO and/or gas oil in boilers</div> <table><tr><td rowspan="4">Combustion plant total rated thermal input (MW_{th})</td><td colspan="4">BAT-AELs for SO₂ (mg/Nm³)</td></tr><tr><td colspan="2">Yearly average</td><td colspan="2">Daily average or average over the sampling period</td></tr><tr><td>New plant</td><td>Existing plant ⁽¹⁾</td><td>New plant</td><td>Existing plant ⁽²⁾</td></tr><tr><td>< 300</td><td>50–175</td><td>50–175</td><td>150–200</td><td>150–200 ⁽³⁾</td></tr><tr><td>≥ 300</td><td>35–50</td><td>50–110</td><td>50–120</td><td>150–165 ⁽⁴⁾⁽⁵⁾</td></tr></table> <div>(1) These BAT-AELs do not apply to plants operated < 1 500 h/yr. (2) For plants operated < 500 h/yr, these levels are indicative. (3)For industrial boilers and district heating plants put into operation no later than 27 November 2003 and operated < 1 500 h/yr, the higher end of the BAT-AEL range is 400 mg/Nm3. (4) The higher end of the BAT-AEL range is 175 mg/Nm3 for plants put into operation no later than 7 January 2014. (5) For industrial boilers and district heating plants put into operation no later than 27 November 2003, which are operated < 1 500 h/yr and for which wet FGD is not applicable, the higher end of the BAT-AEL range is 200 mg/Nm3.</div>	Combustion plant total rated thermal input (MW _{th})	BAT-AELs for SO ₂ (mg/Nm ³)				Yearly average		Daily average or average over the sampling period		New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾	< 300	50–175	50–175	150–200	150–200 ⁽³⁾	≥ 300	35–50	50–110	50–120	150–165 ⁽⁴⁾⁽⁵⁾		
Combustion plant total rated thermal input (MW _{th})	BAT-AELs for SO ₂ (mg/Nm ³)																									
	Yearly average		Daily average or average over the sampling period																							
	New plant		Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾																					
	< 300	50–175	50–175	150–200	150–200 ⁽³⁾																					
≥ 300	35–50	50–110	50–120	150–165 ⁽⁴⁾⁽⁵⁾																						
<div>BAT 30</div> <div>Dust and particulate-bound metal emissions to air</div>	<div>In order to reduce dust and particulate-bound metal emissions to air from the combustion of HFO and/or gas oil in boilers, BAT is to use one or a combination of the techniques given below.</div> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Electrostatic precipitator (ESP)</td><td rowspan="2">See description in Section 8.5</td><td rowspan="3">Generally applicable</td></tr><tr><td>b. Bag filter</td></tr><tr><td>c. Multicyclones</td><td>See description in Section 8.5. Multicyclones can be used in combination with other dedusting techniques</td></tr><tr><td>d. Dry or semi-dry FGD system</td><td>See descriptions in Section 8.5. The technique is mainly used for SO_x, HCl and/or HF control</td><td rowspan="3">See applicability in BAT 29</td></tr><tr><td>e. Wet flue-gas desulphurisation (wet FGD)</td><td>See description in Section 8.5. The technique is mainly used for SO_x, HCl and/or HF control</td></tr><tr><td>f. Fuel choice</td><td>See description in Section 8.5</td><td>Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State</td></tr></table> <div>Table 16</div>	Technique	Description	Applicability	a. Electrostatic precipitator (ESP)	See description in Section 8.5	Generally applicable	b. Bag filter	c. Multicyclones	See description in Section 8.5. Multicyclones can be used in combination with other dedusting techniques	d. Dry or semi-dry FGD system	See descriptions in Section 8.5. The technique is mainly used for SO _x , HCl and/or HF control	See applicability in BAT 29	e. Wet flue-gas desulphurisation (wet FGD)	See description in Section 8.5. The technique is mainly used for SO _x , HCl and/or HF control	f. Fuel choice	See description in Section 8.5	Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State	N/A	N/A						
Technique	Description	Applicability																								
a. Electrostatic precipitator (ESP)	See description in Section 8.5	Generally applicable																								
b. Bag filter																										
c. Multicyclones	See description in Section 8.5. Multicyclones can be used in combination with other dedusting techniques																									
d. Dry or semi-dry FGD system	See descriptions in Section 8.5. The technique is mainly used for SO _x , HCl and/or HF control	See applicability in BAT 29																								
e. Wet flue-gas desulphurisation (wet FGD)	See description in Section 8.5. The technique is mainly used for SO _x , HCl and/or HF control																									
f. Fuel choice	See description in Section 8.5		Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State																							

BAT-associated emission levels (BAT-AELs) for dust emissions to air from the combustion of HFO and/or gas oil in boilers				
Combustion plant total rated thermal input (MW _{th})	BAT-AELs for dust (mg/Nm ³)			
	Yearly average		Daily average or average over the sampling period	
	New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾
	< 300	2–10	2–20	7–18
	≥ 300	2–5	2–10	7–22 ⁽³⁾
(1) These BAT-AELs do not apply to plants operated < 1 500 h/yr.				
(2) For plants operated < 500 h/yr, these levels are indicative.				
(3) The higher end of the BAT-AEL range is 25 mg/Nm3 for plants put into operation no later than 7 January 2014.				
(4) The higher end of the BAT-AEL range is 15 mg/Nm3 for plants put into operation no later than 7 January 2014.				

3.2. HFO- and/or gas-oil-fired engines

Unless otherwise stated, the BAT conclusions presented in this section are generally applicable to the combustion of HFO and/or gas oil in reciprocating engines. They apply in addition to the general BAT conclusions given in Section 1.

As regards HFO- and/or gas-oil-fired engines, secondary abatement techniques for NO_x, SO₂ and dust may not be applicable to engines in islands that are part of a small isolated system or a micro isolated system, due to technical, economic and logistical/infrastructure constraints, pending their interconnection to the mainland electricity grid or access to a natural gas supply. The BAT-AELs for such engines shall therefore only apply in small isolated system and micro isolated system as from 1 January 2025 for new engines, and as from 1 January 2030 for existing engines.

Bat conclusions			STATUS AT INSTALLATION: [ENTER NAME OF OPERATOR]	STATE WHETHER IT IS IN PLACE OR STATE SCHEDULE FOR IMPLEMENTATION
			DATE: [ENTER DATE OF ASSESSMENT]	
			Applicability Assessment (describe how the technique applies or not to your installation)	
BAT 31 Energy efficiency	In order to increase the energy efficiency of HFO and/or gas oil combustion in reciprocating engines, BAT is to use an appropriate combination of the techniques given in BAT 12 and below.		N/A	N/A
	Technique	Description		
	a. Combined cycle	See description in Section 8.2		
		Generally applicable to new units operated ≥ 1 500 h/yr.		
		Applicable to existing units within the constraints associated with the steam cycle design and the space availability.		
Table 17				
BAT-associated energy efficiency levels (BAT-AEELs) for the combustion of HFO and/or gas oil in reciprocating engines				
Type of combustion unit		BAT-AEELs ⁽¹⁾		
		Net electrical efficiency (%) ⁽²⁾		
		New unit	Existing unit	
HFO- and/or gas-oil-fired reciprocating engine — single cycle		41,5–44,5 ⁽¹⁾	38,3–44,5 ⁽¹⁾	
HFO- and/or gas-oil-fired reciprocating engine — combined cycle		> 48 ⁽⁴⁾	No BAT-AEEL	

	<p>(1) These BAT-AEELs do not apply to units operated < 1 500 h/yr.</p> <p>(2) Net electrical efficiency BAT-AEELs apply to CHP units whose design is oriented towards power generation, and to units generating only power.</p> <p>(3)These levels may be difficult to achieve in the case of engines fitted with energy-intensive secondary abatement techniques.</p> <p>(4) This level may be difficult to achieve in the case of engines using a radiator as a cooling system in dry, hot geographical locations.</p>														
BAT 32 NO_x, CO and volatile organic compound emissions to air	<p>In order to prevent or reduce NO_x emissions to air from the combustion of HFO and/or gas oil in reciprocating engines, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Low-NO_x combustion concept in diesel engines</td><td rowspan="4">See descriptions in Section 8.3</td><td>Generally applicable</td></tr><tr><td>b. Exhaust-gas recirculation (EGR)</td><td>Not applicable to four-stroke engines</td></tr><tr><td>c. Water/steam addition</td><td>Applicable within the constraints of water availability. The applicability may be limited where no retrofit package is available</td></tr><tr><td>d. Selective catalytic reduction (SCR)</td><td>Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr. Retrofitting existing combustion plants may be constrained by the availability of sufficient space</td></tr></table>	Technique	Description	Applicability	a. Low-NO _x combustion concept in diesel engines	See descriptions in Section 8.3	Generally applicable	b. Exhaust-gas recirculation (EGR)	Not applicable to four-stroke engines	c. Water/steam addition	Applicable within the constraints of water availability. The applicability may be limited where no retrofit package is available	d. Selective catalytic reduction (SCR)	Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr. Retrofitting existing combustion plants may be constrained by the availability of sufficient space	N/A	N/A
Technique	Description	Applicability													
a. Low-NO _x combustion concept in diesel engines	See descriptions in Section 8.3	Generally applicable													
b. Exhaust-gas recirculation (EGR)		Not applicable to four-stroke engines													
c. Water/steam addition		Applicable within the constraints of water availability. The applicability may be limited where no retrofit package is available													
d. Selective catalytic reduction (SCR)		Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr. Retrofitting existing combustion plants may be constrained by the availability of sufficient space													
BAT 33 reduce emissions of CO and volatile organic compounds	<p>In order to prevent or reduce emissions of CO and volatile organic compounds to air from the combustion of HFO and/or gas oil in reciprocating engines, BAT is to use one or both of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Combustion optimisation</td><td></td><td>Generally applicable</td></tr><tr><td>b. Oxidation catalysts</td><td>See descriptions in Section 8.3</td><td>Not applicable to combustion plants operated < 500 h/yr. The applicability may be limited by the sulphur content of the fuel</td></tr></table> <p>Table 18</p>	Technique	Description	Applicability	a. Combustion optimisation		Generally applicable	b. Oxidation catalysts	See descriptions in Section 8.3	Not applicable to combustion plants operated < 500 h/yr. The applicability may be limited by the sulphur content of the fuel	N/A	N/A			
Technique	Description	Applicability													
a. Combustion optimisation		Generally applicable													
b. Oxidation catalysts	See descriptions in Section 8.3	Not applicable to combustion plants operated < 500 h/yr. The applicability may be limited by the sulphur content of the fuel													

	<div>BAT-associated emission levels (BAT-AELs) for NO_x emissions to air from the combustion of HFO and/or gas oil in reciprocating engines</div> <table><tr><td rowspan="3">Combustion plant total rated thermal input (MW_{th})</td><td colspan="4">BAT-AELs (mg/Nm³)</td></tr><tr><td colspan="2">Yearly average</td><td colspan="2">Daily average or average over the sampling period</td></tr><tr><td>New plant</td><td>Existing plant ⁽¹⁾</td><td>New plant</td><td>Existing plant ⁽²⁾⁽³⁾</td></tr><tr><td>≥ 50</td><td>115–190 ⁽⁴⁾</td><td>125–625</td><td>145–300</td><td>150–750</td></tr></table> <div>(1)These BAT-AELs do not apply to plants operated < 1 500 h/yr or to plants that cannot be fitted with secondary abatement techniques. (2) The BAT-AEL range is 1 150–1 900 mg/Nm3 for plants operated < 1 500 h/yr and for plants that cannot be fitted with secondary abatement techniques. (3) For plants operated < 500 h/yr, these levels are indicative. (4) For plants including units of < 20 MWth combusting HFO, the higher end of the BAT-AEL range applying to those units is 225 mg/Nm3.</div> <div>As an indication, for existing combustion plants burning only HFO and operated ≥ 1 500 h/yr or new combustion plants burning only HFO,</div> <div><div>— the yearly average CO emission levels will generally be 50–175 mg/Nm³,</div><div>— the average over the sampling period for TVOC emission levels will generally be 10–40 mg/Nm³.</div></div>	Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)				Yearly average		Daily average or average over the sampling period		New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾⁽³⁾	≥ 50	115–190 ⁽⁴⁾	125–625	145–300	150–750		
Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)																				
	Yearly average		Daily average or average over the sampling period																		
	New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾⁽³⁾																	
≥ 50	115–190 ⁽⁴⁾	125–625	145–300	150–750																	
<div>BAT 34</div> <div>SO_x, HCl and HF emissions to air</div>	<div>In order to prevent or reduce SOX, HCl and HF emissions to air from the combustion of HFO and/or gas oil in reciprocating engines, BAT is to use one or a combination of the techniques given below.</div> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Fuel choice</td><td rowspan="3">See descriptions in Section 8.4</td><td>Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State</td></tr><tr><td>b. Duct sorbent injection (DSI)</td><td>There may be technical restrictions in the case of existing combustion plants Not applicable to combustion plants operated < 500 h/yr</td></tr><tr><td>c. Wet flue-gas desulphurisation (wet FGD)</td><td>There may be technical and economic restrictions for applying the technique to combustion plants of < 300 MW_{th}. Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr</td></tr></table> <div>Table 19</div> <div>BAT-associated emission levels (BAT-AELs) for SO₂ emissions to air from the combustion of HFO and/or gas oil in reciprocating engines</div>	Technique	Description	Applicability	a. Fuel choice	See descriptions in Section 8.4	Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State	b. Duct sorbent injection (DSI)	There may be technical restrictions in the case of existing combustion plants Not applicable to combustion plants operated < 500 h/yr	c. Wet flue-gas desulphurisation (wet FGD)	There may be technical and economic restrictions for applying the technique to combustion plants of < 300 MW _{th} . Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr	N/A	N/A								
Technique	Description	Applicability																			
a. Fuel choice	See descriptions in Section 8.4	Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State																			
b. Duct sorbent injection (DSI)		There may be technical restrictions in the case of existing combustion plants Not applicable to combustion plants operated < 500 h/yr																			
c. Wet flue-gas desulphurisation (wet FGD)		There may be technical and economic restrictions for applying the technique to combustion plants of < 300 MW _{th} . Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr																			

	<table><tr><td rowspan="4">Combustion plant total rated thermal input (MW_{th}) All sizes</td><td colspan="4">BAT-AELs for SO₂ (mg/Nm³)</td></tr><tr><td colspan="2">Yearly average</td><td colspan="2">Daily average or average over the sampling period</td></tr><tr><td>New plant</td><td>Existing plant ⁽¹⁾</td><td>New plant</td><td>Existing plant ⁽²⁾</td></tr><tr><td>45–100</td><td>100–200 ⁽³⁾</td><td>60–110</td><td>105–235 ⁽³⁾</td></tr></table> <p>(1) These BAT-AELs do not apply to plants operated < 1 500 h/yr. (2) For plants operated < 500 h/yr, these levels are indicative. (3)The higher end of the BAT-AEL range is 280 mg/Nm3 if no secondary abatement technique can be applied. This corresponds to a sulphur content of the fuel of 0,5 wt-% (dry).</p>	Combustion plant total rated thermal input (MW _{th}) All sizes	BAT-AELs for SO ₂ (mg/Nm ³)				Yearly average		Daily average or average over the sampling period		New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾	45–100	100–200 ⁽³⁾	60–110	105–235 ⁽³⁾											
Combustion plant total rated thermal input (MW _{th}) All sizes	BAT-AELs for SO ₂ (mg/Nm ³)																												
	Yearly average		Daily average or average over the sampling period																										
	New plant		Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾																								
	45–100	100–200 ⁽³⁾	60–110	105–235 ⁽³⁾																									
BAT 35 Dust and particulate-bound metal emissions to air	<p>In order to prevent or reduce dust and particulate-bound metal emissions from the combustion of HFO and/or gas oil in reciprocating engines, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Fuel choice</td><td rowspan="3">See descriptions in Section 8.5</td><td>Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State</td></tr><tr><td>b. Electrostatic precipitator (ESP)</td><td rowspan="2">Not applicable to combustion plants operated < 500 h/yr</td></tr><tr><td>c. Bag filter</td></tr></table> <p><i>Table 20</i></p> <p>BAT-associated emission levels (BAT-AELs) for dust emissions to air from the combustion of HFO and/or gas oil in reciprocating engines</p> <table><tr><td rowspan="4">Combustion plant total rated thermal input (MW_{th}) ≥ 50</td><td colspan="4">BAT-AELs for dust (mg/Nm³)</td></tr><tr><td colspan="2">Yearly average</td><td colspan="2">Daily average or average over the sampling period</td></tr><tr><td>New plant</td><td>Existing plant ⁽¹⁾</td><td>New plant</td><td>Existing plant ⁽²⁾</td></tr><tr><td>5–10</td><td>5–35</td><td>10–20</td><td>10–45</td></tr></table> <p>(¹) These BAT-AELs do not apply to plants operated < 1 500 h/yr. (²) For plants operated < 500 h/yr, these levels are indicative.</p>	Technique	Description	Applicability	a. Fuel choice	See descriptions in Section 8.5	Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State	b. Electrostatic precipitator (ESP)	Not applicable to combustion plants operated < 500 h/yr	c. Bag filter	Combustion plant total rated thermal input (MW _{th}) ≥ 50	BAT-AELs for dust (mg/Nm ³)				Yearly average		Daily average or average over the sampling period		New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾	5–10	5–35	10–20	10–45	N/A	N/A
Technique	Description	Applicability																											
a. Fuel choice	See descriptions in Section 8.5	Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State																											
b. Electrostatic precipitator (ESP)		Not applicable to combustion plants operated < 500 h/yr																											
c. Bag filter																													
Combustion plant total rated thermal input (MW _{th}) ≥ 50	BAT-AELs for dust (mg/Nm ³)																												
	Yearly average		Daily average or average over the sampling period																										
	New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾																									
	5–10	5–35	10–20	10–45																									

3.3. Gas-oil-fired gas turbines

Unless stated otherwise, the BAT conclusions presented in this section are generally applicable to the combustion of gas oil in gas turbines. They apply in addition to the general BAT conclusions given in Section 1.

Bat conclusions		STATUS AT INSTALLATION: [ENTER NAME OF OPERATOR]	STATE WHETHER IT IS IN PLACE OR STATE SCHEDULE FOR IMPLEMENTATION																			
		DATE: [ENTER DATE OF ASSESSMENT]																				
		Applicability Assessment (describe how the technique applies or not to your installation)																				
BAT 36	In order to increase the energy efficiency of gas oil combustion in gas turbines, BAT is to use an appropriate combination of the techniques given in BAT 12 and below.	N/A	N/A																			
Energy efficiency	<table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Combined cycle</td><td>See description in Section 8.2</td><td>Generally applicable to new units operated ≥ 1 500 h/yr. Applicable to existing units within the constraints associated with the steam cycle design and the space availability. Not applicable to existing units operated < 1 500 h/yr</td></tr></table> <p>Table 21</p> <p>BAT-associated energy efficiency levels (BAT-AEELs) for gas-oil-fired gas turbines</p> <table><tr><th rowspan="3">Type of combustion unit</th><th colspan="2">BAT-AEELs ⁽¹⁾</th></tr><tr><th colspan="2">Net electrical efficiency (%) ⁽²⁾</th></tr><tr><th>New unit</th><th>Existing unit</th></tr><tr><td>Gas-oil-fired open-cycle gas turbine</td><td>> 33</td><td>25–35,7</td></tr><tr><td>Gas-oil-fired combined cycle gas turbine</td><td>> 40</td><td>33–44</td></tr></table> <p>(1) These BAT-AEELs do not apply to units operated < 1 500 h/yr.</p> <p>(2) Net electrical efficiency BAT-AEELs apply to CHP units whose design is oriented towards power generation, and to units generating only power.</p>	Technique	Description	Applicability	a. Combined cycle	See description in Section 8.2	Generally applicable to new units operated ≥ 1 500 h/yr. Applicable to existing units within the constraints associated with the steam cycle design and the space availability. Not applicable to existing units operated < 1 500 h/yr	Type of combustion unit	BAT-AEELs ⁽¹⁾		Net electrical efficiency (%) ⁽²⁾		New unit	Existing unit	Gas-oil-fired open-cycle gas turbine	> 33	25–35,7	Gas-oil-fired combined cycle gas turbine	> 40	33–44		
Technique	Description	Applicability																				
a. Combined cycle	See description in Section 8.2	Generally applicable to new units operated ≥ 1 500 h/yr. Applicable to existing units within the constraints associated with the steam cycle design and the space availability. Not applicable to existing units operated < 1 500 h/yr																				
Type of combustion unit	BAT-AEELs ⁽¹⁾																					
	Net electrical efficiency (%) ⁽²⁾																					
	New unit	Existing unit																				
Gas-oil-fired open-cycle gas turbine	> 33	25–35,7																				
Gas-oil-fired combined cycle gas turbine	> 40	33–44																				

BAT 37 NO_x and CO emissions to air	<p>In order to prevent or reduce NO_x emissions to air from the combustion of gas oil in gas turbines, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Water/steam addition</td><td rowspan="3">See description in Section 8.3</td><td>The applicability may be limited due to water availability</td></tr><tr><td>b. Low-NO_x burners (LNB)</td><td>Only applicable to turbine models for which low-NO_x burners are available on the market</td></tr><tr><td>c. Selective catalytic reduction (SCR)</td><td>Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr. Retrofitting existing combustion plants may be constrained by the availability of sufficient space</td></tr></table>	Technique	Description	Applicability	a. Water/steam addition	See description in Section 8.3	The applicability may be limited due to water availability	b. Low-NO _x burners (LNB)	Only applicable to turbine models for which low-NO _x burners are available on the market	c. Selective catalytic reduction (SCR)	Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr. Retrofitting existing combustion plants may be constrained by the availability of sufficient space	N/A	N/A
Technique	Description	Applicability											
a. Water/steam addition	See description in Section 8.3	The applicability may be limited due to water availability											
b. Low-NO _x burners (LNB)		Only applicable to turbine models for which low-NO _x burners are available on the market											
c. Selective catalytic reduction (SCR)		Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr. Retrofitting existing combustion plants may be constrained by the availability of sufficient space											
BAT 38 reduce CO emissions	<table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Combustion optimisation</td><td rowspan="2">See description in Section 8.3</td><td>Generally applicable</td></tr><tr><td>b. Oxidation catalysts</td><td>Not applicable to combustion plants operated < 500 h/yr. Retrofitting existing combustion plants may be constrained by the availability of sufficient space</td></tr></table> <p>As an indication, the emission level for NO_x emissions to air from the combustion of gas oil in dual fuel gas turbines for emergency use operated < 500 h/yr will generally be 145–250 mg/Nm³ as a daily average or average over the sampling period.</p>	Technique	Description	Applicability	a. Combustion optimisation	See description in Section 8.3	Generally applicable	b. Oxidation catalysts	Not applicable to combustion plants operated < 500 h/yr. Retrofitting existing combustion plants may be constrained by the availability of sufficient space	N/A	N/A		
Technique	Description	Applicability											
a. Combustion optimisation	See description in Section 8.3	Generally applicable											
b. Oxidation catalysts		Not applicable to combustion plants operated < 500 h/yr. Retrofitting existing combustion plants may be constrained by the availability of sufficient space											
BAT 39 SO_x and dust emissions to air	<p>In order to prevent or reduce SO_x and dust emissions to air from the combustion of gas oil in gas turbines, BAT is to use the technique given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Fuel choice</td><td>See description in Section 8.4</td><td>Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State</td></tr></table> <p style="text-align: center;"><i>Table 22</i></p> <p>BAT-associated emission levels for SO₂ and dust emissions to air from the combustion of gas oil in gas turbines, including dual fuel gas turbines</p>	Technique	Description	Applicability	a. Fuel choice	See description in Section 8.4	Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State	N/A	N/A				
Technique	Description	Applicability											
a. Fuel choice	See description in Section 8.4	Applicable within the constraints associated with the availability of different types of fuel, which may be impacted by the energy policy of the Member State											

	Type of combustion plant	BAT-AELs (mg/Nm ³)					
		SO ₂		Dust			
		Yearly average ⁽¹⁾	Daily average or average over the sampling period ⁽²⁾	Yearly average ⁽¹⁾	Daily average or average over the sampling period ⁽²⁾		
	New and existing plants	35–60	50–66	2–5	2–10		
	<p>(1) These BAT-AELs do not apply to existing plants operated < 1 500 h/yr.</p> <p>(2) For existing plants operated < 500 h/yr, these levels are indicative.</p>						

4. BAT CONCLUSIONS FOR THE COMBUSTION OF GASEOUS FUELS

4.1. BAT conclusions for the combustion of natural gas

Unless otherwise stated, the BAT conclusions presented in this section are generally applicable to the combustion of natural gas. They apply in addition to the general BAT conclusions given in Section 1. They do not apply to combustion plants on offshore platforms; these are covered by Section. 4.3.

Bat conclusions				STATUS AT INSTALLATION: [ENTER NAME OF OPERATOR] DATE: [ENTER DATE OF ASSESSMENT] Applicability Assessment (describe how the technique applies or not to your installation)	STATE WHETHER IT IS IN PLACE OR STATE SCHEDULE FOR IMPLEMENTATION	ERA reply	EGM reply	ERA reply	EGM reply (9 th Dec 2021)
BAT 40	In order to increase the energy efficiency of natural gas combustion, BAT is to use an appropriate combination of the techniques given in BAT 12 and below.			Net electrical efficiency of this installation is calculated and as evidenced by the monitoring data, values comply with BAT-AEELs for an existing CCGT of 50-600 MW _{th} .	Implemented	Kindly indicate the net electrical efficiency. Kindly submit latest performance data.	The net LHV heat rate was 6654.3kJ/kWh equivalent to 54.1% net LHV thermal efficiency Kindly refer to Annex 11 – Performance test.	Kindly revise and ensure that metrics provided are comparable to the BAT-AEELs.	EGM’s 54.1% lies in the upper range of the BAT-AEELs for an existing CCGT, 50 – 600 MW _{th} .
	Energy efficiency	Technique	Description	Applicability					
	a. Combined cycle	See description in Section 8.2	Generally applicable to new gas turbines and engines except when operated < 1 500 h/yr. Applicable to existing gas turbines and engines within the constraints associated with the steam cycle design and the space availability.						

			Not applicable to existing gas turbines and engines operated < 1 500 h/yr.																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							</
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	<table><tr><td>CHP</td><td>CCGT,</td><td>57–</td><td>50–60</td><td>65–95</td><td>No BAT-AEEL</td></tr><tr><td>≥ 600 MW_{th}</td><td></td><td>60,5</td><td></td><td></td><td></td></tr></table> <p>1) These BAT-AEELs do not apply to units operated < 1 500 h/yr.</p> <p>(2) In the case of CHP units, only one of the two BAT-AEELs ‘Net electrical efficiency’ or ‘Net total fuel utilisation’ applies, depending on the CHP unit design (i.e. either more oriented towards electricity generation or heat generation).</p> <p>(3) Net total fuel utilisation BAT-AEELs may not be achievable if the potential heat demand is too low.</p> <p>(4) These BAT-AEELs do not apply to plants generating only electricity.</p> <p>(5) These BAT-AEELs apply to units used for mechanical drive applications.</p> <p>(6) These levels may be difficult to achieve in the case of engines tuned in order to reach NOX levels lower than 190 mg/Nm3.</p>	CHP	CCGT,	57–	50–60	65–95	No BAT-AEEL	≥ 600 MW _{th}		60,5										
CHP	CCGT,	57–	50–60	65–95	No BAT-AEEL															
≥ 600 MW _{th}		60,5																		
BAT 41 Reduce NO_x emissions to air	<p>In order to prevent or reduce NO_x emissions to air from the combustion of natural gas in boilers, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Air and/or fuel staging</td><td>See descriptions in Section 8.3. Air staging is often associated with low-NO_x burners</td><td rowspan="3">Generally applicable</td></tr><tr><td>b. Flue-gas recirculation</td><td>See description in Section 8.3</td></tr><tr><td>c. Low-NO_x burners (LNB)</td><td></td></tr><tr><td>d. Advanced control system</td><td>See description in Section 8.3. This technique is often used in combination with other techniques or may be used alone for combustion plants operated < 500 h/yr</td><td>The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system</td></tr></table>	Technique	Description	Applicability	a. Air and/or fuel staging	See descriptions in Section 8.3. Air staging is often associated with low-NO _x burners	Generally applicable	b. Flue-gas recirculation	See description in Section 8.3	c. Low-NO _x burners (LNB)		d. Advanced control system	See description in Section 8.3. This technique is often used in combination with other techniques or may be used alone for combustion plants operated < 500 h/yr	The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system	<p>This BAT is not applicable to this CCGT installation as CCGT does not have supplementary firing in boilers.</p>	Not applicable	Non-applicability noted			
Technique	Description	Applicability																		
a. Air and/or fuel staging	See descriptions in Section 8.3. Air staging is often associated with low-NO _x burners	Generally applicable																		
b. Flue-gas recirculation	See description in Section 8.3																			
c. Low-NO _x burners (LNB)																				
d. Advanced control system	See description in Section 8.3. This technique is often used in combination with other techniques or may be used alone for combustion plants operated < 500 h/yr	The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system																		

	e. Reduction of the combustion air temperature	See description in Section 8.3	Generally applicable within the constraints associated with the process needs							
	f. Selective non-catalytic reduction (SNCR)		Not applicable to combustion plants operated < 500 h/yr with highly variable boiler loads. The applicability may be limited in the case of combustion plants operated between 500 h/yr and 1 500 h/yr with highly variable boiler loads							
	g. Selective catalytic reduction (SCR)		Not applicable to combustion plants operated < 500 h/yr. Not generally applicable to combustion plants of < 100 MW _{th} . There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr							

BAT 42 prevent or reduce NO_x emissions to air	In order to prevent or reduce NO _x emissions to air from the combustion of natural gas in gas turbines, BAT is to use one or a combination of the techniques given below.			This plant was designed to achieve the required performance using the following combination of techniques: a. CCGTs are run using the installed Siemens T 3000 plant control system. b. The technique of water/steam addition is not applicable to this installation as dry low-NO _x burners are used. c. Dry low-NO _x burners are incorporated into the three gas turbines. d. Combustion air is controlled through Inter Guide Vanes in order to maintain turbine temperature. Moreover- pre-mix combustion is accomplished through gas burner staging. e. Low-NO _x burners (LNB) technique does not apply to this CCGT installation as	Noted.				
	Technique	Description	Applicability						
	a. Advanced control system	See description in Section 8.3. This technique is often used in combination with other techniques or may be used alone for combustion plants operated < 500 h/yr	The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system						
	b. Water/steam addition	See description in Section 8.3	The applicability may be limited due to water availability						
	c. Dry low-NO _x burners (DLN)		The applicability may be limited in the case of turbines where a retrofit package is not available or when water/steam addition systems are installed						
	d. Low-load design concept	Adaptation of the process control and related equipment to maintain good combustion efficiency when the demand in energy varies, e.g. by improving the inlet airflow control capability or by splitting the combustion process into decoupled combustion stages	The applicability may be limited by the gas turbine design						

e. Low-NO _x burners (LNB)	See description in Section 8.3	Generally applicable to supplementary firing for heat recovery steam generators (HRSGs) in the case of combined-cycle gas
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			turbine (CCGT) combustion plants	no firing takes place. f. Emission limits are met with DLN burners and as such SCR is not installed.						
	f. Selective catalytic reduction (SCR)		Not applicable in the case of combustion plants operated < 500 h/yr. Not generally applicable to existing combustion plants of < 100 MW _{th} . Retrofitting existing combustion plants may be constrained by the availability of sufficient space. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr							

BAT 43 prevent or reduce NO_x emissions to air	In order to prevent or reduce NO _x emissions to air from the combustion of natural gas in engines, BAT is to use one or a combination of the techniques given below.			This BAT applies to engines and therefore is not applicable to this CCGT installation.	Not applicable	Kindly specify the installation is within compliance whether the emission limit value stated in the BAT operating over the 70% load.	This BAT applies to engines and therefore is not applicable to this CCGT installation.	Agreed, however kindly indicate the attainable NO _x emissions within the BAT-AEL range for NO _x .	Kindly note that as per Commission Implementing Decision (EU) 2017/1442, Table 24 forms part of BAT 44 and not 43. Nevertheless, in terms of Table 24, as evidenced through the NO _x monitoring data collected by CEMS, EGM attains the BAT-AELs for a CCGT with a total net fuel utilisation of <75%.
	Technique	Description	Applicability						
	a. Advanced control system	See description in Section 8.3. This technique is often used in combination with other techniques or may be used alone for combustion plants operated < 500 h/yr	The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system						
	b. Lean-burn concept	See description in Section 8.3. Generally used in combination with SCR	Only applicable to new gas-fired engines						
	c. Advanced lean-burn concept	See descriptions in Section 8.3	Only applicable to new spark plug ignited engines						
	d. Selective catalytic reduction (SCR)		Retrofitting existing combustion plants may be constrained by the availability of sufficient space. Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr						
<p style="text-align: center;">Table 24</p> <p>BAT-associated emission levels (BAT-AELs) for NO_x emissions to air from the combustion of natural gas in gas turbines</p>									

Type of combustion plant	Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³) ⁽¹⁾⁽²⁾	
		Yearly average ⁽³⁾⁽⁴⁾	Daily average or average over the sampling period
Open-cycle gas turbines (OCGTs) ⁽⁵⁾⁽⁶⁾			
New OCGT	≥ 50	15–35	25–50
Existing OCGT (excluding turbines for mechanical drive applications) — All but plants operated < 500 h/yr	≥ 50	15–50	25–55 ⁽⁷⁾
Combined-cycle gas turbines (CCGTs) ⁽⁵⁾⁽⁸⁾			
New CCGT	≥ 50	10–30	15–40
Existing CCGT with a net total fuel utilisation of < 75 %	≥ 600	10–40	18–50
Existing CCGT with a net total fuel utilisation of ≥ 75 %	≥ 600	10–50	18–55 ⁽⁹⁾
Existing CCGT with a net total fuel utilisation of < 75 %	50–600	10–45	35–55
Existing CCGT with a net total fuel utilisation of ≥ 75 %	50–600	25–50 ⁽¹⁰⁾	35–55 ⁽¹¹⁾
Open- and combined-cycle gas turbines			
Gas turbine put into operation no later than 27 November 2003, or existing gas turbine for emergency use and operated < 500 h/yr	≥ 50	No BAT-AEL	0–140 ⁽¹²⁾⁽¹³⁾
Existing gas turbine for mechanical drive applications — All but plants operated < 500 h/yr	≥ 50	15–50 ⁽¹⁴⁾	25–55 ⁽¹⁵⁾
<div>(1) These BAT-AELs also apply to the combustion of natural gas in dual-fuel-fired turbines.</div> <div>(2) In the case of a gas turbine equipped with DLN, these BAT-AELs apply only when the DLN operation is effective.</div> <div>(3) These BAT-AELs do not apply to existing plants operated < 1 500 h/yr.</div> <div>(4) Optimising the functioning of an existing technique to reduce NOX emissions further may lead to levels of CO emissions at the higher end of the indicative range for CO emissions given after this table.</div>			

	<p>(5) These BAT-AELs do not apply to existing turbines for mechanical drive applications or to plants operated < 500 h/yr.</p> <p>(6) For plants with a net electrical efficiency (EE) greater than 39 %, a correction factor may be applied to the higher end of the range, corresponding to [higher end] × EE/39, where EE is the net electrical energy efficiency or net mechanical energy efficiency of the plant determined at ISO baseload conditions.</p> <p>(7) The higher end of the range is 80 mg/Nm³ in the case of plants which were put into operation no later than 27 November 2003 and are operated between 500 h/yr and 1 500 h/yr.</p> <p>(8) For plants with a net electrical efficiency (EE) greater than 55 %, a correction factor may be applied to the higher end of the BAT-AEL range, corresponding to [higher end] × EE/55, where EE is the net electrical efficiency of the plant determined at ISO baseload conditions.</p> <p>(9) For existing plants put into operation no later than 7 January 2014, the higher end of the BAT-AEL range is 65 mg/Nm³.</p> <p>(10) For existing plants put into operation no later than 7 January 2014, the higher end of the BAT-AEL range is 55 mg/Nm³.</p> <p>(11) For existing plants put into operation no later than 7 January 2014, the higher end of the BAT-AEL range is 80 mg/Nm³.</p> <p>(12) The lower end of the BAT-AEL range for NO_x can be achieved with DLN burners.</p> <p>(13) These levels are indicative.</p> <p>(14) For existing plants put into operation no later than 7 January 2014, the higher end of the BAT-AEL range is 60 mg/Nm³.</p> <p>(15) For existing plants put into operation no later than 7 January 2014, the higher end of the BAT-AEL range is 65 mg/Nm³.</p>						
BAT 44 prevent or reduce CO emissions to air	<p>In order to prevent or reduce CO emissions to air from the combustion of natural gas, BAT is to ensure optimised combustion and/or to use oxidation catalysts.</p> <p>Description</p> <p>See descriptions in Section 8.3.</p> <p>As an indication, the yearly average CO emission levels for each type of existing combustion plant operated ≥ 1 500 h/yr and for each type of new combustion plant will generally be as follows:</p> <ul style="list-style-type: none"> — New OCGT of ≥ 50 MW_{th}: < 5–40 mg/Nm³. For plants with a net electrical efficiency (EE) greater than 39 %, a correction factor may be applied to the higher end of this range, corresponding to [higher end] × EE/39, where EE is the net electrical energy efficiency or net mechanical energy efficiency of the plant determined at ISO baseload conditions. — Existing OCGT of ≥ 50 MW_{th} (excluding turbines for mechanical drive applications): < 5–40 mg/Nm³. The higher end of this range will generally be 80 mg/Nm³ in the case of existing plants that cannot be fitted with dry techniques for 	<p>GT technology utilises a high air to fuel ratio, producing a lean burn. As evidenced through the CO monitoring data collected by CEMS, CO production is well within BAT-AELs for an existing CCGT of ≥50MW_{th}.</p>	Implemented	<p>Kindly indicate status of implementation, it is to be noted that the permit will be updated to reflect the revised BAT-AEL within the range stipulated. ERA employs the strictest achievable limit within the range possible for the plant based on previous reporting data. Should EGM have a suggested indicative BAT-AEL for CO, based on plant performance kindly indicate.</p>	<p>BAT concerns CO emissions, however table provided concerns NO_x emissions. ERA to clarify.</p>	<p>Kindly note that table 24, has been moved upwards, kindly provide the indicate BAT AELs for CO.</p>	<p>Noted regarding Table 24. Kindly see EGM reply for BAT 43 above.</p> <p>Regarding CO, as evidenced through the CO monitoring data collected by CEMS, CO production is well within BAT-AELs for an existing CCGT of ≥50MW_{th}.</p>

	<p>NO_x reduction, or 50 mg/Nm³ for plants that operate at low load.</p> <p>— New CCGT of ≥ 50 MW_{th}: < 5–30 mg/Nm³. For plants with a net electrical efficiency (EE) greater than 55 %, a correction factor may be applied to the higher end of the range, corresponding to [higher end] × EE/55, where EE is the net electrical energy efficiency of the plant determined at ISO baseload conditions.</p> <p>— Existing CCGT of ≥ 50 MW_{th}: < 5–30 mg/Nm³. The higher end of this range will generally be 50 mg/Nm³ for plants that operate at low load.</p> <p>— Existing gas turbines of ≥ 50 MW_{th} for mechanical drive applications: < 5–40 mg/Nm³. The higher end of the range will generally be 50 mg/Nm³when plants operate at low load.</p> <p>In the case of a gas turbine equipped with DLN burners, these indicative levels correspond to when the DLN operation is effective.</p> <p>Table 25</p> <p>BAT-associated emission levels (BAT-AELs) for NO_x emissions to air from the combustion of natural gas in boilers and engines</p> <table><tr><th rowspan="3">Type of combustion plant</th><th colspan="4">BAT-AELs (mg/Nm³)</th></tr><tr><th colspan="2">Yearly average ⁽¹⁾</th><th colspan="2">Daily average or average over the sampling period</th></tr><tr><th>New plant</th><th>Existing plant ⁽²⁾</th><th>New plant</th><th>Existing plant ⁽³⁾</th></tr><tr><td>Boiler</td><td>10–60</td><td>50–100</td><td>30–85</td><td>85–110</td></tr><tr><td>Engine</td><td>20–75</td><td>20–100</td><td>55–85</td><td>55–110</td></tr></table> <p>(1) Optimising the functioning of an existing technique to reduce NOX emissions further may lead to levels of CO emissions at the higher end of the indicative range for CO emissions given after this table.</p> <p>(2) These BAT-AELs do not apply to plants operated < 1 500 h/yr.</p> <p>(3) For plants operated < 500 h/yr, these levels are indicative.</p> <p>(4) These BAT-AELs only apply to spark-ignited and dual-fuel engines. They do not apply to gas-diesel engines. (5) In the case of engines for emergency use operated < 500 h/yr that could not apply the lean-burn concept or use SCR, the higher end of the indicative range is 175 mg/Nm3.</p> <p>As an indication, the yearly average CO emission levels will generally be:</p> <p>— < 5–40 mg/Nm³ for existing boilers operated ≥ 1 500 h/yr,</p>	Type of combustion plant	BAT-AELs (mg/Nm ³)				Yearly average ⁽¹⁾		Daily average or average over the sampling period		New plant	Existing plant ⁽²⁾	New plant	Existing plant ⁽³⁾	Boiler	10–60	50–100	30–85	85–110	Engine	20–75	20–100	55–85	55–110							
Type of combustion plant	BAT-AELs (mg/Nm ³)																														
	Yearly average ⁽¹⁾		Daily average or average over the sampling period																												
	New plant	Existing plant ⁽²⁾	New plant	Existing plant ⁽³⁾																											
Boiler	10–60	50–100	30–85	85–110																											
Engine	20–75	20–100	55–85	55–110																											

	<ul style="list-style-type: none">— < 5–15 mg/Nm³ for new boilers,— 30–100 mg/Nm³ for existing engines operated ≥ 1 500 h/yr and for new engines.																							
BAT 45 reduce non-methane volatile organic compounds (NMVOC) and methane (CH₄)	<p>In order to reduce non-methane volatile organic compounds (NMVOC) and methane (CH₄) emissions to air from the combustion of natural gas in spark-ignited lean-burn gas engines, BAT is to ensure optimised combustion and/or to use oxidation catalysts.</p> <p><i>Description</i></p> <p>See descriptions in Section 8.3. Oxidation catalysts are not effective at reducing the emissions of saturated hydrocarbons containing less than four carbon atoms.</p> <p><i>Table 26</i></p> <p>BAT-associated emission levels (BAT-AELs) for formaldehyde and CH₄ emissions to air from the combustion of natural gas in a spark-ignited lean-burn gas engine</p> <table><tr><th rowspan="4">Combustion plant total rated thermal input (MW_{th})</th><th colspan="3">BAT-AELs (mg/Nm³)</th></tr><tr><th colspan="2">Formaldehyde</th><th>CH₄</th></tr><tr><th colspan="3">Average over the sampling period</th></tr><tr><th>New or existing plant</th><th>New plant</th><th>Existing plant</th></tr><tr><td>≥ 50</td><td>5–15 ⁽¹⁾</td><td>215–500 ⁽²⁾</td><td>215–560 ⁽¹⁾⁽²⁾</td></tr></table> <p><i>(1) For existing plants operated < 500 h/yr, these levels are indicative. (2) This BAT-AEL is expressed as C at full load operation.</i></p>	Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)			Formaldehyde		CH ₄	Average over the sampling period			New or existing plant	New plant	Existing plant	≥ 50	5–15 ⁽¹⁾	215–500 ⁽²⁾	215–560 ⁽¹⁾⁽²⁾	<p>This BAT applies to spark-ignited lean-burn gas engines and therefore is not applicable to this CCGT installation.</p>	Not applicable	<p>EGM to confirm provide with ELV with the bat AEL range for inclusion in the permit.</p>	<p>This BAT applies to spark-ignited lean-burn gas engines and therefore is not applicable to this CCGT installation.</p>	<p>Agreed.</p>	
Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)																							
	Formaldehyde		CH ₄																					
	Average over the sampling period																							
	New or existing plant	New plant	Existing plant																					
≥ 50	5–15 ⁽¹⁾	215–500 ⁽²⁾	215–560 ⁽¹⁾⁽²⁾																					

4.2. BAT conclusions for the combustion of iron and steel process gases

Unless otherwise stated, the BAT conclusions presented in this section are generally applicable to the combustion of iron and steel process gases (blast furnace gas, coke oven gas, basic oxygen furnace gas), individually, in combination, or simultaneously with other gaseous and/or liquid fuels. They apply in addition to the general BAT conclusions given in Section 1.

Bat conclusions		STATUS AT INSTALLATION: [ENTER NAME OF OPERATOR]	STATE WHETHER IT IS IN PLACE OR STATE SCHEDULE FOR IMPLEMENTATION																		
		DATE: [ENTER DATE OF ASSESSMENT]																			
		Applicability Assessment (describe how the technique applies or not to your installation)																			
BAT 46		N/A	N/A																		
Energy efficiency	<p>In order to increase the energy efficiency of the combustion of iron and steel process gases, BAT is to use an appropriate combination of the techniques given in BAT 12 and below.</p> <table><tr><th colspan="2">Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a.</td><td>Process gas management system</td><td>See description in Section 8.2</td><td>Only applicable to integrated steelworks</td></tr></table> <p>Table 27</p> <p>BAT-associated energy efficiency levels (BAT-AEELs) for the combustion of iron and steel process gases in boilers</p> <table><tr><th rowspan="2">Type of combustion unit</th><th colspan="2">BAT-AEELs ⁽¹⁾⁽²⁾</th></tr><tr><th>Net electrical efficiency (%)</th><th>Net total fuel utilisation (%) ⁽³⁾</th></tr><tr><td>Existing multi-fuel firing gas boiler</td><td>30–40</td><td>50–84</td></tr><tr><td>New multi-fuel firing gas boiler ⁽⁴⁾</td><td>36–42,5</td><td>50–84</td></tr></table> <p>(1) These BAT-AEELs do not apply in the case of units operated < 1 500 h/yr.</p> <p>(2) In the case of CHP units, only one of the two BAT-AEELs ‘Net electrical efficiency’ or ‘Net total fuel utilisation’ applies, depending on the CHP unit design (i.e. either more oriented towards electricity generation or towards heat generation).</p> <p>(3) These BAT-AEELs do not apply to plants generating only electricity.</p> <p>(4) The wide range of energy efficiencies in CHP units is largely dependent on the local demand for electricity and heat.</p>	Technique		Description	Applicability	a.	Process gas management system	See description in Section 8.2	Only applicable to integrated steelworks	Type of combustion unit	BAT-AEELs ⁽¹⁾⁽²⁾		Net electrical efficiency (%)	Net total fuel utilisation (%) ⁽³⁾	Existing multi-fuel firing gas boiler	30–40	50–84	New multi-fuel firing gas boiler ⁽⁴⁾	36–42,5	50–84	
Technique		Description	Applicability																		
a.	Process gas management system	See description in Section 8.2	Only applicable to integrated steelworks																		
Type of combustion unit	BAT-AEELs ⁽¹⁾⁽²⁾																				
	Net electrical efficiency (%)	Net total fuel utilisation (%) ⁽³⁾																			
Existing multi-fuel firing gas boiler	30–40	50–84																			
New multi-fuel firing gas boiler ⁽⁴⁾	36–42,5	50–84																			

	<div>Table 28</div> <div>BAT-associated energy efficiency levels (BAT-AEELs) for the combustion of iron and steel process gases in CCGTs</div> <table><tr><th rowspan="3">Type of combustion unit</th><th colspan="3">BAT-AEELs ⁽¹⁾⁽²⁾</th></tr><tr><th colspan="2">Net electrical efficiency (%)</th><th rowspan="2">Net total fuel utilisation (%) ⁽³⁾</th></tr><tr><th>New unit</th><th>Existing unit</th></tr><tr><td>CHP CCGT</td><td>> 47</td><td>40–48</td><td>60–82</td></tr><tr><td>CCGT</td><td>> 47</td><td>40–48</td><td>No BAT-AEEL</td></tr></table> <div>(1) These BAT-AEELs do not apply in the case of units operated < 1 500 h/yr. (2) In the case of CHP units, only one of the two BAT-AEELs ‘Net electrical efficiency’ or ‘Net total fuel utilisation’ applies, depending on the CHP unit design (i.e. either more oriented towards electricity generation or towards heat generation). (3) These BAT-AEELs do not apply to plants generating only electricity.</div>	Type of combustion unit	BAT-AEELs ⁽¹⁾⁽²⁾			Net electrical efficiency (%)		Net total fuel utilisation (%) ⁽³⁾	New unit	Existing unit	CHP CCGT	> 47	40–48	60–82	CCGT	> 47	40–48	No BAT-AEEL						
Type of combustion unit	BAT-AEELs ⁽¹⁾⁽²⁾																							
	Net electrical efficiency (%)		Net total fuel utilisation (%) ⁽³⁾																					
	New unit	Existing unit																						
CHP CCGT	> 47	40–48	60–82																					
CCGT	> 47	40–48	No BAT-AEEL																					
<div>BAT 47</div> <div>NO_x and CO emissions to air</div>	<div>In order to prevent or reduce NO_x emissions to air from the combustion of iron and steel process gases in boilers, BAT is to use one or a combination of the techniques given below.</div> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Low-NO_x burners (LNB)</td><td>See description in Section 8.3. Specially designed low-NO_x burners in multiple rows per type of fuel or including specific features for multi-fuel firing (e.g. multiple dedicated nozzles for burning different fuels, or including fuels premixing)</td><td rowspan="4">Generally applicable</td></tr><tr><td>b. Air staging</td><td rowspan="3">See descriptions in Section 8.3</td></tr><tr><td>c. Fuel staging</td></tr><tr><td>d. Flue-gas recirculation</td></tr><tr><td>e. Process gas management system</td><td>See description in Section 8.2.</td><td>Generally applicable within the constraints associated with the availability of different types of fuel</td></tr><tr><td>f. Advanced control system</td><td>See description in Section 8.3. This technique is used in combination with other techniques</td><td>The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system</td></tr><tr><td>g. Selective non-catalytic reduction (SNCR)</td><td rowspan="2">See descriptions in Section 8.3</td><td>Not applicable to combustion plants operated < 500 h/yr</td></tr><tr><td>h. Selective catalytic reduction (SCR)</td><td>Not applicable to combustion plants operated < 500 h/yr.</td></tr></table>	Technique	Description	Applicability	a. Low-NO _x burners (LNB)	See description in Section 8.3. Specially designed low-NO _x burners in multiple rows per type of fuel or including specific features for multi-fuel firing (e.g. multiple dedicated nozzles for burning different fuels, or including fuels premixing)	Generally applicable	b. Air staging	See descriptions in Section 8.3	c. Fuel staging	d. Flue-gas recirculation	e. Process gas management system	See description in Section 8.2.	Generally applicable within the constraints associated with the availability of different types of fuel	f. Advanced control system	See description in Section 8.3. This technique is used in combination with other techniques	The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system	g. Selective non-catalytic reduction (SNCR)	See descriptions in Section 8.3	Not applicable to combustion plants operated < 500 h/yr	h. Selective catalytic reduction (SCR)	Not applicable to combustion plants operated < 500 h/yr.	N/A	N/A
Technique	Description	Applicability																						
a. Low-NO _x burners (LNB)	See description in Section 8.3. Specially designed low-NO _x burners in multiple rows per type of fuel or including specific features for multi-fuel firing (e.g. multiple dedicated nozzles for burning different fuels, or including fuels premixing)	Generally applicable																						
b. Air staging	See descriptions in Section 8.3																							
c. Fuel staging																								
d. Flue-gas recirculation																								
e. Process gas management system	See description in Section 8.2.	Generally applicable within the constraints associated with the availability of different types of fuel																						
f. Advanced control system	See description in Section 8.3. This technique is used in combination with other techniques	The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system																						
g. Selective non-catalytic reduction (SNCR)	See descriptions in Section 8.3	Not applicable to combustion plants operated < 500 h/yr																						
h. Selective catalytic reduction (SCR)		Not applicable to combustion plants operated < 500 h/yr.																						

	<table><tr><td></td><td></td><td></td><td>Not generally applicable to combustion plants of < 100 MW_{th}. Retrofitting existing combustion plants may be constrained by the availability of sufficient space and by the combustion plant configuration</td></tr></table>				Not generally applicable to combustion plants of < 100 MW _{th} . Retrofitting existing combustion plants may be constrained by the availability of sufficient space and by the combustion plant configuration																		
			Not generally applicable to combustion plants of < 100 MW _{th} . Retrofitting existing combustion plants may be constrained by the availability of sufficient space and by the combustion plant configuration																				
BAT 48 prevent or reduce NO_x emissions to air	<p>In order to prevent or reduce NO_x emissions to air from the combustion of iron and steel process gases in CCGTs, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Process gas management system</td><td>See description in Section 8.2</td><td>Generally applicable within the constraints associated with the availability of different types of fuel</td></tr><tr><td>b. Advanced control system</td><td>See description in Section 8.3. This technique is used in combination with other techniques</td><td>The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system</td></tr><tr><td>c. Water/steam addition</td><td>See description in Section 8.3. In dual fuel gas turbines using DLN for the combustion of iron and steel process gases, water/steam addition is generally used when combusting natural gas</td><td>The applicability may be limited due to water availability</td></tr><tr><td>d. Dry low-NO_x burners(DLN)</td><td>See description in Section 8.3. DLN that combust iron and steel process gases differ from those that combust natural gas only</td><td>Applicable within the constraints associated with the reactivity of iron and steel process gases such as coke oven gas. The applicability may be limited in the case of turbines where a retrofit package is not available or when water/steam addition systems are installed</td></tr><tr><td>e. Low-NO_x burners (LNB)</td><td rowspan="2">See description in Section 8.3</td><td>Only applicable to supplementary firing for heat recovery steam generators (HRSGs) of combined-cycle gas turbine (CCGT) combustion plants</td></tr><tr><td>f. Selective catalytic reduction (SCR)</td><td>Retrofitting existing combustion plants may be constrained by the availability of sufficient space</td></tr></table>	Technique	Description	Applicability	a. Process gas management system	See description in Section 8.2	Generally applicable within the constraints associated with the availability of different types of fuel	b. Advanced control system	See description in Section 8.3. This technique is used in combination with other techniques	The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system	c. Water/steam addition	See description in Section 8.3. In dual fuel gas turbines using DLN for the combustion of iron and steel process gases, water/steam addition is generally used when combusting natural gas	The applicability may be limited due to water availability	d. Dry low-NO _x burners(DLN)	See description in Section 8.3. DLN that combust iron and steel process gases differ from those that combust natural gas only	Applicable within the constraints associated with the reactivity of iron and steel process gases such as coke oven gas. The applicability may be limited in the case of turbines where a retrofit package is not available or when water/steam addition systems are installed	e. Low-NO _x burners (LNB)	See description in Section 8.3	Only applicable to supplementary firing for heat recovery steam generators (HRSGs) of combined-cycle gas turbine (CCGT) combustion plants	f. Selective catalytic reduction (SCR)	Retrofitting existing combustion plants may be constrained by the availability of sufficient space	N/A	N/A
Technique	Description	Applicability																					
a. Process gas management system	See description in Section 8.2	Generally applicable within the constraints associated with the availability of different types of fuel																					
b. Advanced control system	See description in Section 8.3. This technique is used in combination with other techniques	The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system																					
c. Water/steam addition	See description in Section 8.3. In dual fuel gas turbines using DLN for the combustion of iron and steel process gases, water/steam addition is generally used when combusting natural gas	The applicability may be limited due to water availability																					
d. Dry low-NO _x burners(DLN)	See description in Section 8.3. DLN that combust iron and steel process gases differ from those that combust natural gas only	Applicable within the constraints associated with the reactivity of iron and steel process gases such as coke oven gas. The applicability may be limited in the case of turbines where a retrofit package is not available or when water/steam addition systems are installed																					
e. Low-NO _x burners (LNB)	See description in Section 8.3	Only applicable to supplementary firing for heat recovery steam generators (HRSGs) of combined-cycle gas turbine (CCGT) combustion plants																					
f. Selective catalytic reduction (SCR)		Retrofitting existing combustion plants may be constrained by the availability of sufficient space																					

<div>BAT 49</div> <div>prevent or reduce CO emissions to air</div>	In order to prevent or reduce CO emissions to air from the combustion of iron and steel process gases, BAT is to use one or a combination of the techniques given below.			N/A	N/A																						
	<table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Combustion optimisation</td><td rowspan="2">See descriptions in Section 8.3</td><td>Generally applicable</td></tr><tr><td>b. Oxidation catalysts</td><td>Only applicable to CCGTs. The applicability may be limited by lack of space, the load requirements and the sulphur content of the fuel</td></tr></table>					Technique	Description	Applicability	a. Combustion optimisation	See descriptions in Section 8.3	Generally applicable	b. Oxidation catalysts	Only applicable to CCGTs. The applicability may be limited by lack of space, the load requirements and the sulphur content of the fuel														
	Technique	Description	Applicability																								
	a. Combustion optimisation	See descriptions in Section 8.3	Generally applicable																								
	b. Oxidation catalysts		Only applicable to CCGTs. The applicability may be limited by lack of space, the load requirements and the sulphur content of the fuel																								
	Table 29																										
	BAT-associated emission levels (BAT-AELs) for NO _x emissions to air from the combustion of 100 % iron and steel process gases																										
	<table><tr><th rowspan="2">Type of combustion plant</th><th rowspan="2">O₂ reference level (vol-%)</th><th colspan="2">BAT-AELs (mg/Nm³) ⁽¹⁾</th></tr><tr><th>Yearly average</th><th>Daily average or average over the sampling period</th></tr><tr><td>New boiler</td><td>3</td><td>15–65</td><td>22–100</td></tr><tr><td>Existing boiler</td><td>3</td><td>20–100 ⁽²⁾⁽³⁾</td><td>22–110 ⁽²⁾⁽⁴⁾⁽⁵⁾</td></tr><tr><td>New CCGT</td><td>15</td><td>20–35</td><td>30–50</td></tr><tr><td>Existing CCGT</td><td>15</td><td>20–50 ⁽²⁾⁽³⁾</td><td>30–55 ⁽⁵⁾⁽⁶⁾</td></tr></table>					Type of combustion plant	O ₂ reference level (vol-%)	BAT-AELs (mg/Nm ³) ⁽¹⁾		Yearly average	Daily average or average over the sampling period	New boiler	3	15–65	22–100	Existing boiler	3	20–100 ⁽²⁾⁽³⁾	22–110 ⁽²⁾⁽⁴⁾⁽⁵⁾	New CCGT	15	20–35	30–50	Existing CCGT	15	20–50 ⁽²⁾⁽³⁾	30–55 ⁽⁵⁾⁽⁶⁾
	Type of combustion plant	O ₂ reference level (vol-%)	BAT-AELs (mg/Nm ³) ⁽¹⁾																								
			Yearly average			Daily average or average over the sampling period																					
New boiler	3	15–65	22–100																								
Existing boiler	3	20–100 ⁽²⁾⁽³⁾	22–110 ⁽²⁾⁽⁴⁾⁽⁵⁾																								
New CCGT	15	20–35	30–50																								
Existing CCGT	15	20–50 ⁽²⁾⁽³⁾	30–55 ⁽⁵⁾⁽⁶⁾																								
(1) Plants combusting a mixture of gases with an equivalent LHV of > 20 MJ/Nm3 are expected to emit at the higher end of the BAT-AEL ranges.																											
(2) The lower end of the BAT-AEL range can be achieved when using SCR.																											
(3) For plants operated < 1 500 h/yr, these BAT AELs do not apply.																											
(4) In the case of plants put into operation no later than 7 January 2014, the higher end of the BAT-AEL range is 160 mg/Nm3. Furthermore, the higher end of the BAT-AEL range may be exceeded when SCR cannot be used and when using a high share of COG (e.g. > 50 %) and/or when combusting COG with a relatively high level of H2. In this case, the higher end of the BAT-AEL range is 220 mg/Nm3.																											
(5) For plants operated < 500 h/yr, these levels are indicative.																											
(6) In the case of plants put into operation no later than 7 January 2014, the higher end of the BAT-AEL range is 70 mg/Nm3.																											
As an indication, the yearly average CO emission levels will generally be:																											
— < 5–100 mg/Nm ³ for existing boilers operated ≥ 1 500 h/yr,																											
— < 5–35 mg/Nm ³ for new boilers,																											
— < 5–20 mg/Nm ³ for existing CCGTs operated ≥ 1 500 h/yr or new CCGTs.																											

<div>BAT 50</div> <div>SO_x emissions to air</div>	<div>In order to prevent or reduce SO_x emissions to air from the combustion of iron and steel process gases, BAT is to use a combination of the techniques given below.</div> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Process gas management system and auxiliary fuel choice</td><td>See description in Section 8.2. To the extent allowed by the iron- and steel-works, maximise the use of: — a majority of blast furnace gas with a low sulphur content in the fuel diet, — a combination of fuels with a low averaged sulphur content, e.g. individual process fuels with a very low S content such as: — Blast furnace gas with a sulphur content < 10 mg/Nm³, — coke oven gas with a sulphur content < 300 mg/Nm³, — and auxiliary fuels such as: — natural gas, — liquid fuels with a sulphur content of ≤ 0,4 % (in boilers). Use of a limited amount of fuels with a higher sulphur content</td><td>Generally applicable within the constraints associated with the availability of different types of fuel</td></tr><tr><td>b. Coke oven gas pretreatment at the iron- and steel-works</td><td>Use of one of the following techniques: — desulphurisation by absorption systems, — wet oxidative desulphurisation</td><td>Only applicable to coke oven gas combustion plants</td></tr></table> <div>Table 30 BAT-associated emission levels (BAT-AELs) for SO₂ emissions to air from the combustion of 100 % iron and steel process gases</div> <table><tr><th rowspan="2">Type of combustion plant</th><th rowspan="2">O₂ reference level (%)</th><th colspan="2">BAT-AELs for SO₂ (mg/Nm³)</th></tr><tr><th>Yearly average ⁽¹⁾</th><th>Daily average or average over the sampling period ⁽²⁾</th></tr><tr><td>New or existing boiler</td><td>3</td><td>25–150</td><td>50–200 ⁽³⁾</td></tr><tr><td>New or existing CCGT</td><td>15</td><td>10–45</td><td>20–70</td></tr></table> <div>(1) For existing plants operated < 1 500 h/yr, these BAT AELs do not apply. (2) For existing plants operated < 500 h/yr, these levels are indicative. (3) The higher end of the BAT-AEL range may be exceeded when using a high share of COG (e.g. > 50 %). In this case, the higher end of the BAT-AEL range is 300 mg/Nm3.</div>	Technique	Description	Applicability	a. Process gas management system and auxiliary fuel choice	See description in Section 8.2. To the extent allowed by the iron- and steel-works, maximise the use of: — a majority of blast furnace gas with a low sulphur content in the fuel diet, — a combination of fuels with a low averaged sulphur content, e.g. individual process fuels with a very low S content such as: — Blast furnace gas with a sulphur content < 10 mg/Nm ³ , — coke oven gas with a sulphur content < 300 mg/Nm ³ , — and auxiliary fuels such as: — natural gas, — liquid fuels with a sulphur content of ≤ 0,4 % (in boilers). Use of a limited amount of fuels with a higher sulphur content	Generally applicable within the constraints associated with the availability of different types of fuel	b. Coke oven gas pretreatment at the iron- and steel-works	Use of one of the following techniques: — desulphurisation by absorption systems, — wet oxidative desulphurisation	Only applicable to coke oven gas combustion plants	Type of combustion plant	O ₂ reference level (%)	BAT-AELs for SO ₂ (mg/Nm ³)		Yearly average ⁽¹⁾	Daily average or average over the sampling period ⁽²⁾	New or existing boiler	3	25–150	50–200 ⁽³⁾	New or existing CCGT	15	10–45	20–70	N/A	N/A
Technique	Description	Applicability																								
a. Process gas management system and auxiliary fuel choice	See description in Section 8.2. To the extent allowed by the iron- and steel-works, maximise the use of: — a majority of blast furnace gas with a low sulphur content in the fuel diet, — a combination of fuels with a low averaged sulphur content, e.g. individual process fuels with a very low S content such as: — Blast furnace gas with a sulphur content < 10 mg/Nm ³ , — coke oven gas with a sulphur content < 300 mg/Nm ³ , — and auxiliary fuels such as: — natural gas, — liquid fuels with a sulphur content of ≤ 0,4 % (in boilers). Use of a limited amount of fuels with a higher sulphur content	Generally applicable within the constraints associated with the availability of different types of fuel																								
b. Coke oven gas pretreatment at the iron- and steel-works	Use of one of the following techniques: — desulphurisation by absorption systems, — wet oxidative desulphurisation	Only applicable to coke oven gas combustion plants																								
Type of combustion plant	O ₂ reference level (%)	BAT-AELs for SO ₂ (mg/Nm ³)																								
		Yearly average ⁽¹⁾	Daily average or average over the sampling period ⁽²⁾																							
New or existing boiler	3	25–150	50–200 ⁽³⁾																							
New or existing CCGT	15	10–45	20–70																							
<div>BAT 51</div> <div>Dust emissions to air</div>	<div>In order to reduce dust emissions to air from the combustion of iron and steel process gases, BAT is to use one or a combination of the techniques given below.</div>	N/A	N/A																							

Technique		Description	Applicability
a.	Fuel choice/management	Use of a combination of process gases and auxiliary fuels with a low averaged dust or ash content	Generally applicable within the constraints associated with the availability of different types of fuel
b.	Blast furnace gas pretreatment at the iron- and steel-works	Use of one or a combination of dry dedusting devices (e.g. deflectors, dust catchers, cyclones, electrostatic precipitators) and/or subsequent dust abatement (venturi scrubbers, hurdle-type scrubbers, annular gap scrubbers, wet electrostatic precipitators, disintegrators)	Only applicable if blast furnace gas is combusted
c.	Basic oxygen furnace gas pretreatment at the iron- and steel-works	Use of dry (e.g. ESP or bag filter) or wet (e.g. wet ESP or scrubber) dedusting. Further descriptions are given in the Iron and Steel BREF	Only applicable if basic oxygen furnace gas is combusted
d.	Electrostatic precipitator (ESP)	See descriptions in Section 8.5	Only applicable to combustion plants combusting a significant proportion of auxiliary fuels with a high ash content
e.	Bag filter		

Table 31

BAT-associated emission levels (BAT-AELs) for dust emissions to air from the combustion of 100 % iron and steel process gases

Type of combustion plant	BAT-AELs for dust (mg/Nm ³)	
	Yearly average ⁽¹⁾	Daily average or average over the sampling period ⁽²⁾
New or existing boiler	2–7	2–10
New or existing CCGT	2–5	2–5

(1) For existing plants operated < 1 500 h/yr, these BAT-AELs do not apply.

(2) For existing plants operated < 500 h/yr, these levels are indicative

4.3. BAT conclusions for the combustion of gaseous and/or liquid fuels on offshore platforms

Unless otherwise stated, the BAT conclusions presented in this section are generally applicable to the combustion of gaseous and/or liquid fuels on offshore platforms. They apply in addition to the general BAT conclusions given in Section 1.

Bat conclusions			STATUS AT INSTALLATION: [ENTER NAME OF OPERATOR]	STATE WHETHER IT IS IN PLACE OR STATE SCHEDULE FOR IMPLEMENTATION
			DATE: [ENTER DATE OF ASSESSMENT]	
			Applicability Assessment (describe how the technique applies or not to your installation)	
BAT 52 improve the general environmental performance	In order to improve the general environmental performance of the combustion of gaseous and/or liquid fuels on offshore platforms, BAT is to use one or a combination of the techniques given below.		N/A	N/A
	Techniques	Description		
	a. Process optimisation	Optimise the process in order to minimise the mechanical power requirements		
	b. Control pressure losses	Optimise and maintain inlet and exhaust systems in a way that keeps the pressure losses as low as possible		
	c. Load control	Operate multiple generator or compressor sets at load points which minimise emissions		
	d. Minimise the 'spinning reserve'	When running with spinning reserve for operational reliability reasons, the number of additional turbines is minimised, except in exceptional circumstances		
	e. Fuel choice	Provide a fuel gas supply from a point in the topside oil and gas process which offers a minimum range of fuel gas combustion parameters, e.g. calorific value, and minimum concentrations of sulphurous compounds to minimise SO ₂ formation. For liquid distillate fuels, preference is given to low-sulphur fuels		
	f. Injection timing	Optimise injection timing in engines		

	<table><tr><td>g.</td><td>Heat recovery</td><td>Utilisation of gas turbine/engine exhaust heat for platform heating purposes</td><td>Generally applicable to new combustion plants. In existing combustion plants, the applicability may be restricted by the level of heat demand and the combustion plant layout (space)</td></tr><tr><td>h.</td><td>Power integration of multiple gas fields/oilfields</td><td>Use of a central power source to supply a number of participating platforms located at different gas fields/oilfields</td><td>The applicability may be limited depending on the location of the different gas fields/oilfields and on the organisation of the different participating platforms, including alignment of time schedules regarding planning, start-up and cessation of production</td></tr></table>	g.	Heat recovery	Utilisation of gas turbine/engine exhaust heat for platform heating purposes	Generally applicable to new combustion plants. In existing combustion plants, the applicability may be restricted by the level of heat demand and the combustion plant layout (space)	h.	Power integration of multiple gas fields/oilfields	Use of a central power source to supply a number of participating platforms located at different gas fields/oilfields	The applicability may be limited depending on the location of the different gas fields/oilfields and on the organisation of the different participating platforms, including alignment of time schedules regarding planning, start-up and cessation of production						
g.	Heat recovery	Utilisation of gas turbine/engine exhaust heat for platform heating purposes	Generally applicable to new combustion plants. In existing combustion plants, the applicability may be restricted by the level of heat demand and the combustion plant layout (space)												
h.	Power integration of multiple gas fields/oilfields	Use of a central power source to supply a number of participating platforms located at different gas fields/oilfields	The applicability may be limited depending on the location of the different gas fields/oilfields and on the organisation of the different participating platforms, including alignment of time schedules regarding planning, start-up and cessation of production												
BAT 53 prevent or reduce NO_x emissions to air	<p>In order to prevent or reduce NO_x emissions to air from the combustion of gaseous and/or liquid fuels on offshore platforms, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Advanced control system</td><td rowspan="4">See descriptions in Section 8.3</td><td>The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system</td></tr><tr><td>b. Dry low-NO_x burners (DLN)</td><td>Applicable to new gas turbines (standard equipment) within the constraints associated with fuel quality variations. The applicability may be limited for existing gas turbines by: availability of a retrofit package (for low-load operation), complexity of the platform organisation and space availability</td></tr><tr><td>c. Lean-burn concept</td><td>Only applicable to new gas-fired engines</td></tr><tr><td>d. Low-NO_x burners (LNB)</td><td>Only applicable to boilers</td></tr></table>	Technique	Description	Applicability	a. Advanced control system	See descriptions in Section 8.3	The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system	b. Dry low-NO _x burners (DLN)	Applicable to new gas turbines (standard equipment) within the constraints associated with fuel quality variations. The applicability may be limited for existing gas turbines by: availability of a retrofit package (for low-load operation), complexity of the platform organisation and space availability	c. Lean-burn concept	Only applicable to new gas-fired engines	d. Low-NO _x burners (LNB)	Only applicable to boilers	N/A	N/A
Technique	Description	Applicability													
a. Advanced control system	See descriptions in Section 8.3	The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system													
b. Dry low-NO _x burners (DLN)		Applicable to new gas turbines (standard equipment) within the constraints associated with fuel quality variations. The applicability may be limited for existing gas turbines by: availability of a retrofit package (for low-load operation), complexity of the platform organisation and space availability													
c. Lean-burn concept		Only applicable to new gas-fired engines													
d. Low-NO _x burners (LNB)		Only applicable to boilers													
BAT 54 prevent or reduce CO emissions to air	<p>In order to prevent or reduce CO emissions to air from the combustion of gaseous and/or liquid fuels in gas turbines on offshore platforms, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Combustion optimisation</td><td rowspan="2">See descriptions in Section 8.3</td><td>Generally applicable</td></tr><tr><td>b. Oxidation catalysts</td><td>Not applicable to combustion plants operated < 500 h/yr.</td></tr></table>	Technique	Description	Applicability	a. Combustion optimisation	See descriptions in Section 8.3	Generally applicable	b. Oxidation catalysts	Not applicable to combustion plants operated < 500 h/yr.	N/A	N/A				
Technique	Description	Applicability													
a. Combustion optimisation	See descriptions in Section 8.3	Generally applicable													
b. Oxidation catalysts		Not applicable to combustion plants operated < 500 h/yr.													

			Retrofitting existing combustion plants may be constrained by the availability of sufficient space and by weight restrictions									
<p><i>Table 32</i></p> <p>BAT-associated emission levels (BAT-AELs) for NO_x emissions to air from the combustion of gaseous fuels in open-cycle gas turbines on offshore platforms</p> <table><tr><th rowspan="2">Type of combustion plant</th><th>BAT-AELs (mg/Nm³) ⁽¹⁾</th></tr><tr><th>Average over the sampling period</th></tr><tr><td>New gas turbine combusting gaseous fuels ⁽²⁾</td><td>15–50 ⁽³⁾</td></tr><tr><td>Existing gas turbine combusting gaseous fuels ⁽²⁾</td><td>< 50–350 ⁽⁴⁾</td></tr></table> <p>(1) These BAT-AELs are based on > 70 % of baseload power available on the day. (2) This includes single fuel and dual fuel gas turbines. (3) The higher end of the BAT-AEL range is 250 mg/Nm3 if DLN burners are not applicable. (4) The lower end of the BAT-AEL range can be achieved with DLN burners.</p> <p>As an indication, the average CO emission levels over the sampling period will generally be:</p> <p>— < 100 mg/Nm³ for existing gas turbines combusting gaseous fuels on offshore platforms operated ≥ 1 500 h/yr,</p> <p>— < 75 mg/Nm³ for new gas turbines combusting gaseous fuels on offshore platforms.</p>						Type of combustion plant	BAT-AELs (mg/Nm ³) ⁽¹⁾	Average over the sampling period	New gas turbine combusting gaseous fuels ⁽²⁾	15–50 ⁽³⁾	Existing gas turbine combusting gaseous fuels ⁽²⁾	< 50–350 ⁽⁴⁾
Type of combustion plant	BAT-AELs (mg/Nm ³) ⁽¹⁾											
	Average over the sampling period											
New gas turbine combusting gaseous fuels ⁽²⁾	15–50 ⁽³⁾											
Existing gas turbine combusting gaseous fuels ⁽²⁾	< 50–350 ⁽⁴⁾											

5. BAT CONCLUSIONS FOR MULTI-FUEL-FIRED PLANTS

5.1. BAT conclusions for the combustion of process fuels from the chemical industry

Unless otherwise stated, the BAT conclusions presented in this section are generally applicable to the combustion of process fuels from the chemical industry, individually, in combination, or simultaneously with other gaseous and/or liquid fuels. They apply in addition to the general BAT conclusions given in Section 1.

Bat conclusions					STATUS AT INSTALLATION: [ENTER NAME OF OPERATOR]		STATE WHETHER IT IS IN PLACE OR STATE SCHEDULE FOR IMPLEMENTATION									
					DATE: [ENTER DATE OF ASSESSMENT]											
					Applicability Assessment (describe how the technique applies or not to your installation)											
BAT 55	In order to improve the general environmental performance of the combustion of process fuels from the chemical industry in boilers, BAT is to use an appropriate combination of the techniques given in BAT 6 and below.				N/A		N/A									
General environmental performance	<table><tr><th colspan="2">Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a.</td><td>Pretreatment of process fuel from the chemical industry</td><td>Perform fuel pretreatment on and/or off the site of the combustion plant to improve the environmental performance of fuel combustion</td><td>Applicable within the constraints associated with process fuel characteristics and space availability</td></tr></table>				Technique		Description	Applicability	a.	Pretreatment of process fuel from the chemical industry	Perform fuel pretreatment on and/or off the site of the combustion plant to improve the environmental performance of fuel combustion	Applicable within the constraints associated with process fuel characteristics and space availability				
					Technique		Description	Applicability								
					a.	Pretreatment of process fuel from the chemical industry	Perform fuel pretreatment on and/or off the site of the combustion plant to improve the environmental performance of fuel combustion	Applicable within the constraints associated with process fuel characteristics and space availability								
5.1.2. Energy efficiency																
Table 33																
BAT-associated energy efficiency levels (BAT-AEELs) for the combustion of process fuels from the chemical industry in boilers																
Type of combustion unit				BAT-AEELs ¹⁾ (2)												
				Net electrical efficiency (%)		Net total fuel utilisation (%) ³⁾ (4)										
				New unit	Existing unit	New unit	Existing unit									

	<table><tr><td>Boiler using liquid process fuels from the chemical industry, including when mixed with HFO, gas oil and/or other liquid fuels</td><td>> 36,4</td><td>35,6–37,4</td><td>80–96</td><td>80–96</td></tr><tr><td>Boiler using gaseous process fuels from the chemical industry, including when mixed with natural gas and/or other gaseous fuels</td><td>39–42,5</td><td>38–40</td><td>78–95</td><td>78–95</td></tr></table> <p>(1) These BAT-AEELs do not apply to units operated < 1 500 h/yr. (2) In the case of CHP units, only one of the two BAT-AEELs ‘Net electrical efficiency’ or ‘Net total fuel utilisation’ applies, depending on the CHP unit design (i.e. either more oriented towards generation electricity or towards heat generation). (3) These BAT-AEELs may not be achievable if the potential heat demand is too low. (4) These BAT-AEELs do not apply to plants generating only electricity.</p>	Boiler using liquid process fuels from the chemical industry, including when mixed with HFO, gas oil and/or other liquid fuels	> 36,4	35,6–37,4	80–96	80–96	Boiler using gaseous process fuels from the chemical industry, including when mixed with natural gas and/or other gaseous fuels	39–42,5	38–40	78–95	78–95														
Boiler using liquid process fuels from the chemical industry, including when mixed with HFO, gas oil and/or other liquid fuels	> 36,4	35,6–37,4	80–96	80–96																					
Boiler using gaseous process fuels from the chemical industry, including when mixed with natural gas and/or other gaseous fuels	39–42,5	38–40	78–95	78–95																					
BAT 56 NO_x and CO emissions to air	<p>In order to prevent or reduce NOX emissions to air while limiting CO emissions to air from the combustion of process fuels from the chemical industry, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Low-NO_x burners (LNB)</td><td rowspan="3">See descriptions in Section 8.3</td><td rowspan="3">Generally applicable</td></tr><tr><td>b. Air staging</td></tr><tr><td>c. Fuel staging</td></tr><tr><td></td><td>See description in Section 8.3. Applying fuel staging when using liquid fuel mixtures may require a specific burner design</td><td></td></tr><tr><td>d. Flue-gas recirculation</td><td rowspan="5">See descriptions in Section 8.3</td><td>Generally applicable to new combustion plants. Applicable to existing combustion plants within the constraints associated with chemical installation safety</td></tr><tr><td>e. Water/steam addition</td><td>The applicability may be limited due to water availability</td></tr><tr><td>f. Fuel choice</td><td>Applicable within the constraints associated with the availability of different types of fuel and/or an alternative use of the process fuel</td></tr><tr><td>g. Advanced control system</td><td>The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system</td></tr><tr><td>h. Selective non-catalytic reduction (SNCR)</td><td>Applicable to existing combustion plants within the constraints associated with chemical installation safety. Not applicable to combustion plants operated < 500 h/yr. The applicability may be limited in the case of combustion plants operated between 500 h/yr and</td></tr></table>	Technique	Description	Applicability	a. Low-NO _x burners (LNB)	See descriptions in Section 8.3	Generally applicable	b. Air staging	c. Fuel staging		See description in Section 8.3. Applying fuel staging when using liquid fuel mixtures may require a specific burner design		d. Flue-gas recirculation	See descriptions in Section 8.3	Generally applicable to new combustion plants. Applicable to existing combustion plants within the constraints associated with chemical installation safety	e. Water/steam addition	The applicability may be limited due to water availability	f. Fuel choice	Applicable within the constraints associated with the availability of different types of fuel and/or an alternative use of the process fuel	g. Advanced control system	The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system	h. Selective non-catalytic reduction (SNCR)	Applicable to existing combustion plants within the constraints associated with chemical installation safety. Not applicable to combustion plants operated < 500 h/yr. The applicability may be limited in the case of combustion plants operated between 500 h/yr and	N/A	N/A
Technique	Description	Applicability																							
a. Low-NO _x burners (LNB)	See descriptions in Section 8.3	Generally applicable																							
b. Air staging																									
c. Fuel staging																									
	See description in Section 8.3. Applying fuel staging when using liquid fuel mixtures may require a specific burner design																								
d. Flue-gas recirculation	See descriptions in Section 8.3	Generally applicable to new combustion plants. Applicable to existing combustion plants within the constraints associated with chemical installation safety																							
e. Water/steam addition		The applicability may be limited due to water availability																							
f. Fuel choice		Applicable within the constraints associated with the availability of different types of fuel and/or an alternative use of the process fuel																							
g. Advanced control system		The applicability to old combustion plants may be constrained by the need to retrofit the combustion system and/or control command system																							
h. Selective non-catalytic reduction (SNCR)		Applicable to existing combustion plants within the constraints associated with chemical installation safety. Not applicable to combustion plants operated < 500 h/yr. The applicability may be limited in the case of combustion plants operated between 500 h/yr and																							

			1 500 h/yr with frequent fuel changes and frequent load variations																									
	i. Selective catalytic reduction (SCR)		Applicable to existing combustion plants within the constraints associated with duct configuration, space availability and chemical installation safety. Not applicable to combustion plants operated < 500 h/yr. There may be technical and economic restrictions for retrofitting existing combustion plants operated between 500 h/yr and 1 500 h/yr. Not generally applicable to combustion plants of < 100 MW _{th}																									
<p style="text-align: center;"><i>Table 34</i></p> <p style="text-align: center;">BAT-associated emission levels (BAT-AELs) for NO_x emissions to air from the combustion of 100 % process fuels from the chemical industry in boilers</p> <table><tr><th rowspan="3">Fuel phase used in the combustion plant</th><th colspan="4">BAT-AELs (mg/Nm³)</th></tr><tr><th colspan="2">Yearly average</th><th colspan="2">Daily average or average over the sampling period</th></tr><tr><th>New plant</th><th>Existing plant ⁽¹⁾</th><th>New plant</th><th>Existing plant ⁽²⁾</th></tr><tr><td>Mixture of gases and liquids</td><td>30–85</td><td>80–290</td><td>50–110</td><td>100–330 ⁽³⁾</td></tr><tr><td>Gases only</td><td>20–80</td><td>70–100 ⁽⁴⁾</td><td>30–100</td><td>85–110 ⁽⁵⁾</td></tr></table> <p>(1) For plants operated < 1 500 h/yr, these BAT AELs do not apply. (2) For plants operated < 500 h/yr, these levels are indicative. (3) For existing plants of ≤ 500 MW_{th} put into operation no later than 27 November 2003 using liquid fuels with a nitrogen content higher than 0,6 wt-%, the higher end of the BAT-AEL range is 380 mg/Nm₃. (4) For existing plants put into operation no later than 7 January 2014, the higher end of the BAT-AEL range is 180 mg/Nm₃. (5) For existing plants put into operation no later than 7 January 2014, the higher end of the BAT-AEL range is 210 mg/Nm₃.</p> <p>As an indication, the yearly average CO emission levels for existing plants operated ≥ 1 500 h/yr and for new plants will generally be < 5–30 mg/Nm³.</p>						Fuel phase used in the combustion plant	BAT-AELs (mg/Nm ³)				Yearly average		Daily average or average over the sampling period		New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾	Mixture of gases and liquids	30–85	80–290	50–110	100–330 ⁽³⁾	Gases only	20–80	70–100 ⁽⁴⁾	30–100	85–110 ⁽⁵⁾
Fuel phase used in the combustion plant	BAT-AELs (mg/Nm ³)																											
	Yearly average		Daily average or average over the sampling period																									
	New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾																								
Mixture of gases and liquids	30–85	80–290	50–110	100–330 ⁽³⁾																								
Gases only	20–80	70–100 ⁽⁴⁾	30–100	85–110 ⁽⁵⁾																								
BAT 57																												
SO_x, HCl and HF emissions to air	In order to reduce SOX, HCl and HF emissions to air from the combustion of process fuels from the chemical industry in boilers, BAT is to use one or a combination of the techniques given below.				N/A																							
	Technique	Description	Applicability																									

	a.	Fuel choice	See descriptions in Section 8.4	Applicable within the constraints associated with the availability of different types of fuel and/or an alternative use of the process fuel															
	b.	Boiler sorbent injection (in-furnace or in-bed)		Applicable to existing combustion plants within the constraints associated with duct configuration, space availability and chemical installation safety.															
	c.	Duct sorbent injection (DSI)		Wet FGD and seawater FGD are not applicable to combustion plants operated < 500 h/yr.															
	d.	Spray dry absorber (SDA)		There may be technical and economic restrictions for applying wet FGD or seawater FGD to combustion plants of < 300 MW _{th} , and for retrofitting combustion plants operated between 500 h/yr and 1 500 h/yr with wet FGD or seawater FGD															
	e.	Wet scrubbing	See description in Section 8.4. Wet scrubbing is used to remove HCl and HF when no wet FGD is used to reduce SO _x emissions																
	f.	Wet flue-gas desulphurisation (wet FGD)	See descriptions in Section 8.4																
	g.	Seawater FGD																	
<p><i>Table 35</i></p> <p>BAT-associated emission levels (BAT-AELs) for SO₂ emissions to air from the combustion of 100 % process fuels from the chemical industry in boilers</p> <table><tr><th rowspan="2">Type of combustion plant</th><th colspan="2">BAT-AELs (mg/Nm³)</th></tr><tr><th>Yearly average ⁽¹⁾</th><th>Daily average or average over the sampling period ⁽²⁾</th></tr><tr><td>New and existing boilers</td><td>10–110</td><td>90–200</td></tr></table> <p>(1) For existing plants operated < 1 500 h/yr, these BAT-AELs do not apply. (2) For existing plants operated < 500 h/yr, these levels are indicative.</p> <p><i>Table 36</i></p> <p>BAT-associated emission levels (BAT-AELs) for HCl and HF emissions to air from the combustion of process fuels from the chemical industry in boilers</p> <table><tr><th rowspan="3">Combustion plant total rated thermal input (MW_{th})</th><th colspan="2">BAT-AELs (mg/Nm³)</th></tr><tr><th>HCl</th><th>HF</th></tr><tr><th colspan="2">Average of samples obtained during one year</th></tr></table>					Type of combustion plant	BAT-AELs (mg/Nm ³)		Yearly average ⁽¹⁾	Daily average or average over the sampling period ⁽²⁾	New and existing boilers	10–110	90–200	Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)		HCl	HF	Average of samples obtained during one year	
Type of combustion plant	BAT-AELs (mg/Nm ³)																		
	Yearly average ⁽¹⁾	Daily average or average over the sampling period ⁽²⁾																	
New and existing boilers	10–110	90–200																	
Combustion plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)																		
	HCl	HF																	
	Average of samples obtained during one year																		

	<table><tr><td></td><td>New plant</td><td>Existing plant ⁽¹⁾</td><td>New plant</td><td>Existing plant ⁽¹⁾</td></tr><tr><td>< 100</td><td>1–7</td><td>2–15 ⁽²⁾</td><td>< 1–3</td><td>< 1–6 ⁽³⁾</td></tr><tr><td>≥ 100</td><td>1–5</td><td>1–9 ⁽²⁾</td><td>< 1–2</td><td>< 1–3 ⁽³⁾</td></tr></table> <p>(1) For plants operated < 500 h/yr, these levels are indicative. (2) In the case of plants operated < 1 500 h/yr, the higher end of the BAT-AEL range is 20 mg/Nm₃. (3) In the case of plants operated < 1 500 h/yr, the higher end of the BAT-AEL range is 7 mg/Nm₃.</p>		New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽¹⁾	< 100	1–7	2–15 ⁽²⁾	< 1–3	< 1–6 ⁽³⁾	≥ 100	1–5	1–9 ⁽²⁾	< 1–2	< 1–3 ⁽³⁾																								
	New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽¹⁾																																				
< 100	1–7	2–15 ⁽²⁾	< 1–3	< 1–6 ⁽³⁾																																				
≥ 100	1–5	1–9 ⁽²⁾	< 1–2	< 1–3 ⁽³⁾																																				
BAT 58 Dust and particulate-bound metal emissions to air	<p>In order to reduce emissions to air of dust, particulate-bound metals, and trace species from the combustion of process fuels from the chemical industry in boilers, BAT is to use one or a combination of the techniques given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Electrostatic precipitator (ESP)</td><td rowspan="2">See descriptions in Section 8.5</td><td rowspan="2">Generally applicable</td></tr><tr><td>b. Bag filter</td></tr><tr><td>c. Fuel choice</td><td>See description in Section 8.5. Use of a combination of process fuels from the chemical industry and auxiliary fuels with a low averaged dust or ash content</td><td>Applicable within the constraints associated with the availability of different types of fuel and/or an alternative use of the process fuel</td></tr><tr><td>d. Dry or semi-dry FGD system</td><td rowspan="2">See descriptions in Section 8.5. The technique is mainly used for SO_x, HCl and/or HF control</td><td rowspan="2">See applicability in BAT 57</td></tr><tr><td>e. Wet flue-gas desulphurisation (wet FGD)</td></tr></table> <p>Table 37 BAT-associated emission levels (BAT-AELs) for dust emissions to air from the combustion of mixtures of gases and liquids composed of 100 % process fuels from the chemical industry in boilers</p> <table><tr><th rowspan="3">Combustion plant total rated thermal input (MW_{th})</th><th colspan="4">BAT-AELs for dust (mg/Nm³)</th></tr><tr><th colspan="2">Yearly average</th><th colspan="2">Daily average or average over the sampling period</th></tr><tr><th>New plant</th><th>Existing plant ⁽¹⁾</th><th>New plant</th><th>Existing plant ⁽²⁾</th></tr><tr><td>< 300</td><td>2–5</td><td>2–15</td><td>2–10</td><td>2–22 ⁽³⁾</td></tr><tr><td>≥ 300</td><td>2–5</td><td>2–10 ⁽⁴⁾</td><td>2–10</td><td>2–11 ⁽³⁾</td></tr></table> <p>(1) For plants operated < 1 500 h/yr, these BAT-AELs do not apply. (2) For plants operated < 500 h/yr, these levels are indicative. (3) For plants put into operation no later than 7 January 2014, the higher end of the BAT-AEL range is 25 mg/Nm₃. (4) For plants put into operation no later than 7 January 2014, the higher end of the BAT-AEL range is 15 mg/Nm₃.</p>	Technique	Description	Applicability	a. Electrostatic precipitator (ESP)	See descriptions in Section 8.5	Generally applicable	b. Bag filter	c. Fuel choice	See description in Section 8.5. Use of a combination of process fuels from the chemical industry and auxiliary fuels with a low averaged dust or ash content	Applicable within the constraints associated with the availability of different types of fuel and/or an alternative use of the process fuel	d. Dry or semi-dry FGD system	See descriptions in Section 8.5. The technique is mainly used for SO _x , HCl and/or HF control	See applicability in BAT 57	e. Wet flue-gas desulphurisation (wet FGD)	Combustion plant total rated thermal input (MW _{th})	BAT-AELs for dust (mg/Nm ³)				Yearly average		Daily average or average over the sampling period		New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾	< 300	2–5	2–15	2–10	2–22 ⁽³⁾	≥ 300	2–5	2–10 ⁽⁴⁾	2–10	2–11 ⁽³⁾	N/A	N/A
Technique	Description	Applicability																																						
a. Electrostatic precipitator (ESP)	See descriptions in Section 8.5	Generally applicable																																						
b. Bag filter																																								
c. Fuel choice	See description in Section 8.5. Use of a combination of process fuels from the chemical industry and auxiliary fuels with a low averaged dust or ash content	Applicable within the constraints associated with the availability of different types of fuel and/or an alternative use of the process fuel																																						
d. Dry or semi-dry FGD system	See descriptions in Section 8.5. The technique is mainly used for SO _x , HCl and/or HF control	See applicability in BAT 57																																						
e. Wet flue-gas desulphurisation (wet FGD)																																								
Combustion plant total rated thermal input (MW _{th})	BAT-AELs for dust (mg/Nm ³)																																							
	Yearly average		Daily average or average over the sampling period																																					
	New plant	Existing plant ⁽¹⁾	New plant	Existing plant ⁽²⁾																																				
< 300	2–5	2–15	2–10	2–22 ⁽³⁾																																				
≥ 300	2–5	2–10 ⁽⁴⁾	2–10	2–11 ⁽³⁾																																				
BAT 59 Emissions of volatile organic compounds and polychlorinated dibenzo-dioxins and -furans to air	<p>In order to reduce emissions to air of volatile organic compounds and polychlorinated dibenzo-dioxins and -furans from the combustion of process fuels from the chemical industry in boilers, BAT is to use one or a combination of the techniques given in BAT 6 and below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr></table>	Technique	Description	Applicability	N/A	N/A																																		
Technique	Description	Applicability																																						

	a.	Activated carbon injection	See description in Section 8.5	Only applicable to combustion plants using fuels derived from chemical processes involving chlorinated substances. For the applicability of SCR and rapid quenching see BAT 56 and BAT 57		
	b.	Rapid quenching using wet scrubbing/flue-gas condenser	See description of wet scrubbing/flue-gas condenser in Section 8.4			
	c.	Selective catalytic reduction (SCR)	See description in Section 8.3. The SCR system is adapted and larger than an SCR system only used for NO _x reduction			
<i>Table 38</i>						
BAT-associated emission levels (BAT-AELs) for PCDD/F and TVOC emissions to air from the combustion of 100 % process fuels from the chemical industry in boilers						
		Pollutant	Unit	BAT-AELs		
Average over the sampling period						
		PCDD/F ⁽¹⁾	ng I-TEQ/Nm ³	< 0,012–0,036		
		TVOC	mg/Nm ³	0,6–12		
1) These BAT-AELs only apply to plants using fuels derived from chemical processes involving chlorinated substances.						

6. BAT CONCLUSIONS FOR THE CO-INCINERATION OF WASTE

Unless otherwise stated, the BAT conclusions

presented in this section are generally applicable to the co-incineration of waste in combustion plants. They apply in addition to the general BAT conclusions given in Section 1.

When waste is co-incinerated, the BAT-AELs in this section apply to the entire flue-gas volume generated.

In addition, when waste is co-incinerated together with the fuels covered by Section 2, the BAT-AELs set out in Section 2 also apply (i) to the entire flue-gas volume generated, and (ii) to the flue-gas volume resulting from the combustion of the fuels covered by that section using the mixing rule formula of Annex VI (part 4) to Directive 2010/75/EU, in which the BAT-AELs for the flue-gas volume resulting from the combustion of waste are to be determined on the basis of BAT 61.

Bat conclusions			STATUS AT INSTALLATION: [ENTER NAME OF OPERATOR]	STATE WHETHER IT IS IN PLACE OR STATE SCHEDULE FOR IMPLEMENTATION
			DATE: [ENTER DATE OF ASSESSMENT]	
			Applicability Assessment (describe how the technique applies or not to your installation)	
BAT 60 General environmental performance	In order to improve the general environmental performance of the co-incineration of waste in combustion plants, to ensure stable combustion conditions, and to reduce emissions to air, BAT is to use technique BAT 60 (a) below and a combination of the techniques given in BAT 6 and/or the other techniques below.		N/A	N/A
	Technique	Description		
	a. Waste pre-acceptance and acceptance	Implement a procedure for receiving any waste at the combustion plant according to the corresponding BAT from the Waste Treatment BREF. Acceptance criteria are set for critical parameters such as heating value, and the content of water, ash, chlorine and fluorine, sulphur, nitrogen, PCB, metals (volatile (e.g. Hg, Tl, Pb, Co, Se) and non-volatile (e.g. V, Cu, Cd, Cr, Ni)), phosphorus and alkali (when using animal by-products). Apply quality assurance systems for each waste load to guarantee the characteristics of the wastes co-incinerated and to control the values of defined critical parameters (e.g. EN 15358 for non-hazardous solid recovered fuel)		
	b. Waste selection/limitation	Careful selection of waste type and mass flow, together with limiting the percentage of the most polluted waste that can be co-incinerated. Limit the	Applicable within the constraints associated with the	

		proportion of ash, sulphur, fluorine, mercury and/or chlorine in the waste entering the combustion plant. Limitation of the amount of waste to be co-incinerated	waste management policy of the Member State		
	c. Waste mixing with the main fuel	Effective mixing of waste and the main fuel, as a heterogeneous or poorly mixed fuel stream or an uneven distribution may influence the ignition and combustion in the boiler and should be prevented	Mixing is only possible when the grinding behaviour of the main fuel and waste is similar or when the amount of waste is very small compared to the main fuel		
	d. Waste drying	Pre-drying of the waste before introducing it into the combustion chamber, with a view to maintaining the high performance of the boiler	The applicability may be limited by insufficient recoverable heat from the process, by the required combustion conditions, or by the waste moisture content		
	e. Waste pretreatment	See techniques described in the Waste Treatment and Waste Incineration BREFs, including milling, pyrolysis and gasification	See applicability in the Waste Treatment BREF and in the Waste incineration BREF		
BAT 61 prevent increased emissions from the co-incineration of waste in combustion plants	In order to prevent increased emissions from the co-incineration of waste in combustion plants, BAT is to take appropriate measures to ensure that the emissions of polluting substances in the part of the flue-gases resulting from waste co-incineration are not higher than those resulting from the application of BAT conclusions for the incineration of waste.			N/A	N/A
BAT 62 minimise the impact on residues	In order to minimise the impact on residues recycling of the co-incineration of waste in combustion plants, BAT is to maintain a good quality of gypsum, ashes and slags as well as other residues, in line with the requirements set for their recycling when the plant is not co-incinerating waste, by using one or a combination of the techniques given in BAT 60 and/or by restricting the co-incineration to waste fractions with pollutant concentrations similar to those in other combusted fuels.			N/A	N/A
BAT 63 Energy efficiency	In order to increase the energy efficiency of the co-incineration of waste, BAT is to use an appropriate combination of the techniques given in BAT 12 and BAT 19, depending on the main fuel type used and on the plant configuration. The BAT-associated energy efficiency levels (BAT-AEELs) are given in Table 8 for the co-incineration of waste with biomass and/or peat and in Table 2 for the co-incineration of waste with coal and/or lignite.			N/A	N/A

BAT 64 NO_x and CO emissions to air	In order to prevent or reduce NO _x emissions to air while limiting CO and N ₂ O emissions from the co-incineration of waste with coal and/or lignite, BAT is to use one or a combination of the techniques given in BAT 20.	N/A	N/A														
BAT 65	In order to prevent or reduce NO _x emissions to air while limiting CO and N ₂ O emissions from the co-incineration of waste with biomass and/or peat, BAT is to use one or a combination of the techniques given in BAT 24.	N/A	N/A														
BAT 66 SO_x, HCl and HF emissions to air	In order to prevent or reduce SO _x , HCl and HF emissions to air from the co-incineration of waste with coal and/or lignite, BAT is to use one or a combination of the techniques given in BAT 21.	N/A	N/A														
BAT 67	In order to prevent or reduce SO _x , HCl and HF emissions to air from the co-incineration of waste with biomass and/or peat, BAT is to use one or a combination of the techniques given in BAT 25.	N/A	N/A														
BAT 68 Dust and particulate-bound metal emissions to air	<p>In order to reduce dust and particulate-bound metal emissions to air from the co-incineration of waste with coal and/or lignite, BAT is to use one or a combination of the techniques given in BAT 22.</p> <p><i>Table 39</i></p> <p>BAT-associated emission levels (BAT-AELs) for metal emissions to air from the co-incineration of waste with coal and/or lignite</p> <table><tr><th rowspan="2">Combustion plant total rated thermal input (MW_{th})</th><th colspan="2">BAT-AELs</th><th rowspan="2">Averaging period</th></tr><tr><th>Sb + As + Pb + Cr + Co + Cu + Mn + Ni + V (mg/Nm³)</th><th>Cd + Tl (µg/Nm³)</th></tr><tr><td>< 300</td><td>0,005–0,5</td><td>5–12</td><td>Average over the sampling period</td></tr><tr><td>≥ 300</td><td>0,005–0,2</td><td>5–6</td><td>Average of samples obtained during one year</td></tr></table>	Combustion plant total rated thermal input (MW _{th})	BAT-AELs		Averaging period	Sb + As + Pb + Cr + Co + Cu + Mn + Ni + V (mg/Nm ³)	Cd + Tl (µg/Nm ³)	< 300	0,005–0,5	5–12	Average over the sampling period	≥ 300	0,005–0,2	5–6	Average of samples obtained during one year	N/A	N/A
Combustion plant total rated thermal input (MW _{th})	BAT-AELs		Averaging period														
	Sb + As + Pb + Cr + Co + Cu + Mn + Ni + V (mg/Nm ³)	Cd + Tl (µg/Nm ³)															
< 300	0,005–0,5	5–12	Average over the sampling period														
≥ 300	0,005–0,2	5–6	Average of samples obtained during one year														
BAT 69 reduce dust and particulate-bound metal emissions	<p>In order to reduce dust and particulate-bound metal emissions to air from the co-incineration of waste with biomass and/or peat, BAT is to use one or a combination of the techniques given in BAT 26.</p> <p><i>Table 40</i></p> <p>BAT-associated emission levels (BAT-AELs) for metal emissions to air from the co-incineration of waste with biomass and/or peat</p> <table><tr><th colspan="2">BAT-AELs (average of samples obtained during one year)</th></tr><tr><td>Sb + As + Pb + Cr + Co + Cu + Mn + Ni + V (mg/Nm³)</td><td>Cd+Tl (µg/Nm³)</td></tr></table>	BAT-AELs (average of samples obtained during one year)		Sb + As + Pb + Cr + Co + Cu + Mn + Ni + V (mg/Nm ³)	Cd+Tl (µg/Nm ³)	N/A	N/A										
BAT-AELs (average of samples obtained during one year)																	
Sb + As + Pb + Cr + Co + Cu + Mn + Ni + V (mg/Nm ³)	Cd+Tl (µg/Nm ³)																

	0,075–0,3	< 5																				
BAT 70	In order to reduce mercury emissions to air from the co-incineration of waste with biomass, peat, coal and/or lignite, BAT is to use one or a combination of the techniques given in BAT 23 and BAT 27			N/A																		
Mercury emissions to air					N/A																	
BAT 71	In order to reduce emissions of volatile organic compounds and polychlorinated dibenzo-dioxins and -furans to air from the co-incineration of waste with biomass, peat, coal and/or lignite, BAT is to use a combination of the techniques given in BAT 6, BAT 26 and below.			N/A																		
Emissions of volatile organic compounds and polychlorinated dibenzo-dioxins and -furans to air					N/A																	
<table><tr><th colspan="2">Technique</th><th>Description</th><th colspan="2">Applicability</th></tr><tr><td>a.</td><td>Activated carbon injection</td><td>See description in Section 8.5. This process is based on the adsorption of pollutant molecules by the activated carbon</td><td colspan="2" rowspan="2">Generally applicable</td></tr><tr><td>b.</td><td>Rapid quenching using wet scrubbing/flue-gas condenser</td><td>See description of wet scrubbing/flue-gas condenser in Section 8.4</td></tr><tr><td>c.</td><td>Selective catalytic reduction (SCR)</td><td>See description in Section 8.3. The SCR system is adapted and larger than an SCR system only used for NO_x reduction</td><td colspan="2">See applicability in BAT 20 and in BAT 24</td></tr></table>					Technique		Description	Applicability		a.	Activated carbon injection	See description in Section 8.5. This process is based on the adsorption of pollutant molecules by the activated carbon	Generally applicable		b.	Rapid quenching using wet scrubbing/flue-gas condenser	See description of wet scrubbing/flue-gas condenser in Section 8.4	c.	Selective catalytic reduction (SCR)	See description in Section 8.3. The SCR system is adapted and larger than an SCR system only used for NO _x reduction	See applicability in BAT 20 and in BAT 24	
Technique		Description	Applicability																			
a.	Activated carbon injection	See description in Section 8.5. This process is based on the adsorption of pollutant molecules by the activated carbon	Generally applicable																			
b.	Rapid quenching using wet scrubbing/flue-gas condenser	See description of wet scrubbing/flue-gas condenser in Section 8.4																				
c.	Selective catalytic reduction (SCR)	See description in Section 8.3. The SCR system is adapted and larger than an SCR system only used for NO _x reduction	See applicability in BAT 20 and in BAT 24																			
<p>Table 41</p> <p>BAT-associated emission levels (BAT-AELs) for PCDD/F and TVOC emissions to air from the co-incineration of waste with biomass, peat, coal and/or lignite</p> <table><tr><th rowspan="3">Type of combustion plant</th><th colspan="3">BAT-AELs</th></tr><tr><th>PCDD/F (ng I-TEQ/Nm³)</th><th colspan="2">TVOC (mg/Nm³)</th></tr><tr><th>Average over the sampling period</th><th>Yearly average</th><th>Daily average</th></tr><tr><td>Biomass-, peat-, coal- and/or lignite-fired combustion plant</td><td>< 0,01–0,03</td><td>< 0,1–5</td><td>0,5–10</td></tr></table>					Type of combustion plant	BAT-AELs			PCDD/F (ng I-TEQ/Nm³)	TVOC (mg/Nm³)		Average over the sampling period	Yearly average	Daily average	Biomass-, peat-, coal- and/or lignite-fired combustion plant	< 0,01–0,03	< 0,1–5	0,5–10				
Type of combustion plant	BAT-AELs																					
	PCDD/F (ng I-TEQ/Nm³)	TVOC (mg/Nm³)																				
	Average over the sampling period	Yearly average	Daily average																			
Biomass-, peat-, coal- and/or lignite-fired combustion plant	< 0,01–0,03	< 0,1–5	0,5–10																			

7. BAT CONCLUSIONS FOR GASIFICATION

Unless otherwise stated, the BAT conclusions presented in this section are generally applicable to all gasification plants directly associated to combustion plants, and to IGCC plants. They apply in addition to the general BAT conclusions given in Section 1.

Bat conclusions			STATUS AT INSTALLATION: [ENTER NAME OF OPERATOR] DATE: [ENTER DATE OF ASSESSMENT] Applicability Assessment (describe how the technique applies or not to your installation)	STATE WHETHER IT IS IN PLACE OR STATE SCHEDULE FOR IMPLEMENTATION
BAT 72 Energy efficiency	In order to increase the energy efficiency of IGCC and gasification units, BAT is to use one or a combination of the techniques given in BAT 12 and below.		N/A	N/A
	Technique	Description		
	a. Heat recovery from the gasification process	As the syngas needs to be cooled down to be cleaned further, energy can be recovered for producing additional steam to be added to the steam turbine cycle, enabling additional electrical power to be produced		
	b. Integration of gasification and combustion processes	The unit can be designed with full integration of the air supply unit (ASU) and the gas turbine, with all the air fed to the ASU being supplied (extracted) from the gas turbine compressor		
	c. Dry feedstock feeding system	Use of a dry system for feeding the fuel to the gasifier, in order to improve the energy efficiency of the gasification process		
	d. High-temperature and -pressure gasification	Use of gasification technique with high-temperature and -pressure operating parameters, in order to maximise the efficiency of energy conversion		
	e. Design improvements	Design improvements, such as:		
			Generally applicable to IGCC units	

	<table><tr><td></td><td></td><td><ul style="list-style-type: none">— modifications of the gasifier refractory and/or cooling system,— installation of an expander to recover energy from the syngas pressure drop before combustion</td><td></td></tr></table> <div>Table 42</div> <div>BAT-associated energy efficiency levels (BAT-AEELs) for gasification and IGCC units</div> <table><tr><th rowspan="3">Type of combustion unit configuration</th><th colspan="3">BAT-AEELs</th></tr><tr><th colspan="2">Net electrical efficiency (%) of an IGCC unit</th><th rowspan="2">Net total fuel utilisation (%) of a new or existing gasification unit</th></tr><tr><th>New unit</th><th>Existing unit</th></tr><tr><td>Gasification unit directly associated to a boiler without prior syngas treatment</td><td colspan="2">No BAT-AEEL</td><td>> 98</td></tr><tr><td>Gasification unit directly associated to a boiler with prior syngas treatment</td><td colspan="2">No BAT-AEEL</td><td>> 91</td></tr><tr><td>IGCC unit</td><td>No BAT-AEEL</td><td>34–46</td><td>> 91</td></tr></table>			<ul style="list-style-type: none">— modifications of the gasifier refractory and/or cooling system,— installation of an expander to recover energy from the syngas pressure drop before combustion		Type of combustion unit configuration	BAT-AEELs			Net electrical efficiency (%) of an IGCC unit		Net total fuel utilisation (%) of a new or existing gasification unit	New unit	Existing unit	Gasification unit directly associated to a boiler without prior syngas treatment	No BAT-AEEL		> 98	Gasification unit directly associated to a boiler with prior syngas treatment	No BAT-AEEL		> 91	IGCC unit	No BAT-AEEL	34–46	> 91		
		<ul style="list-style-type: none">— modifications of the gasifier refractory and/or cooling system,— installation of an expander to recover energy from the syngas pressure drop before combustion																										
Type of combustion unit configuration	BAT-AEELs																											
	Net electrical efficiency (%) of an IGCC unit		Net total fuel utilisation (%) of a new or existing gasification unit																									
	New unit	Existing unit																										
Gasification unit directly associated to a boiler without prior syngas treatment	No BAT-AEEL		> 98																									
Gasification unit directly associated to a boiler with prior syngas treatment	No BAT-AEEL		> 91																									
IGCC unit	No BAT-AEEL	34–46	> 91																									
<div>BAT 73</div> <div>NO_x and CO emissions to air</div>	<div>In order to prevent and/or reduce NO_x emissions to air while limiting CO emissions to air from IGCC plants, BAT is to use one or a combination of the techniques given below.</div> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Combustion optimisation</td><td>See description in Section 8.3</td><td>Generally applicable</td></tr><tr><td>b. Water/steam addition</td><td>See description in Section 8.3. Some intermediate-pressure steam from the steam turbine is reused for this purpose</td><td>Only applicable to the gas turbine part of the IGCC plant. The applicability may be limited due to water availability</td></tr><tr><td>c. Dry low-NO_x burners (DLN)</td><td>See description in Section 8.3</td><td>Only applicable to the gas turbine part of the IGCC plant. Generally applicable to new IGCC plants. Applicable on a case-by-case basis for existing IGCC plants, depending on the availability of a retrofit</td></tr></table>	Technique	Description	Applicability	a. Combustion optimisation	See description in Section 8.3	Generally applicable	b. Water/steam addition	See description in Section 8.3. Some intermediate-pressure steam from the steam turbine is reused for this purpose	Only applicable to the gas turbine part of the IGCC plant. The applicability may be limited due to water availability	c. Dry low-NO _x burners (DLN)	See description in Section 8.3	Only applicable to the gas turbine part of the IGCC plant. Generally applicable to new IGCC plants. Applicable on a case-by-case basis for existing IGCC plants, depending on the availability of a retrofit	N/A	N/A													
Technique	Description	Applicability																										
a. Combustion optimisation	See description in Section 8.3	Generally applicable																										
b. Water/steam addition	See description in Section 8.3. Some intermediate-pressure steam from the steam turbine is reused for this purpose	Only applicable to the gas turbine part of the IGCC plant. The applicability may be limited due to water availability																										
c. Dry low-NO _x burners (DLN)	See description in Section 8.3	Only applicable to the gas turbine part of the IGCC plant. Generally applicable to new IGCC plants. Applicable on a case-by-case basis for existing IGCC plants, depending on the availability of a retrofit																										

			package. Not applicable for syngas with a hydrogen content of > 15 %																			
	d. Syngas dilution with waste nitrogen from the air supply unit (ASU)	The ASU separates the oxygen from the nitrogen in the air, in order to supply high-quality oxygen to the gasifier. The waste nitrogen from the ASU is reused to reduce the combustion temperature in the gas turbine, by being premixed with the syngas before combustion	Only applicable when an ASU is used for the gasification process																			
	e. Selective catalytic reduction (SCR)	See description in Section 8.3	Not applicable to IGCC plants operated < 500 h/yr. Retrofitting existing IGCC plants may be constrained by the availability of sufficient space. There may be technical and economic restrictions for retrofitting existing IGCC plants operated between 500 h/yr and 1 500 h/yr																			
<p style="text-align: center;">Table 43</p> <p style="text-align: center;">BAT-associated emission levels (BAT-AELs) for NO_x emissions to air from IGCC plants</p> <table><tr><th rowspan="3">IGCC plant total rated thermal input (MW_{th})</th><th colspan="4">BAT-AELs (mg/Nm³)</th></tr><tr><th colspan="2">Yearly average</th><th colspan="2">Daily average or average over the sampling period</th></tr><tr><th>New plant</th><th>Existing plant</th><th>New plant</th><th>Existing plant</th></tr><tr><td>≥ 100</td><td>10–25</td><td>12–45</td><td>1–35</td><td>1–60</td></tr></table> <p>As an indication, the yearly average CO emission levels for existing plants operated ≥ 1 500 h/yr and for new plants will generally be < 5–30 mg/Nm³.</p>					IGCC plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)				Yearly average		Daily average or average over the sampling period		New plant	Existing plant	New plant	Existing plant	≥ 100	10–25	12–45	1–35	1–60
IGCC plant total rated thermal input (MW _{th})	BAT-AELs (mg/Nm ³)																					
	Yearly average		Daily average or average over the sampling period																			
	New plant	Existing plant	New plant	Existing plant																		
≥ 100	10–25	12–45	1–35	1–60																		
BAT 74 SO_x emissions to air	<p>In order to reduce SO_x emissions to air from IGCC plants, BAT is to use the technique given below.</p> <table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Acid gas removal</td><td>Sulphur compounds from the feedstock of a gasification process are removed from the syngas via acid gas removal, e.g. including a COS (and HCN) hydrolysis reactor and the absorption of H₂S using a solvent such as methyl diethanolamine. Sulphur is then recovered as either liquid or solid elemental sulphur (e.g. through a Claus unit), or as sulphuric acid, depending on market demands</td><td>The applicability may be limited in the case of biomass IGCC plants due to the very low sulphur content in biomass</td></tr></table> <p>The BAT-associated emission level (BAT-AEL) for SO₂ emissions to air from IGCC plants of ≥ 100 MW_{th} is 3–16 mg/Nm³, expressed as a yearly average.</p>				Technique	Description	Applicability	a. Acid gas removal	Sulphur compounds from the feedstock of a gasification process are removed from the syngas via acid gas removal, e.g. including a COS (and HCN) hydrolysis reactor and the absorption of H ₂ S using a solvent such as methyl diethanolamine. Sulphur is then recovered as either liquid or solid elemental sulphur (e.g. through a Claus unit), or as sulphuric acid, depending on market demands	The applicability may be limited in the case of biomass IGCC plants due to the very low sulphur content in biomass												
Technique	Description	Applicability																				
a. Acid gas removal	Sulphur compounds from the feedstock of a gasification process are removed from the syngas via acid gas removal, e.g. including a COS (and HCN) hydrolysis reactor and the absorption of H ₂ S using a solvent such as methyl diethanolamine. Sulphur is then recovered as either liquid or solid elemental sulphur (e.g. through a Claus unit), or as sulphuric acid, depending on market demands	The applicability may be limited in the case of biomass IGCC plants due to the very low sulphur content in biomass																				
	N/A																					
	N/A																					

BAT 75 Dust, particulate-bound metal, ammonia and halogen emissions to air	In order to prevent or reduce dust, particulate-bound metal, ammonia and halogen emissions to air from IGCC plants, BAT is to use one or a combination of the techniques given below.			N/A	N/A										
	<table><tr><th>Technique</th><th>Description</th><th>Applicability</th></tr><tr><td>a. Syngas filtration</td><td>Dedusting using fly ash cyclones, bag filters, ESPs and/or candle filters to remove fly ash and unconverted carbon. Bag filters and ESPs are used in the case of syngas temperatures up to 400 °C</td><td rowspan="3">Generally applicable</td></tr><tr><td>b. Syngas tars and ashes recirculation to the gasifier</td><td>Tars and ashes with a high carbon content generated in the raw syngas are separated in cyclones and recirculated to the gasifier, in the case of a low syngas temperature at the gasifier outlet (< 1 100 °C)</td></tr><tr><td>c. Syngas washing</td><td>Syngas passes through a water scrubber, downstream of other dedusting technique(s), where chlorides, ammonia, particles and halides are separated</td></tr></table>					Technique	Description	Applicability	a. Syngas filtration	Dedusting using fly ash cyclones, bag filters, ESPs and/or candle filters to remove fly ash and unconverted carbon. Bag filters and ESPs are used in the case of syngas temperatures up to 400 °C	Generally applicable	b. Syngas tars and ashes recirculation to the gasifier	Tars and ashes with a high carbon content generated in the raw syngas are separated in cyclones and recirculated to the gasifier, in the case of a low syngas temperature at the gasifier outlet (< 1 100 °C)	c. Syngas washing	Syngas passes through a water scrubber, downstream of other dedusting technique(s), where chlorides, ammonia, particles and halides are separated
	Technique	Description	Applicability												
	a. Syngas filtration	Dedusting using fly ash cyclones, bag filters, ESPs and/or candle filters to remove fly ash and unconverted carbon. Bag filters and ESPs are used in the case of syngas temperatures up to 400 °C	Generally applicable												
	b. Syngas tars and ashes recirculation to the gasifier	Tars and ashes with a high carbon content generated in the raw syngas are separated in cyclones and recirculated to the gasifier, in the case of a low syngas temperature at the gasifier outlet (< 1 100 °C)													
c. Syngas washing	Syngas passes through a water scrubber, downstream of other dedusting technique(s), where chlorides, ammonia, particles and halides are separated														
<p><i>Table 44</i></p> <p>BAT-associated emission levels (BAT-AELs) for dust and particulate-bound metal emissions to air from IGCC plants</p>															
<table><tr><th rowspan="2">IGCC plant total rated thermal input (MW_{th})</th><th colspan="3">BAT-AELs</th></tr><tr><th>Sb + As + Pb + Cr + Co + Cu + Mn + Ni + V (mg/Nm³) (Average over the sampling period)</th><th>Hg (µg/Nm³) (Average over the sampling period)</th><th>Dust (mg/Nm³) (yearly average)</th></tr><tr><td>≥ 100</td><td>< 0,025</td><td>< 1</td><td>< 2,5</td></tr></table>			IGCC plant total rated thermal input (MW _{th})	BAT-AELs			Sb + As + Pb + Cr + Co + Cu + Mn + Ni + V (mg/Nm ³) (Average over the sampling period)	Hg (µg/Nm ³) (Average over the sampling period)	Dust (mg/Nm ³) (yearly average)	≥ 100	< 0,025	< 1	< 2,5		
IGCC plant total rated thermal input (MW _{th})	BAT-AELs														
	Sb + As + Pb + Cr + Co + Cu + Mn + Ni + V (mg/Nm ³) (Average over the sampling period)	Hg (µg/Nm ³) (Average over the sampling period)	Dust (mg/Nm ³) (yearly average)												
≥ 100	< 0,025	< 1	< 2,5												

8. DESCRIPTION OF TECHNIQUES

8.1. General techniques

Technique	Description
Advanced control system	The use of a computer-based automatic system to control the combustion efficiency and support the prevention and/or reduction of emissions. This also includes the use of high-performance monitoring.
Combustion optimisation	Measures taken to maximise the efficiency of energy conversion, e.g. in the furnace/boiler, while minimising emissions (in particular of CO). This is achieved by a combination of techniques including good design of the combustion equipment, optimisation of the temperature (e.g. efficient mixing of the fuel and combustion air) and residence time in the combustion zone, and use of an advanced control system.

8.2. Techniques to increase energy efficiency

Technique	Description
Advanced control system	See Section 8.1
CHP readiness	The measures taken to allow the later export of a useful quantity of heat to an off-site heat load in a way that will achieve at least a 10 % reduction in primary energy usage compared to the separate generation of the heat and power produced. This includes identifying and retaining access to specific points in the steam system from which steam can be extracted, as well as making sufficient space available to allow the later fitting of items such as pipework, heat exchangers, extra water demineralisation capacity, standby boiler plant and back-pressure turbines. Balance of Plant (BoP) systems and control/instrumentation systems are suitable for upgrade. Later connection of back-pressure turbine(s) is also possible.
Combined cycle	Combination of two or more thermodynamic cycles, e.g. a Brayton cycle (gas turbine/combustion engine) with a Rankine cycle (steam turbine/boiler), to convert heat loss from the flue-gas of the first cycle to useful energy by subsequent cycle(s).
Combustion optimisation	See Section 8.1
Flue-gas condenser	A heat exchanger where water is preheated by the flue-gas before it is heated in the steam condenser. The vapour content in the flue-gas thus condenses as it is cooled by the heating water. The flue-gas condenser is used both to increase the energy efficiency of the combustion unit and to remove pollutants such as dust, SO _x , HCl, and HF from the flue-gas.
Process gas management system	A system that enables the iron and steel process gases that can be used as fuels (e.g. blast furnace, coke oven, basic oxygen furnace gases) to be directed to the combustion plants, depending on the availability of these fuels and on the type of combustion plants in an integrated steelworks.
Supercritical steam conditions	The use of a steam circuit, including steam reheating systems, in which steam can reach pressures above 220,6 bar and temperatures of > 540 °C.
Ultra-supercritical steam conditions	The use of a steam circuit, including reheat systems, in which steam can reach pressures above 250–300 bar and temperatures above 580–600 °C.
Wet stack	The design of the stack in order to enable water vapour condensation from the saturated flue-gas and thus to avoid using a flue-gas reheater after the wet FGD.

8.3. Techniques to reduce emissions of NO_x and/or CO to air

Technique	Description
Advanced control system	See Section 8.1

Air staging	The creation of several combustion zones in the combustion chamber with different oxygen contents for reducing NO _x emissions and ensuring optimised combustion. The technique involves a primary combustion zone with substoichiometric firing (i.e. with deficiency of air) and a second reburn combustion zone (running with excess air) to improve combustion. Some old, small boilers may require a capacity reduction to allow the space for air staging.
Combined techniques for NO _x and SO _x reduction	The use of complex and integrated abatement techniques for combined reduction of NO _x , SO _x and, often, other pollutants from the flue-gas, e.g. activated carbon and DeSONO _x processes. They can be applied either alone or in combination with other primary techniques in coal-fired PC boilers.
Combustion optimisation	See Section 8.1
Dry low-NO _x burners (DLN)	Gas turbine burners that include the premixing of the air and fuel before entering the combustion zone. By mixing air and fuel before combustion, a homogeneous temperature distribution and a lower flame temperature are achieved, resulting in lower NO _x emissions.
Flue-gas or exhaust-gas recirculation (FGR/EGR)	Recirculation of part of the flue-gas to the combustion chamber to replace part of the fresh combustion air, with the dual effect of cooling the temperature and limiting the O ₂ content for nitrogen oxidation, thus limiting the NO _x generation. It implies the supply of flue-gas from the furnace into the flame to reduce the oxygen content and therefore the temperature of the flame. The use of special burners or other provisions is based on the internal recirculation of combustion gases which cool the root of the flames and reduce the oxygen content in the hottest part of the flames.
Fuel choice	The use of fuel with a low nitrogen content.
Fuel staging	The technique is based on the reduction of the flame temperature or localised hot spots by the creation of several combustion zones in the combustion chamber with different injection levels of fuel and air. The retrofit may be less efficient in smaller plants than in larger plants.
Lean-burn concept and advanced lean-burn concept	The control of the peak flame temperature through lean-burn conditions is the primary combustion approach to limiting NO _x formation in gas engines. Lean combustion decreases the fuel to air ratio in the zones where NO _x is generated so that the peak flame temperature is less than the stoichiometric adiabatic flame temperature, therefore reducing thermal NO _x formation. The optimisation of this concept is called the 'advanced lean-burn concept'.
Low-NO _x burners (LNB)	The technique (including ultra- or advanced low-NO _x burners) is based on the principles of reducing peak flame temperatures; boiler burners are designed to delay but improve the combustion and increase the heat transfer (increased emissivity of the flame). The air/fuel mixing reduces the availability of oxygen and reduces the peak flame temperature, thus retarding the conversion of fuel-bound nitrogen to NO _x and the formation of thermal NO _x , while maintaining high combustion efficiency. It may be associated with a modified design of the furnace combustion chamber. The design of ultra-low-NO _x burners (ULNBs) includes combustion staging (air/fuel) and firebox gases' recirculation (internal flue-gas recirculation). The performance of the technique may be influenced by the boiler design when retrofitting old plants.
Low-NO _x combustion concept in diesel engines	The technique consists of a combination of internal engine modifications, e.g. combustion and fuel injection optimisation (the very late fuel injection timing in combination with early inlet air valve closing), turbocharging or Miller cycle.
Oxidation catalysts	The use of catalysts (that usually contain precious metals such as palladium or platinum) to oxidise carbon monoxide and unburnt hydrocarbons with oxygen to form CO ₂ and water vapour.
Reduction of the combustion air temperature	The use of combustion air at ambient temperature. The combustion air is not preheated in a regenerative air preheater.
Selective catalytic reduction (SCR)	Selective reduction of nitrogen oxides with ammonia or urea in the presence of a catalyst. The technique is based on the reduction of NO _x to nitrogen in a catalytic bed by reaction with ammonia (in general aqueous solution) at an optimum operating temperature of around 300–450 °C. Several layers of catalyst may be applied. A higher NO _x reduction is achieved with the use of several catalyst layers. The technique design can be modular, and special catalysts and/or preheating can be used to cope with low loads or with a wide flue-gas temperature window. 'In-duct' or 'slip' SCR is a technique that combines SNCR with downstream SCR which reduces the ammonia slip from the SNCR unit.

Selective non-catalytic reduction (SNCR)	Selective reduction of nitrogen oxides with ammonia or urea without a catalyst. The technique is based on the reduction of NO _x to nitrogen by reaction with ammonia or urea at a high temperature. The operating temperature window is maintained between 800 °C and 1000 °C for optimal reaction.
Water/steam addition	Water or steam is used as a diluent for reducing the combustion temperature in gas turbines, engines or boilers and thus the thermal NO _x formation. It is either premixed with the fuel prior to its combustion (fuel emulsion, humidification or saturation) or directly injected in the combustion chamber (water/steam injection).

8.4. Techniques to reduce emissions of SO_x, HCl and/or HF to air

Technique	Description
Boiler sorbent injection (in-furnace or in-bed)	The direct injection of a dry sorbent into the combustion chamber, or the addition of magnesium- or calcium-based adsorbents to the bed of a fluidised bed boiler. The surface of the sorbent particles reacts with the SO ₂ in the flue-gas or in the fluidised bed boiler. It is mostly used in combination with a dust abatement technique.
Circulating fluidised bed (CFB) dry scrubber	Flue-gas from the boiler air preheater enters the CFB absorber at the bottom and flows vertically upwards through a Venturi section where a solid sorbent and water are injected separately into the flue-gas stream. It is mostly used in combination with a dust abatement technique.
Combined techniques for NO _x and SO _x reduction	See Section 8.3
Duct sorbent injection (DSI)	The injection and dispersion of a dry powder sorbent in the flue-gas stream. The sorbent (e.g. sodium carbonate, sodium bicarbonate, hydrated lime) reacts with acid gases (e.g. the gaseous sulphur species and HCl) to form a solid which is removed with dust abatement techniques (bag filter or electrostatic precipitator). DSI is mostly used in combination with a bag filter.
Flue-gas condenser	See Section 8.2
Fuel choice	The use of a fuel with a low sulphur, chlorine and/or fluorine content
Process gas management system	See Section 8.2
Seawater FGD	A specific non-regenerative type of wet scrubbing using the natural alkalinity of the seawater to absorb the acidic compounds in the flue-gas. Generally requires an upstream abatement of dust.
Spray dry absorber (SDA)	A suspension/solution of an alkaline reagent is introduced and dispersed in the flue-gas stream. The material reacts with the gaseous sulphur species to form a solid which is removed with dust abatement techniques (bag filter or electrostatic precipitator). SDA is mostly used in combination with a bag filter.
Wet flue-gas desulphurisation (wet FGD)	Technique or combination of scrubbing techniques by which sulphur oxides are removed from flue-gases through various processes generally involving an alkaline sorbent for capturing gaseous SO ₂ and transforming it into solids. In the wet scrubbing process, gaseous compounds are dissolved in a suitable liquid (water or alkaline solution). Simultaneous removal of solid and gaseous compounds may be achieved. Downstream of the wet scrubber, the flue-gases are saturated with water and separation of the droplets is required before discharging the flue-gases. The liquid resulting from the wet scrubbing is sent to a waste water treatment plant and the insoluble matter is collected by sedimentation or filtration.
Wet scrubbing	Use of a liquid, typically water or an aqueous solution, to capture the acidic compounds from the flue-gas by absorption.

8.5. Techniques to reduce emissions to air of dust, metals including mercury, and/or PCDD/F

Technique	Description
Bag filter	Bag or fabric filters are constructed from porous woven or felted fabric through which gases are passed to remove particles. The use of a bag filter requires the selection of a fabric suitable for the characteristics of the flue-gas and the maximum operating temperature.

Boiler sorbent injection (in-furnace or in-bed)	See general description in Section 8.4. There are co-benefits in the form of dust and metal emissions reduction.
Carbon sorbent (e.g. activated carbon or halogenated activated carbon) injection in the flue-gas	Mercury and/or PCDD/F adsorption by carbon sorbents, such as (halogenated) activated carbon, with or without chemical treatment. The sorbent injection system can be enhanced by the addition of a supplementary bag filter.
Dry or semi-dry FGD system	See general description of each technique (i.e. spray dry absorber (SDA), duct sorbent injection (DSI), circulating fluidised bed (CFB) dry scrubber) in Section 8.4. There are co-benefits in the form of dust and metal emissions reduction.
Electrostatic precipitator (ESP)	Electrostatic precipitators operate such that particles are charged and separated under the influence of an electrical field. Electrostatic precipitators are capable of operating under a wide range of conditions. The abatement efficiency typically depends on the number of fields, the residence time (size), catalyst properties, and upstream particle removal devices. ESPs generally include between two and five fields. The most modern (high-performance) ESPs have up to seven fields.
Fuel choice	The use of a fuel with a low ash or metals (e.g. mercury) content.
Multicyclones	Set of dust control systems, based on centrifugal force, whereby particles are separated from the carrier gas, assembled in one or several enclosures.
Use of halogenated additives in the fuel or injected in the furnace	Addition of halogen compounds (e.g. brominated additives) into the furnace to oxidise elemental mercury into soluble or particulate species, thereby enhancing mercury removal in downstream abatement systems.
Wet flue-gas desulphurisation (wet FGD)	See general description in Section 8.4. There are co-benefits in the form of dust and metals emission reduction.

8.6. Techniques to reduce emissions to water

Technique	Description
Adsorption on activated carbon	The retention of soluble pollutants on the surface of solid, highly porous particles (the adsorbent). Activated carbon is typically used for the adsorption of organic compounds and mercury.
Aerobic biological treatment	The biological oxidation of dissolved organic pollutants with oxygen using the metabolism of microorganisms. In the presence of dissolved oxygen — injected as air or pure oxygen — the organic components are mineralised into carbon dioxide and water or are transformed into other metabolites and biomass. Under certain conditions, aerobic nitrification also takes place whereby microorganisms oxidise ammonium (NH_4^+) to the intermediate nitrite (NO_2^-), which is then further oxidised to nitrate (NO_3^-).
Anoxic/anaerobic biological treatment	The biological reduction of pollutants using the metabolism of microorganisms (e.g. nitrate (NO_3^-) is reduced to elemental gaseous nitrogen, oxidised species of mercury are reduced to elemental mercury). The anoxic/anaerobic treatment of waste water from the use of wet abatement systems is typically carried out in fixed-film bioreactors using activated carbon as a carrier. The anoxic/anaerobic biological treatment for the removal of mercury is applied in combination with other techniques.
Coagulation and flocculation	Coagulation and flocculation are used to separate suspended solids from waste water and are often carried out in successive steps. Coagulation is carried out by adding coagulants with charges opposite to those of the suspended solids. Flocculation is carried out by adding polymers, so that collisions of microfloc particles cause them to bond thereby producing larger flocs.
Crystallisation	The removal of ionic pollutants from waste water by crystallising them on a seed material such as sand or minerals, in a fluidised bed process
Filtration	The separation of solids from waste water by passing it through a porous medium. It includes different types of techniques, e.g. sand filtration, microfiltration and ultrafiltration.

Flotation	The separation of solid or liquid particles from waste water by attaching them to fine gas bubbles, usually air. The buoyant particles accumulate at the water surface and are collected with skimmers.
Ion exchange	The retention of ionic pollutants from waste water and their replacement by more acceptable ions using an ion exchange resin. The pollutants are temporarily retained and afterwards released into a regeneration or backwashing liquid.
Neutralisation	The adjustment of the pH of the waste water to the neutral pH level (approximately 7) by adding chemicals. Sodium hydroxide (NaOH) or calcium hydroxide ($\text{Ca}(\text{OH})_2$) is generally used to increase the pH whereas sulphuric acid (H_2SO_4), hydrochloric acid (HCl) or carbon dioxide (CO_2) is generally used to decrease the pH. The precipitation of some pollutants may occur during neutralisation.

9. DEFINITIONS:

For the purposes of these BAT conclusions, the following definitions apply

Term used	Definition
General terms	
Boiler	Any combustion plant with the exception of engines, gas turbines, and process furnaces or heaters
Combined-cycle gas turbine (CCGT)	<p>A CCGT is a combustion plant where two thermodynamic cycles are used (i.e. Brayton and Rankine cycles). In a CCGT, heat from the flue-gas of a gas turbine (operating according to the Brayton cycle to produce electricity) is converted to useful energy in a heat recovery steam generator (HRSG), where it is used to generate steam, which then expands in a steam turbine (operating according to the Rankine cycle to produce additional electricity).</p> <p>For the purpose of these BAT conclusions, a CCGT includes configurations both with and without supplementary firing of the HRSG</p>
Combustion plant	<p>Any technical apparatus in which fuels are oxidised in order to use the heat thus generated. For the purposes of these BAT conclusions, a combination formed of</p> <ul style="list-style-type: none"> — two or more separate combustion plants where the flue-gases are discharged through a common stack, or — separate combustion plants that have been granted a permit for the first time on or after 1 July 1987, or for which the operators have submitted a complete application for a permit on or after that date, which are installed in such a way that, taking technical and economic factors into account, their flue-gases could, in the judgment of the competent authority, be discharged through a common stack <p>is considered as a single combustion plant.</p> <p>For calculating the total rated thermal input of such a combination, the capacities of all individual combustion plants concerned, which have a rated thermal input of at least 15 MW, shall be added together</p>
Combustion unit	Individual combustion plant
Continuous measurement	Measurement using an automated measuring system permanently installed on site
Direct discharge	Discharge (to a receiving water body) at the point where the emission leaves the installation without further downstream treatment
Flue-gas desulphurisation (FGD) system	System composed of one or a combination of abatement technique(s) whose purpose is to reduce the level of SO _x emitted by a combustion plant
Flue-gas desulphurisation (FGD) system — existing	A flue-gas desulphurisation (FGD) system that is not a new FGD system
Flue-gas desulphurisation (FGD) system — new	Either a flue-gas desulphurisation (FGD) system in a new plant or a FGD system that includes at least one abatement technique introduced or completely replaced in an existing plant following the publication of these BAT conclusions
Gas oil	<p>Any petroleum-derived liquid fuel falling within CN code 2710 19 25, 2710 19 29, 2710 19 47, 2710 19 48, 2710 20 17 or 2710 20 19.</p> <p>Or any petroleum-derived liquid fuel of which less than 65 vol-% (including losses) distils at 250 °C and of which at least 85 vol-% (including losses) distils at 350 °C by the ASTM D86 method</p>
Heavy fuel oil (HFO)	Any petroleum-derived liquid fuel falling within CN code 2710 19 51 to 2710 19 68, 2710 20 31, 2710 20 35, 2710 20 39.

	Or any petroleum-derived liquid fuel, other than gas oil, which, by reason of its distillation limits, falls within the category of heavy oils intended for use as fuel and of which less than 65 vol-% (including losses) distils at 250 °C by the ASTM D86 method. If the distillation cannot be determined by the ASTM D86 method, the petroleum product is also categorised as a heavy fuel oil
Net electrical efficiency (combustion unit and IGCC)	Ratio between the net electrical output (electricity produced on the high-voltage side of the main transformer minus the imported energy — e.g. for auxiliary systems' consumption) and the fuel/feedstock energy input (as the fuel/feedstock lower heating value) at the combustion unit boundary over a given period of time
Net mechanical energy efficiency	Ratio between the mechanical power at load coupling and the thermal power supplied by the fuel
Net total fuel utilisation (combustion unit and IGCC)	Ratio between the net produced energy (electricity, hot water, steam, mechanical energy produced minus the imported electrical and/or thermal energy (e.g. for auxiliary systems' consumption)) and the fuel energy input (as the fuel lower heating value) at the combustion unit boundary over a given period of time
Net total fuel utilisation (gasification unit)	Ratio between the net produced energy (electricity, hot water, steam, mechanical energy produced, and syngas (as the syngas lower heating value) minus the imported electrical and/or thermal energy (e.g. for auxiliary systems' consumption)) and the fuel/feedstock energy input (as the fuel/feedstock lower heating value) at the gasification unit boundary over a given period of time
Operated hours	The time, expressed in hours, during which a combustion plant, in whole or in part, is operated and is discharging emissions to air, excluding start-up and shutdown periods
Periodic measurement	Determination of a measurand (a particular quantity subject to measurement) at specified time intervals
Plant — existing	A combustion plant that is not a new plant
Plant — new	A combustion plant first permitted at the installation following the publication of these BAT conclusions or a complete replacement of a combustion plant on the existing foundations following the publication of these BAT conclusions
Post-combustion plant	System designed to purify the flue-gases by combustion which is not operated as an independent combustion plant, such as a thermal oxidiser (i.e. tail gas incinerator), used for the removal of the pollutant(s) (e.g. VOC) content from the flue-gas with or without the recovery of the heat generated therein. Staged combustion techniques, where each combustion stage is confined within a separate chamber, which may have distinct combustion process characteristics (e.g. fuel to air ratio, temperature profile), are considered integrated in the combustion process and are not considered post-combustion plants. Similarly, when gases generated in a process heater/furnace or in another combustion process are subsequently oxidised in a distinct combustion plant to recover their energetic value (with or without the use of auxiliary fuel) to produce electricity, steam, hot water/oil or mechanical energy, the latter plant is not considered a post-combustion plant
Predictive emissions monitoring system (PEMS)	System used to determine the emissions concentration of a pollutant from an emission source on a continuous basis, based on its relationship with a number of characteristic continuously monitored process parameters (e.g. the fuel gas consumption, the air to fuel ratio) and fuel or feed quality data (e.g. the sulphur content)
Process fuels from the chemical industry	Gaseous and/or liquid by-products generated by the (petro-)chemical industry and used as non-commercial fuels in combustion plants

Process furnaces or heaters	<p>Process furnaces or heaters are:</p> <p>— combustion plants whose flue-gases are used for the thermal treatment of objects or feed material through a direct contact heating mechanism (e.g. cement and lime kiln, glass furnace, asphalt kiln, drying process, reactor used in the (petro-)chemical industry, ferrous metal processing furnaces), or</p> <p>— combustion plants whose radiant and/or conductive heat is transferred to objects or feed material through a solid wall without using an intermediary heat transfer fluid (e.g. coke battery furnace, cowper, furnace or reactor heating a process stream used in the (petro-)chemical industry such as a steam cracker furnace, process heater used for the regasification of liquefied natural gas (LNG) in LNG terminals).</p> <p>As a consequence of the application of good energy recovery practices, process heaters/furnaces may have an associated steam/electricity generation system. This is considered to be an integral design feature of the process heater/furnace that cannot be considered in isolation</p>
Refinery fuels	Solid, liquid or gaseous combustible material from the distillation and conversion steps of the refining of crude oil. Examples are refinery fuel gas (RFG), syngas, refinery oils, and pet coke
Residues	Substances or objects generated by the activities covered by the scope of this document, as waste or by-products
Start-up and shut-down period	The time period of plant operation as determined pursuant to the provisions of Commission Implementing Decision 2012/249/EU (*)
Unit — existing	A combustion unit that is not a new unit
Unit- new	A combustion unit first permitted at the combustion plant following the publication of these BAT conclusions or a complete replacement of a combustion unit on the existing foundations of the combustion plant following the publication of these BAT conclusions
Valid (hourly average)	An hourly average is considered valid when there is no maintenance or malfunction of the automated measuring system

(*) Commission Implementing Decision 2012/249/EU of 7 May 2012 concerning the determination of start-up and shut-down periods for the purposes of Directive 2010/75/EU of the European Parliament and of the Council on industrial emissions (OJ L 123, 9.5.2012, p. 44).

DEFINITIONS

For the purposes of these BAT conclusions, the following **definitions** apply:

Term used	Definition
General terms	
Pollutants/parameters	
As	The sum of arsenic and its compounds, expressed as As.
C ₃	Hydrocarbons having a carbon number equal to three

C ₄ +	Hydrocarbons having a carbon number of four or greater
Cd	The sum of cadmium and its compounds, expressed as Cd.
Cd+Tl	The sum of cadmium, thallium and their compounds, expressed as Cd+Tl.
CH ₄	Methane
CO	Carbon monoxide.
COD	Chemical oxygen demand. Amount of oxygen needed for the total oxidation of the organic matter to carbon dioxide
COS	Carbonyl sulphide
Cr	The sum of chromium and its compounds, expressed as Cr.
Cu	The sum of copper and its compounds, expressed as Cu.
Dust	Total particulate matter (in air).
Fluoride	Dissolved fluoride, expressed as F ⁻
H ₂ S	Hydrogen sulphide
HCl	Hydrogen chloride.
HCN	Hydrogen cyanide
HF	Hydrogen fluoride.
Hg	The sum of mercury and its compounds, expressed as Hg.
N ₂ O	Dinitrogen monoxide (nitrous oxide).
NH ₃	Ammonia.
Ni	The sum of nickel and its compounds, expressed as Ni.
NO _x	The sum of nitrogen monoxide (NO) and nitrogen dioxide (NO ₂), expressed as NO ₂ .
Pb	The sum of lead and its compounds, expressed as Pb.
PCDD/F	Polychlorinated dibenzo- <i>p</i> -dioxins and -furans.
RCG	Raw concentration in the flue-gas. Concentration of SO ₂ in the raw flue-gas as a yearly average (under the standard conditions given under General considerations) at the inlet of the SO _x abatement system, expressed at a reference oxygen content of 6 vol-% O ₂
Sb+As+Pb+Cr+Co+Cu+Mn+Ni+V	The sum of antimony, arsenic, lead, chromium, cobalt, copper, manganese, nickel, vanadium and their compounds, expressed as Sb+As+Pb+Cr+Co+Cu+Mn+Ni+V.

SO ₂	Sulphur dioxide.
SO ₃	Sulphur trioxide
SO _x	The sum of sulphur dioxide (SO ₂) and sulphur trioxide (SO ₃), expressed as SO ₂
Sulphate (SO ₄ ²⁻)	Dissolved sulphate, expressed as SO ₄ ²⁻ .
Sulphide, easily released	The sum of dissolved sulphide and of those undissolved sulphides that are easily released upon acidification, expressed as S ²⁻
Sulphite	Dissolved sulphite, expressed as SO ₃ ²⁻
TOC	Total organic carbon, expressed as C (in water);
TSS	Total suspended solids. Mass concentration of all suspended solids (in water), measured via filtration through glass fibre filters and gravimetry.
TVOC	Total volatile organic carbon, expressed as C (in air).
Zn	The sum of zinc and its compounds, expressed as Zn.

Acronyms

For the purposes of these BAT conclusions, the following acronyms apply:

Acronym	Definition
ASU	Air supply unit
CCGT	Combined-cycle gas turbine, with or without supplementary firing
CFB	Circulating fluidised bed
CHP	Combined heat and power
COG	Coke oven gas
COS	Carbonyl sulphide
DLN	Dry low-NO _x burners
DSI	Duct sorbent injection
ESP	Electrostatic precipitator
FBC	Fluidised bed combustion

FGD	Flue-gas desulphurisation
HFO	Heavy fuel oil
HRSG	Heat recovery steam generator
IGCC	Integrated gasification combined cycle
LHV	Lower heating value
LNB	Low-NO _x burners
LNG	Liquefied natural gas
OCGT	Open-cycle gas turbine
OTNOC	Other than normal operating conditions
PC	Pulverised combustion
PEMS	Predictive emissions monitoring system
SCR	Selective catalytic reduction
SDA	Spray dry absorber
SNCR	Selective non-catalytic reduction